

**GEORGIA PACIFIC CORPORATION  
BROWN STOCK WASHER LINES  
CLEAN CONDENSATE ALTERNATIVE  
REPORT**

**TOLEDO, OREGON  
PAPER MILL**

**NOVEMBER 5-6, 2014**

Permit #21-0005

Prepared: January 6, 2014

Prepared by:



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## EXECUTIVE SUMMARY

The November 2014 results of Georgia Pacific's Brownstock Washers (BSW) testing are summarized below.

### Brownstock Washers Testing Results

Source	MeOH (ppm)	Flow (dscfm)	MeOH (lb/day)	Production (ODT/day)	Emissions (lb/ODT)
<b>Kraft Brownstock Washer #1 (EU 128-A)</b>					
Washer Hood Vent	0.00	0	0.00	386	
Foam Breaker Vent	331.02	1,818	72.24		
Vacuum Pump Exhaust	29.52	1576	5.59		
<b>#1 BSW Sum</b>			<b>77.83</b>		
<b>Kraft Brownstock Washer #2 (EU 128-B)</b>					
Combined Vent	88.41	2,576	27.17	352	
<b>#2 BSW Sum</b>			<b>27.17</b>		
<b>Kraft Brownstock Washer #3 (EU 128-C)</b>					
Combined Vent	274.23	799	26.50	399	
<b>#3 BSW Sum</b>			<b>26.50</b>		
<b>Totals for #1, #2, #3 Brownstock Washers</b>			<b>131.50</b>	<b>1,137</b>	<b>0.116</b>

Detailed discussions and results from this emissions test project are included in the body of this report.

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## 1.0 SOURCE INFORMATION AND TEST DATE

Georgia Pacific's Toledo Paper Mill hired Bighorn Environmental to conduct source testing on its Brownstock Washers (BSW) to quantify their emissions of methanol. Bighorn conducted the source tests on November 5-6, 2014 to accurately quantify emissions from these sources. This testing was conducted to determine compliance with the CCA rules as outlined in their Title V permit.

Georgia Pacific's Dan Kunde and Karl Schumacher coordinated the project. Mr. Kunde and Mr. Schumacher oversaw the testing. Bighorn's Collin Rose, Clayton Krietzman and Tim Homer conducted three-one hour runs on each source on the three Brownstock Washers. Table 1 lists sources, test dates, and times.

**TABLE 1. SOURCE TEST DATES AND TIMES**

<b>SOURCE</b>	<b>DATE</b>	<b>TIME</b>
<b>Kraft Brownstock Washer #1 (EU 128-A)</b>		
Washer Hood Vent	11/6/14	Not tested, see note Section 2.0
Foam Breaker Vent	11/6/14	09:10-10:10; 10:35-11:35; 11:55-12:55
Vacuum Pump Exhaust	11/6/14	09:10-10:10; 10:35-11:35; 11:55-12:55
<b>Kraft Brownstock Washer #2 (EU 128-B)</b>		
Combined Vent	11/5/14	14:00-15:00; 15:10-16:10; 16:19-17:19
<b>Kraft Brownstock Washer #3 (EU 128-C)</b>		
Combined Vent	11/5/14	09:55-10:55; 11:00-12:00; 12:5-13:05

## 2.0 POLLUTANTS AND TEST METHODS

Bighorn Environmental conducted Methanol source tests on Georgia Pacific's Brownstock Washers using its source sampling equipment. After the samples were gathered, they were sent to ACC for analysis. Chain of custody forms can be found in the Appendix.

Bighorn performed velocity traverses to calculate flow rates and convert analytical data to emission concentrations and rates. Table 3 outlines the test methods Bighorn used.

**TABLE 3. TEST METHODS**

<b>PARAMETER</b>	<b>TEST METHODS</b>
Velocity & Flow	EPA Method 1, 1A & 2
Moisture	ODEQ Method 4
Methanol	NCASI CI/SG/PULP-94.03

When trying to obtain velocity readings on the #1 BSW combined vent, the flow readings were "backward", i.e. the flow was towards the BSW hood and away from the stack vent. This was verified with both the pitot tube and also inserting a rag into the stack and observing it "flutter" toward the BSW hood. Therefore no testing was conducted on this source. These reverse flows were verified at the beginning, middle and end of each test. An explanation by the engineer who designed the system outlining the reason for this can be found in the Appendix.

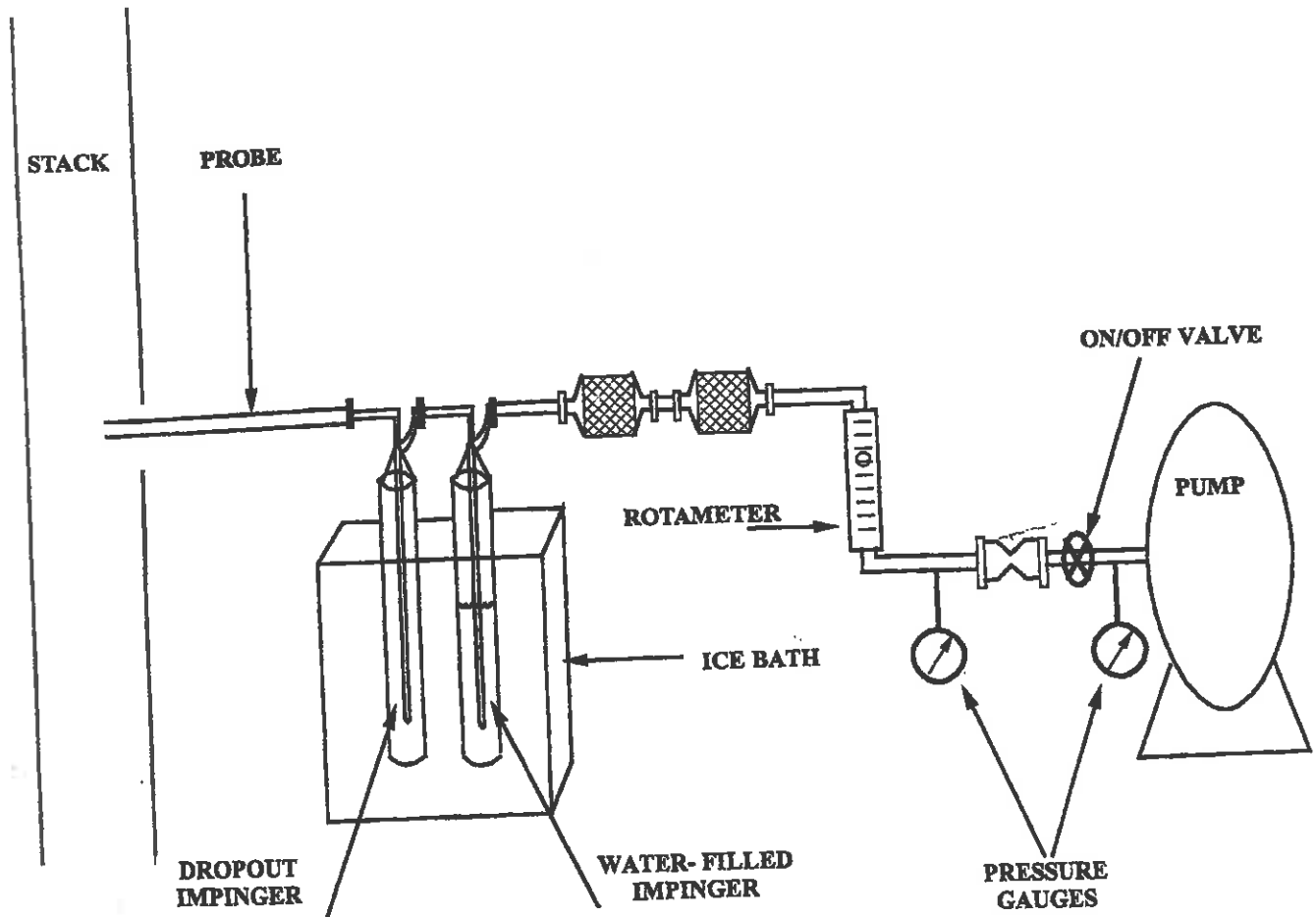
Georgia Pacific petitioned EPA to use the NCASI Method in place of EPA Method 308 for Methanol. EPA approved this deviation, and the associated letters can be found in the Appendix.

Stack moisture was measured using ODEQ Method 4 and two measurements were taken and recorded during each run.

### 3.0 SOURCE SAMPLING EQUIPMENT

Figure 1 is a schematic of Bighorns Sampling Train used for the testing of Methanol.

FIGURE 1. NCASI METHANOL SAMPLING TRAIN



#### 4.0 RESULTS

Table 4 summarizes the results from the Brown Stock Washer Line testing.

**Table 4. Brownstock Washers Emissions Results**

Source	MeOH (ppm)	Flow (dscfm)	MeOH (lb/day)	Production (ODT/day)	Emissions (lb/ODT)
<b>Kraft Brownstock Washer #1 (EU 128-A)</b>					
Washer Hood Vent	0.00	0	0.00	386	
Foam Breaker Vent	331.02	1,818	72.24		
Vacuum Pump Exhaust	29.52	1576	5.59		
<b>#1 BSW Sum</b>			<b>77.83</b>		
<b>Kraft Brownstock Washer #2 (EU 128-B)</b>					
Combined Vent	88.41	2,576	27.17	352	
<b>#2 BSW Sum</b>			<b>27.17</b>		
<b>Kraft Brownstock Washer #3 (EU 128-C)</b>					
Combined Vent	274.23	799	26.50	399	
<b>#3 BSW Sum</b>			<b>26.50</b>		
<b>Totals for #1, #2, #3 Brownstock Washers</b>			<b>131.50</b>	<b>1,137</b>	<b>0.116</b>

Field data sheets, flow rate information, analytical data, calculated emissions data, and calculations are contained in Appendices A-B. Appendix D contains Georgia Pacific's production data for this project.

## 5.0 SUPPORTING DATA

Supporting data sheets are located in Appendix A while required support equipment quality control records are in Appendix C.

## 6.0 QUALITY ASSURANCE

Bighorn's QA procedures follow EPA's *Quality Assurance Handbook for Air Pollution Measurement Systems, Vol. III, Stationary Source Specific Methods* September 1994 as revised and amended (#EPA/600/R-94/038c). Bighorn used EPA method specific quality assurance procedures. The following *July 1, 2013 40 CFR 60* sections were referenced for this project:

Appendix A - Methods 1, 2, 4 and NCASI CI/SG/PULP-94.03

Bighorn Environmental is zealous in our commitment to thorough quality practices. We conduct stringent quality assurance and quality control (QA and QC) procedures on all reference CEMS and support equipment.

Bighorn employs the latest CAI and Advanced Pollution Incorporated (API) CEMS that are considered state-of-the-art by environmental professionals. We've designed an effective primary sample conditioner that works in concert with Horiba's secondary conditioners. Together, they provide dry, clean sample gas to Bighorn's CEMS.

EPA Protocol No. 1 first order QA standards allow Bighorn to challenge equipment and methods to ensure that data is valid for determining monitor accuracy and precision. Before each test, Bighorn challenges its monitors and then entire system at the probe which simulates actual sampling. QA standards introduced at the sample probe traverse through all sample lines, conditioning chambers, and monitors to determine initial system integrity or bias. Following each test, Bighorn conducts QA of the entire monitoring system to determine final system bias and test calibration drift.

Bighorn's Mobile Air Emissions Laboratory contain two APC Model 1400 uninterruptible power supplies (UPS) to complement our QA/QC commitment. These QC devices continuously regulate and condition client-supplied 120 VAC power so Bighorn's electronic analyzers receive a consistent clean  $115 \pm 5$  VAC signal. Chronic brownout and over-voltage conditions are eliminated thereby reducing hardware failures and data errors. Also, temporary power outages do not shut down our CEMS nor jeopardize data quality because the UPS' generate consistent pure sine wave signals for up to one hour with their built in batteries.

Cross checks such as manual calculations of Bighorn's automated DAS computer generated results allow test results verification. Bighorn files manufacturers' accuracy certificates and interference tables for CEMS, flow controllers, gases, etc. Additionally dry gas meters, pitot tubes, thermocouples, gas dividers, etc. are certified as per EPA



requirements and frequencies. Where EPA frequencies are not specified, Bighorn has established those based on state regulatory criteria.

Thorough chain-of-custody procedures and documentation provide proof of our QA/QC efforts. Relevant QA/QC documentation is included in this final report's Appendices for results support and regulatory review.

**APPENDIX A  
SUPPORTING DATA**

EMISSION RATE

Georgia Pacific					
#1 BSW Foam Breaker					
Emissions Rates Calculations					
6-Nov-14					
	<b>#1 BSW Foam Breaker</b>				
	Run #1	Run #2	Run #3	Average	
	09:10-10:10	10:35-11:35	11:55-12:55		
MeOH (ppm)	278.3625	470.7149	243.9800	331.0191	
Stack Flow:					
acfm:	2173	2250	2208	2211	
dscfm:	1789	1839	1826	1818	
Pulp Production:					
ODT/day:	386.00	386.00	386.00	386.0000	
MeOH Emissions at Standard Conditions:					
lb/hr.:	2.48626	4.32066	2.22345	3.0101	
lb/day:	59.67023	103.69594	53.36284	72.2430	
lb/ODT:	0.15459	0.26864	0.13825	0.1872	

00001



Georgia Pacific  
 #1 BSW Foam Breaker  
 Stack Gas Flow Rate Data and Calculations  
 6-Nov-14

Run #1

Barometric Pressure: 29.81  
 Stack Diameter or Dimensions (in.): 15.75  
 Cross Sectional Area (sq ft): 1.3529699  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.2	115	575	-0.06	29.81	0.4472
2	0.21	115	575	-0.06	29.81	0.4583
3	0.21	115	575	-0.06	29.81	0.4583
4	0.19	115	575	-0.06	29.81	0.4359
5	0.22	115	575	-0.06	29.81	0.469
6	0.23	115	575	-0.06	29.81	0.4796
7	0.21	115	575	-0.06	29.81	0.4583
8	0.19	115	575	-0.06	29.81	0.4359
9	0.19	115	575	-0.06	29.81	0.4359
10	0.19	115	575	-0.06	29.81	0.4359
11	0.2	115	575	-0.06	29.81	0.4472
12	0.2	115	575	-0.06	29.81	0.4472
13	0.16	115	575	-0.06	29.81	0.4
14	0.19	115	575	-0.06	29.81	0.4359
15	0.2	115	575	-0.06	29.81	0.4472
16	0.2	115	575	-0.06	29.81	0.4472
AVG.		115.00	575.00		29.81	0.4462

wet bulb temp. (deg F): 115.00

stack vapor pressure: 2.9774087

%H2O: 9.9894312

Molecular Density: 0.9001057

Molecular weight of dry gas: 28.708 lb/lb mole dry

Molecular weight of wet stack gas: 27.638332 lb/lb mole wet

Stack gas velocity at stack conditions: 1606.34207 afpm

Stack gas flow rate at std. conditions: 1789.45946 dscfm

Stack gas flow rate at stack conditions: 2173.33249 acfm

Georgia Pacific  
 #1 BSW Foam Breaker  
 Stack Gas Flow Rate Data and Calculations  
 6-Nov-14

Run #2

Barometric Pressure: 29.81  
 Stack Diameter or Dimensions (in.): 15.75  
 Cross Sectional Area (sq ft): 1.3529699  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.2	116.5	576.5	-0.06	29.81	0.4472
2	0.2	116.5	576.5	-0.06	29.81	0.4472
3	0.2	116.5	576.5	-0.06	29.81	0.4472
4	0.23	116.5	576.5	-0.06	29.81	0.4796
5	0.21	116.5	576.5	-0.06	29.81	0.4583
6	0.24	116.5	576.5	-0.06	29.81	0.4899
7	0.22	116.5	576.5	-0.06	29.81	0.469
8	0.22	116.5	576.5	-0.06	29.81	0.469
9	0.23	116.5	576.5	-0.06	29.81	0.4796
10	0.23	116.5	576.5	-0.06	29.81	0.4796
11	0.25	116.5	576.5	-0.06	29.81	0.5
12	0.23	116.5	576.5	-0.06	29.81	0.4796
13	0.22	116.5	576.5	-0.06	29.81	0.469
14	0.19	116.5	576.5	-0.06	29.81	0.4359
15	0.16	116.5	576.5	-0.06	29.81	0.4
16	0.18	116.5	576.5	-0.06	29.81	0.4243
AVG.		116.5	576.5		29.81	0.461

wet bulb temp. (deg F): 116.50

stack vapor pressure: 3.1091027

%H2O: 10.431275

Molecular Density: 0.8956873

Molecular weight of dry gas: 28.7032 lb/lb mole dry

Molecular weight of wet stack gas: 27.58672 lb/lb mole wet

Stack gas velocity at stack conditions: 1663.27274 afpm

Stack gas flow rate at std. conditions: 1838.98727 dscfm

Stack gas flow rate at stack conditions: 2250.35798 acfm

Georgia Pacific  
 #1 BSW Foam Breaker  
 Stack Gas Flow Rate Data and Calculations  
 6-Nov-14

Run #3

Barometric Pressure: 29.81  
 Stack Diameter or Dimensions (in.): 15.75  
 Cross Sectional Area (sq ft): 1.3529699  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.19	114.5	574.5	-0.07	29.80	0.4359
2	0.23	114.5	574.5	-0.07	29.80	0.4796
3	0.23	114.5	574.5	-0.07	29.80	0.4796
4	0.23	114.5	574.5	-0.07	29.80	0.4796
5	0.22	114.5	574.5	-0.07	29.80	0.469
6	0.2	114.5	574.5	-0.07	29.80	0.4472
7	0.2	114.5	574.5	-0.07	29.80	0.4472
8	0.2	114.5	574.5	-0.07	29.80	0.4472
9	0.18	114.5	574.5	-0.07	29.80	0.4243
10	0.19	114.5	574.5	-0.07	29.80	0.4359
11	0.2	114.5	574.5	-0.07	29.80	0.4472
12	0.19	114.5	574.5	-0.07	29.80	0.4359
13	0.19	114.5	574.5	-0.07	29.80	0.4359
14	0.21	114.5	574.5	-0.07	29.80	0.4583
15	0.22	114.5	574.5	-0.07	29.80	0.469
16	0.22	114.5	574.5	-0.07	29.80	0.469
AVG.		114.5	574.5		29.80	0.4538

wet bulb temp. (deg F): 114.00

stack vapor pressure: 2.8923602

%H2O: 9.6873009

Molecular Density: 0.903127

Molecular weight of dry gas: 28.708 lb/lb mole dry

Molecular weight of wet stack gas: 27.670684 lb/lb mole wet

Stack gas velocity at stack conditions: 1632.12459 afpm

Stack gas flow rate at std. conditions: 1825.82669 dscfm

Stack gas flow rate at stack conditions: 2208.21546 acfm

**Average stack gas flow rate at standard conditions:**

**1818 dscfm**

**Average stack gas flow rate at stack conditions:**

**2211 acfm**

**Avg % Mois**

10.04

**Average Velocity**

1633.91

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/6/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: #1 Fean Brecker

Run Number: 1  
 Start Time: 9:10 Stop Time: 10:10  
 Ambient Temp at Start: 50 Ambient Temp at Stop: 50  
 Barometric Pressure: 29.81

Leak Test

Time: 9:30 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 10:12 Final Measurement (in Hga): 0 on DGM  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample FlowRate:  
 1. 58 2. 58 3. 60 4. 60 5. 61 Avg: 15.2 C  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM Temp  
 DGM Pressure

Rotameter Readings	QA/QC Measures
Time: <u>9:20</u> Flow: <u>3.946</u>	Train Spike Conducted? Yes No
Time: <u>9:30</u> Flow: <u>8.003</u>	Duplicate Conducted? Yes No
Time: <u>9:40</u> Flow: <u>12.213</u>	Spiked Duplicate Made? Yes No
Time: <u>9:50</u> Flow: <u>16.001</u>	Field Blank Made? Yes No
Time: <u>10:00</u> Flow: <u>19.984</u>	Field Spike Made? Yes No
Time: <u>10:10</u> Flow: <u>23.997</u>	

Sample Bottle Weight(s):  
 Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments  
DGM used for sample volume collection

Bottle # 9  
 Box # 2

Figure 2. Field Sampling Data Sheet

	Dry Bulb	Wet bulb
1	115	115
2	115	115
Avg	115	115

August 1998



NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/6/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: #1 From Brecker

Run Number: \_\_\_\_\_  
 Start Time: 1035 Stop Time: 1135  
 Ambient Temp at Start: 50 Ambient Temp at Stop: 52  
 Barometric Pressure: 29.91

**Leak Test**

Time: 1030 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1136 Final Measurement (in Hga): 0 in DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes No

**System Flow Rate Measurement**

Average of 5 flow measurements for Pre-Sample FlowRate:  
 1. 60 2. 61 3. 62 4. 62 5. 63 Avg: 16.40  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!)  
 Avg: \_\_\_\_\_

DGM Temp  
DGM Pressure

Rotameter Readings		QA/QC Measures	
Time: <u>1045</u>	Flow: <u>4.072</u>	Train Spike Conducted?	Yes No
Time: <u>1055</u>	Flow: <u>8.009</u>	Duplicate Conducted?	Yes No
Time: <u>1105</u>	Flow: <u>12.017</u>	Spiked Duplicate Made?	Yes No
Time: <u>1115</u>	Flow: <u>16.034</u>	Field Blank Made?	Yes No
Time: <u>1125</u>	Flow: <u>20.021</u>	Field Spike Made?	Yes No
Time: <u>1135</u>	Flow: <u>24.033</u>		

**Sample Bottle Weight(s):**  
 Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

**Notes/Comments**  
DGM used for sample volume collection

Bottle #11

Box #2

Figure 2. Field Sampling Data Sheet

	Dry Bulb	Wet bulb
1	117	117
2	116	116
Avg	116.5	116.5

August 1998

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: CP-Toledo Date: 11/6/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: #2 Foam Breaker

Run Number: 3  
 Start Time: 1155 Stop Time: 1255  
 Ambient Temp at Start: 50 Ambient Temp at Stop: 50  
 Barometric Pressure: 29.81

Leak Test

Time: 1151 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1257 Final Measurement (in Hga): 0 on DGM  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample FlowRate:  
 1. 62 2. 62 3. 62 4. 63 5. 63 Avg: 16.9  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM  
Temp  
DGM  
Pressure

Rotameter Readings   
 Time: 1205 Flow: 3.902  
 Time: 1215 Flow: 7.977  
 Time: 1225 Flow: 11.983  
 Time: 1235 Flow: 16.001  
 Time: 1245 Flow: 26.022  
 Time: 1255 Flow: 24.613

QA/QC Measures  
 Train Spike Conducted? Yes No  
 Duplicate Conducted? Yes No  
 Spiked Duplicate Made? Yes No  
 Field Blank Made? Yes No  
 Field Spike Made? Yes No

Sample Bottle Weight(s):

Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments

DGM used for sample volume collection

Bottle #13

Box #2

Figure 2. Field Sampling Data Sheet

	Dry Bulb	Wet bulb
1	114	113
2	115	115
Avg	114.5	114

## GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant: GP-Toledo		Location: Toledo, OR		Source: #1 Foam Breaker	
Date: 11/11/14 <del>1/01/1900</del>		Operator: Homer		Run No.: 1 & 2	
Barometric Press.: 29.81		Reading Location: Lab		Ambient Temp:	
Elevation: 0		Elevation Corr.: 0		Corr. Bar. Press.: 0	
Avg. wet bulb temp (F):		% O2:		% CO2:	
Pitot tube ID #: 4' Stype		Pitot Cp:		Last Calibration:	
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check	
				Vel. At 0 reference	Angle to get 0 Flow
1	.120	See next	-.06	0	0
2	.121			0	0
3	.121			0	0
4	.119			0	0
5	.122			.102	5
6	.123			.103	4
7	.121			0	0
8	.119			0	0
9	.119			.103	5
10	.119			.103	5
11	.120			0	0
12	.120			0	0
13	.116			.101	2
14	.119			0	0
15	.120			0	0
16	.120			0	0
1	.120		-.06		
2	.120				
3	.120				
4	.123				
5	.121				
6	.124				
7	.122				
8	.122				

RUN #1

RUN #2

## GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant		GP-Toledo	Location:		Toledo, OR	Source:		#1 Foam Breaker
Date		11/6/14	<del>1/0/1900</del>	Operator:		Homer	Run No.: 2&3	
Barometric Press.		0	Reading Location:		Lab	Ambient Temp:		0
Elevation:		0	Elevation Corr.:		0	Corr. Bar. Press.:		0
Avg. wet bulb temp (F)		0	% O2			% CO2:		
Pitot tube ID #:		4' Stype	Pitot Cp:		0	Last Calibration:		1/0/1900
Traversal Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check				
				Vel. At 0 reference	Angle to get 0 Flow			
9	.23							
10	.23							
11	.25							
12	.23							
13	.22							
14	.19							
15	.16							
16	.18							
1	.19							
2	.23							
3	.23							
4	.23							
5	.22							
6	.20							
7	.20							
8	.20							
9	.18							
10	.19							
11	.20							
12	.19							
13	.19							
14	.21							
15	.22							
16	.22							

RUN #2

RUN #3

## TRAVERSE POINT LOCATION WORKSHEET METHOD 1

### DATA

### STACK CROSS SECTION DIAGRAM

Plant:	GP-Toledo	Location:	Toledo, OR	See Diagram	
Source:	#1 Foam Breaker, Combinded Vent	Operator:	Homer		
Date		Port Depth(in.):	0.125		
Stack Dia. (in.)	15.75	Stack Area (ft2):	1.35		
Distance to disturbance:					
Upstream(ft):		Downstream(ft):			
# of traverse points required:			16		
Traverse point #	% of Stack Dia.	Stack Dia.	% of Stack Dia. X Stack Dia.	Port Depth	Taverse Point Location
1	0.032	15.75	0.5	0.125	0.63
2	0.105	15.75	1.7	0.125	1.78
3	0.194	15.75	3.1	0.125	3.18
4	0.323	15.75	5.1	0.125	5.21
5	0.677	15.75	10.7	0.125	10.79
6	0.806	15.75	12.7	0.125	12.82
7	0.895	15.75	14.1	0.125	14.22
8	0.968	15.75	15.2	0.125	15.37

**NOTES:** \_\_\_\_\_

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MeOH concentration

Georgia Pacific				
#1 BSW Vacuum Pump Exhaust				
11/6/2014				
Total MeOH catch & DGM volume				
<b>Run 1</b>				
DGM Volume (l)	24.029			
Meter Y	1.006			
DGM Temp (C)	13.2			
Baro Pressure	29.81			
DGM Volume (dsc)	24.657			
			Total MeOH catch (mirco g)	950.00
MW of MeOH	32.04		Correction Factor	1
MeOH (ppmvd)	28.909029			
<b>Run 2</b>				
DGM Volume (l)	24.25			
Meter Y	1.006			
DGM Temp (C)	15.40			
Baro Pressure	29.81			
DGM Volume (dsc)	24.693			
			Total MeOH catch (mirco g)	925.00
MW of MeOH	32.04		Correction Factor	1
MeOH (ppmvd)	28.106141			
<b>Run 3</b>				
DGM Volume (l)	24.01			
Meter Y	1.006			
DGM Temp (C)	17.60			
Baro Pressure	29.81			
DGM Volume (dsc)	24.264			
			Total MeOH catch (mirco g)	1020.00
MW of MeOH	32.04		Correction Factor	1
MeOH (ppmvd)	31.5413			

Georgia Pacific  
 #1 BSW Vacuum Pump Exhaust  
 Stack Gas Flow Rate Data and Calculations  
 6-Nov-14

Run #1

Barometric Pressure: 29.81  
 Stack Diameter or Dimensions (in.): 10  
 Cross Sectional Area (sq ft): 0.5454149  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.53	101.3	561.3	0	29.81	0.728
2	0.91	101.3	561.3	0	29.81	0.9539
3	0.94	101.3	561.3	0	29.81	0.9695
4	0.82	101.3	561.3	0	29.81	0.9055
5	0.44	101.3	561.3	0	29.81	0.6633
6	0.88	101.3	561.3	0	29.81	0.9381
7	0.9	101.3	561.3	0	29.81	0.9487
8	0.92	101.3	561.3	0	29.81	0.9592
AVG.		101.30	561.30		29.81	0.8833

wet bulb temp. (deg F): 97.70  
 stack vapor pressure: 1.7836937  
 %H2O: 5.8569194  
 Molecular Density: 0.9414308

Molecular weight of dry gas: 28.708 lb/lb mole dry  
 Molecular weight of wet stack gas: 28.080841 lb/lb mole wet  
 Stack gas velocity at stack conditions: 3116.8014 afpm  
 Stack gas flow rate at std. conditions: 1499.90525 dscfm  
 Stack gas flow rate at stack conditions: 1699.95002 acfm



Georgia Pacific  
 #1 BSW Vacuum Pump Exhaust  
 Stack Gas Flow Rate Data and Calculations  
 6-Nov-14

Run #2

Barometric Pressure: 29.81  
 Stack Diameter or Dimensions (in.): 10  
 Cross Sectional Area (sq ft): 0.5454149  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.62	102.5	562.5	0	29.81	0.7874
2	0.9	102.5	562.5	0	29.81	0.9487
3	0.92	102.5	562.5	0	29.81	0.9592
4	0.88	102.5	562.5	0	29.81	0.9381
5	0.9	102.5	562.5	0	29.81	0.9487
6	0.89	102.5	562.5	0	29.81	0.9434
7	0.91	102.5	562.5	0	29.81	0.9539
8	0.84	102.5	562.5	0	29.81	0.9165
AVG.		102.5	562.5		29.81	0.9245

wet bulb temp. (deg F): 100.60

stack vapor pressure: 1.9460891

%H2O: 6.4617748

Molecular Density: 0.9353823

Molecular weight of dry gas: 28.7032 lb/lb mole dry

Molecular weight of wet stack gas: 28.011583 lb/lb mole wet

Stack gas velocity at stack conditions: 3269.69571 afpm

Stack gas flow rate at std. conditions: 1560.03833 dscfm

Stack gas flow rate at stack conditions: 1783.34086 acfm

Georgia Pacific  
 #1 BSW Vacuum Pump Exhaust  
 Stack Gas Flow Rate Data and Calculations  
 6-Nov-14

Run #3

Barometric Pressure: 29.81  
 Stack Diameter or Dimensions (in.): 10  
 Cross Sectional Area (sq ft): 0.5454149  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.84	102.5	562.5	0	29.81	0.9165
2	0.96	102.5	562.5	0	29.81	0.9798
3	1	102.5	562.5	0	29.81	1
4	1.1	102.5	562.5	0	29.81	1.0488
5	1	102.5	562.5	0	29.81	1
6	0.96	102.5	562.5	0	29.81	0.9798
7	0.98	102.5	562.5	0	29.81	0.9899
8	0.97	102.5	562.5	0	29.81	0.9849
AVG.		102.5	562.5		29.81	0.9875

wet bulb temp. (deg F): 99.50

stack vapor pressure: 1.8828898

%H2O: 6.2110657

Molecular Density: 0.9378893

Molecular weight of dry gas: 28.708 lb/lb mole dry

Molecular weight of wet stack gas: 28.042919 lb/lb mole wet

Stack gas velocity at stack conditions: 3490.50879 afpm

Stack gas flow rate at std. conditions: 1669.85646 dscfm

Stack gas flow rate at stack conditions: 1903.77561 acfm

**Average stack gas flow rate at standard conditions:**

**1577 dscfm**

**Average stack gas flow rate at stack conditions:**

**1796 acfm**

**Avg % Mois**

**6.18**

**Average Velocity**

**3292.34**

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: CP-Toledo Date: 11/6/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: #4 BSW - Vacuum Pump

Run Number: A  
 Start Time: 910 Stop Time: 1010  
 Ambient Temp at Start: 50 Ambient Temp at Stop: 50  
 Barometric Pressure: 29.91

Leak Test

Time: 0805 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1012 Final Measurement (in Hga): 0 on DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria?  Yes  No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample Flow Rate: OC  
 1. 12 2. 12 3. 14 4. 14 5. 14 Avg: 13.2  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM Temp  
 DGM Pressure

Rotameter Readings

Time: 920 Flow: 15.42  
 Time: 930 Flow: 8.09  
 Time: 940 Flow: 12.64  
 Time: 950 Flow: 16.34  
 Time: 1000 Flow: 20.14  
 Time: 1010 Flow: 24.029

QA/QC Measures

Train Spike Conducted?	Yes	No
Duplicate Conducted?	Yes	No
Spiked Duplicate Made?	Yes	No
Field Blank Made?	Yes	No
Field Spike Made?	Yes	No

Sample Bottle Weight(s):

Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments

DGM used for sample volume collection

Bottle # 8

Figure 2. Field Sampling Data Sheet

	Dry Bulb	Wet bulb
1	102.2	98.2
2	100.4	96.8
Avg	101.3	97.7

Bottle # 2 yellow  
 39  
 37

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP- Toledo Date: 11/6/14  
 City, State: Toledo, OH Sampler's Name: Homer  
 Source Name/Description: BSU #1 - Vacuum Pump

Run Number: 2  
 Start Time: 1035 Stop Time: 1135  
 Ambient Temp at Start: 50 Ambient Temp at Stop: \_\_\_\_\_

Barometric Pressure: \_\_\_\_\_

Leak Test

Time: 1025 Initial Measurement (in Hga): 12 on 0.6m no bubbles  
 Time: 1137 Final Measurement (in Hga): 6 on 0.6m no bubbles  
 Leak Check Criteria: Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria?  Yes  No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample Flow Rate: \_\_\_\_\_  
 1. \_\_\_\_\_ 2. \_\_\_\_\_ 3. \_\_\_\_\_ 4. \_\_\_\_\_ 5. \_\_\_\_\_ Avg: 15.4 missing  
 Average of 5 flow measurements for Post-Sample Flow Rate: \_\_\_\_\_  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: used  
 Overall Average Sample Flow Rate: (indicate units!) \_\_\_\_\_ Avg: \_\_\_\_\_

DGM  
Temp  
DGM  
Pressure

used  
Run 1 13

Rotameter Readings		QA/QC Measures		
Time: <u>1045</u>	Flow: <u>4.08</u>	Train Spike Conducted?	Yes	No
Time: <u>1055</u>	Flow: <u>6.09</u>	Duplicate Conducted?	Yes	No
Time: <u>1105</u>	Flow: <u>12.08</u>	Spiked Duplicate Made?	Yes	No
Time: <u>1115</u>	Flow: <u>16.2</u>	Field Blank Made?	Yes	No
Time: <u>1125</u>	Flow: <u>20.25</u>	Field Spike Made?	Yes	No
Time: <u>1135</u>	Flow: <u>24.25</u>			

Sample Bottle Weight(s):  
 Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments  
DGM used for sample volume collection

Bottle #10

Bar #2

Figure 2. Field Sampling Data Sheet

	Dry Bulb	Wet bulb
1	101	99
2	104	102.2
Avg	102.5	100.6

August 1998

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/6/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: #1 BSW Vacuum Pump

Run Number: 3  
 Start Time: 1155 Stop Time: 1255  
 Ambient Temp at Start: 50 Ambient Temp at Stop: 56  
 Barometric Pressure: \_\_\_\_\_

Leak Test

Time: 1150 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1257 Final Measurement (in Hga): 0 on DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample Flow Rate:  
 1. 17 2. 17 3. 18 4. 18 5. 18 Avg: 17.6  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM Temp  
 DGM Pressure

Rotameter Readings		QA/QC Measures	
Time: <u>1205</u>	Flow: <u>4.02</u>	Train Spike Conducted?	Yes No
Time: <u>1215</u>	Flow: <u>8.08</u>	Duplicate Conducted?	Yes No
Time: <u>1225</u>	Flow: <u>17.15</u>	Spiked Duplicate Made?	Yes No
Time: <u>1235</u>	Flow: <u>16.20</u>	Field Blank Made?	Yes No
Time: <u>1245</u>	Flow: <u>20.15</u>	Field Spike Made?	Yes No
Time: <u>1255</u>	Flow: <u>24.01</u>		

Sample Bottle Weight(s):

Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments

DGM used for sample volume collection

Bottle #12

Bar #2

Figure 2. Field Sampling Data Sheet

	Dry Bulb	Wet bulb
1	102	99
2	103	101
Avg	102.5	99.5

August 1998

## GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant: GP-Toledo		Location: Toledo, OR		Source: #1 Vacuum Pump	
Date:		Operator: Homer		Run No.: 1 & 2&3	
Barometric Press.:		Reading Location: Lab		Ambient Temp.:	
Elevation: 0		Elevation Corr.: 0		Corr. Bar. Press.: 0	
Avg. wet bulb temp (F):		% O2:		% CO2:	
Pitot tube ID #: 4' Stype		Pitot Cp:		Last Calibration:	
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check	
				Vel. At 0 reference	Angle to get 0 Flow
1	.53	102.2	0	.07	5
2	.91			.06	2
3	.94			.17	5
4	.82			.11	3
5	.94			0	0
6	.88			.14	3
7	.90			.17	3
8	.92			.06	3
1	.62			.06	5
2	.90			.07	3
3	.92			.10	5
4	.88			.11	5
5	.90			.02	3
6	.89			.07	5
7	.91			.06	5
8	.84	100.4		.01	3
1	.84				
2	.96				
3	1.0				
4	1.1				
5	1.0				
6	.96				
7	.98				
8	.97				

Horizontal traverse only Bottom port poured black liquid everywhere



EMISSION RATE

Georgia Pacific				
Kraft BSW #2 Combined Vent				
Emissions Rates Calculations				
5-Nov-14				
	<b>Kraft BSW #2 Combined Vent</b>			
	Run #1	Run #2	Run #3	Average
	14:00-15:00	15:10-16:09	16:19-17:19	
<b>MeOH (ppm)</b>	118.4989	92.7630	53.9736	88.4118
Stack Flow:				
acfm:	3301	3308	3401	3337
dsicfm:	2540	2561	2628	2576
Pulp Production:				
ODT/day:	352.00	352.00	352.00	352.00
<b>MeOH Emissions at Standard Conditions:</b>				
lb/hr.:	1.50240	1.18554	0.70792	1.13195
lb/day.:	36.05751	28.45294	16.99003	27.16683
lb/ODT:	0.10244	0.08083	0.04827	0.07718

00022



MeOH concentration

Georgia Pacific				
Kraft BSW #2 Combined Vent				
11/5/2014				
Total MeOH catch & DGM volume				
<b>Run 1</b>				
DGM Volume (l)	24.007			
Meter Y	1.01			
DGM Temp (C)	25.4			
Baro Pressure	29.76			
DGM Volume (dscl)	23.68			
			Total MeOH catch (mirco g)	3740
MW of MeOH	32.04		Correction Factor	1
MeOH (ppmvd)	118.49885			
<b>Run 2</b>				
DGM Volume (l)	24.051			
Meter Y	1.01			
DGM Temp (C)	24.7			
Baro Pressure	29.76			
DGM Volume (dscl)	23.78			
			Total MeOH catch (mirco g)	2940
MW of MeOH	32.04		Correction Factor	1
MeOH (ppmvd)	92.762971			
<b>Run 3</b>				
DGM Volume (l)	24.126			
Meter Y	1.01			
DGM Temp (C)	24			
Baro Pressure	29.76			
DGM Volume (dscl)	23.91			
			Total MeOH catch (mirco g)	1720
MW of MeOH	32.04		Correction Factor	1
MeOH (ppmvd)	53.973576			

Georgia Pacific  
 Kraft BSW #2 Combined Vent  
 Stack Gas Flow Rate Data and Calculations  
 5-Nov-14

Run #1

Barometric Pressure: 29.76  
 Stack Diameter or Dimensions (in.): 16  
 Cross Sectional Area (sq ft): 1.3962622  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.5	130.1	590.1	-0.74	29.71	0.7071
2	0.52	130.1	590.1	-0.74	29.71	0.7211
3	0.53	130.1	590.1	-0.74	29.71	0.728
4	0.29	130.1	590.1	-0.74	29.71	0.5385
5	0.31	130.1	590.1	-0.74	29.71	0.5568
6	0.38	130.1	590.1	-0.74	29.71	0.6164
7	0.4	130.1	590.1	-0.74	29.71	0.6325
8	0.34	130.1	590.1	-0.74	29.71	0.5831
9	0.38	130.1	590.1	-0.74	29.71	0.6164
10	0.41	130.1	590.1	-0.74	29.71	0.6403
11	0.35	130.1	590.1	-0.74	29.71	0.5916
12	0.27	130.1	590.1	-0.74	29.71	0.5196
13	0.51	130.1	590.1	-0.74	29.71	0.7141
14	0.55	130.1	590.1	-0.74	29.71	0.7416
15	0.44	130.1	590.1	-0.74	29.71	0.6633
16	0.53	130.1	590.1	-0.74	29.71	0.728
AVG.		130.10	590.10		29.71	0.6437

wet bulb temp. (deg F): 125.60

stack vapor pressure: 4.0208647

%H2O: 13.388152

Molecular Density: 0.8661185

Molecular weight of dry gas: 28.7796 lb/lb mole dry

Molecular weight of wet stack gas: 27.336411 lb/lb mole wet

Stack gas velocity at stack conditions: 2364.43494 afpm

Stack gas flow rate at std. conditions: 2540.13345 dscfm

Stack gas flow rate at stack conditions: 3301.37118 acfm

Georgia Pacific  
 Kraft BSW #2 Combined Vent  
 Stack Gas Flow Rate Data and Calculations  
 5-Nov-14

Run #2

Barometric Pressure: 29.76  
 Stack Diameter or Dimensions (in.): 16  
 Cross Sectional Area (sq ft): 1.3962622  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F) (deg R)		Stack Static Pressure (in. H2O) (in Hg.)		Sqrt ^P
1	0.51	128.6	588.6	-0.77	29.70	0.7141
2	0.54	128.6	588.6	-0.77	29.70	0.7348
3	0.55	128.6	588.6	-0.77	29.70	0.7416
4	0.31	128.6	588.6	-0.77	29.70	0.5568
5	0.31	128.6	588.6	-0.77	29.70	0.5568
6	0.33	128.6	588.6	-0.77	29.70	0.5745
7	0.41	128.6	588.6	-0.77	29.70	0.6403
8	0.36	128.6	588.6	-0.77	29.70	0.6
9	0.51	128.6	588.6	-0.77	29.70	0.7141
10	0.5	128.6	588.6	-0.77	29.70	0.7071
11	0.5	128.6	588.6	-0.77	29.70	0.7071
12	0.36	128.6	588.6	-0.77	29.70	0.6
13	0.25	128.6	588.6	-0.77	29.70	0.5
14	0.39	128.6	588.6	-0.77	29.70	0.6245
15	0.46	128.6	588.6	-0.77	29.70	0.6782
16	0.47	128.6	588.6	-0.77	29.70	0.6856
AVG.		128.6	588.6		29.70	0.646

wet bulb temp. (deg F): 124.70  
 stack vapor pressure: 3.9216231  
 %H2O: 13.074289  
 Molecular Density: 0.8692571  
 Molecular weight of dry gas: 28.7688 lb/lb mole dry  
 Molecular weight of wet stack gas: 27.360856 lb/lb mole wet  
 Stack gas velocity at stack conditions: 2368.94023 afpm  
 Stack gas flow rate at std. conditions: 2560.51501 dscfm  
 Stack gas flow rate at stack conditions: 3307.66174 acfm

Georgia Pacific  
 Kraft BSW #2 Combined Vent  
 Stack Gas Flow Rate Data and Calculations  
 5-Nov-14

Run #3

Barometric Pressure: 29.76  
 Stack Diameter or Dimensions (in.): 16  
 Cross Sectional Area (sq ft): 1.3962622  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.47	130.1	590.1	-0.79	29.70	0.6856
2	0.37	130.1	590.1	-0.79	29.70	0.6083
3	0.4	130.1	590.1	-0.79	29.70	0.6325
4	0.41	130.1	590.1	-0.79	29.70	0.6403
5	0.42	130.1	590.1	-0.79	29.70	0.6481
6	0.36	130.1	590.1	-0.79	29.70	0.6
7	0.51	130.1	590.1	-0.79	29.70	0.7141
8	0.62	130.1	590.1	-0.79	29.70	0.7874
9	0.49	130.1	590.1	-0.79	29.70	0.7
10	0.5	130.1	590.1	-0.79	29.70	0.7071
11	0.41	130.1	590.1	-0.79	29.70	0.6403
12	0.36	130.1	590.1	-0.79	29.70	0.6
13	0.4	130.1	590.1	-0.79	29.70	0.6325
14	0.32	130.1	590.1	-0.79	29.70	0.5657
15	0.48	130.1	590.1	-0.79	29.70	0.6928
16	0.58	130.1	590.1	-0.79	29.70	0.7616
AVG.		130.1	590.1		29.70	0.6635

wet bulb temp. (deg F): 124.70

stack vapor pressure: 3.9216231

%H2O: 13.025587

Molecular Density: 0.8697441

Molecular weight of dry gas: 28.7704 lb/lb mole dry

Molecular weight of wet stack gas: 27.367492 lb/lb mole wet

Stack gas velocity at stack conditions: 2436.11765 afpm

Stack gas flow rate at std. conditions: 2627.77316 dscfm

Stack gas flow rate at stack conditions: 3401.45904 acfm

**Average stack gas flow rate at standard conditions:**

**2576 dscfm**

**Average stack gas flow rate at stack conditions:**

**3337 acfm**

**Avg % Mois**

13.16

**Average Velocity**

2389.83

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/5/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: BSU vent #2

Run Number: 1  
 Start Time: 1900 Stop Time: 1500  
 Ambient Temp at Start: 60 Ambient Temp at Stop: 60  
 Barometric Pressure: 29.76

Leak Test

Time: 1355 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1501 Final Measurement (in Hga): 0 on DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample Flow Rate:  
 1. 71 2. 76 3. 78 4. 80 5. 81 Avg: 25.40  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM Temp  
DGM Pressure

Rotameter Readings

Time: 1410 Flow: 3.941  
 Time: 1420 Flow: 7.991  
 Time: 1430 Flow: 12.044  
 Time: 1440 Flow: 15.973  
 Time: 1450 Flow: 19.875  
 Time: 1500 Flow: 29.007

QA/QC Measures

Train Spike Conducted? Yes No  
 Duplicate Conducted? Yes No  
 Spiked Duplicate Made? Yes No  
 Field Blank Made? Yes No  
 Field Spike Made? Yes No

Sample Bottle Weight(s):

Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments

DGM used for sample volume collection

Bottle # 4

Figure 2. Field Sampling Data Sheet

Dry Bulb	Wet bulb
131	127.4
2129.2	123.8
Avg 130.1	125.6

Box #2 Y2101

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/5/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: BSU vent #2

Run Number: 2  
 Start Time: 1510 Stop Time: 1610  
 Ambient Temp at Start: 60 Ambient Temp at Stop: 56  
 Barometric Pressure: 29.76

Leak Test

Time: 1505 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1612 Final Measurement (in Hga): 0 on DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes  No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample FlowRate:  
 1. 28 2. 76 3. 76 4. 76 5. 76 Avg: 247 c  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM  
Temp  
DGM  
Pressure

Rotamejer Readings	QA/QC Measures
Time: <u>1520</u> Flow: <u>4.139</u>	Train Spike Conducted? Yes No
Time: <u>1530</u> Flow: <u>8.002</u>	Duplicate Conducted? Yes No
Time: <u>1540</u> Flow: <u>11.905</u>	Spiked Duplicate Made? Yes No
Time: <u>1550</u> Flow: <u>16.157</u>	Field Blank Made? Yes No
Time: <u>1600</u> Flow: <u>20.009</u>	Field Spike Made? Yes No
Time: <u>1610</u> Flow: <u>24.051</u>	

Sample Bottle Weight(s):  
 Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments  
DGM used for sample volume collection

CR  
Bottle # 3 5

Bottle # 7

Figure 2. Field Sampling Data Sheet

Dry Bulb	Wet bulb
<u>127.9</u>	<u>123.8</u>
<u>2.129.2</u>	<u>125.6</u>
Avg <u>128.6</u>	<u>124.7</u>

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/5/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: BSW vent #2

Run Number: 3  
 Start Time: 1620 Stop Time: 1720  
 Ambient Temp at Start: 54 Ambient Temp at Stop: 55  
 Barometric Pressure: 29.76

**Leak Test**  
 Time: 1615 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1725 Final Measurement (in Hga): 0 on DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes  No

**System Flow Rate Measurement**  
 Average of 5 flow measurements for Pre-Sample FlowRate:  
 1. 71 2. 74 3. 76 4. 25 5. 26 Avg: 24.0  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM  
Temp  
DGM  
Pressure

Rotameter Readings	QA/QC Measures
Time: <u>1630</u> Flow: <u>3.859</u>	Train Spike Conducted? Yes No
Time: <u>1640</u> Flow: <u>7.920</u>	Duplicate Conducted? Yes No
Time: <u>1650</u> Flow: <u>11.918</u>	Spiked Duplicate Made? Yes No
Time: <u>1700</u> Flow: <u>16.1009</u>	Field Blank Made? Yes No
Time: <u>1710</u> Flow: <u>20.0500</u>	Field Spike Made? Yes No
Time: <u>1720</u> Flow: <u>29.1260</u>	

**Sample Bottle Weight(s):**  
 Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

**Notes/Comments**  
DGM used for sample volume collection

Bottle #5

Box #2

Figure 2. Field Sampling Data Sheet

Bk	Dry Bulb	Wet bulb
1	<u>142.2</u> <u>124.2</u>	<u>123.8</u>
2	<u>131</u>	<u>125.6</u>
Avg	<u>130.1</u>	<u>124.7</u>

## GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant: GP-Toledo		Location: Toledo, OR		Source: <del>#2</del> BSW Combined Vent	
Date: 11-5-14		Operator: Homer		Run No.: 1 & 2	
Barometric Press: 29.76		Reading Location: Lab		Ambient Temp: 55	
Elevation: 0		Elevation Corr.: 0		Corr. Bar. Press.: 0	
Avg. wet bulb temp (F): 127.4		% O2		% CO2	
Pitot tube ID #: 4" Stype		Pitot Cp: 0.84		Last Calibration:	
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check	
				Vel. At 0 reference	Angle to get 0 Flow
1	.50	131	-.74	0	0
2	.52			0	0
3	.53			0	0
4	.29			0	0
5	.31			.15	5
6	.38			0	0
7	.40			0	0
8	.34			0	0
9	.38			0	0
10	.41			.09	3
11	.35			.06	4
12	.27			0	0
13	.51			0	0
14	.55			0	0
15	.44			0	0
16	.53			0	0
<hr/>					
1	.51	127.4	-.77		
2	.54				
3	.55				
4	.31				
5	.31				
6	.33				
7	.41				
8	.36				

RUN #1

RUN #2

Run 2  
 Dry 127.4 | 129.2  
 Wet 123.8 | 125.6

Run 3  
 Dry 129.2 | 131  
 Wet 123.8 | 125.6

Run 1  
 Dry 131 | 129.2  
 Wet 127.4 | 123.8



## GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant: GP-Toledo		Location: Toledo, OR		Source: <del>#1248</del> BSW Combined Vent	
Date: 11-5-14 11/01/2000		Operator: Homer		Run No.: 2&3	
Barometric Press. 29.76		Reading Location: Lab		Ambient Temp: 55 0	
Elevation: 0		Elevation Corr.: 0		Corr. Bar. Press.: 0	
Avg. wet bulb temp (F): 0		% O2:		% CO2:	
Pitot tube ID #: 4' Stype		Pitot Cp: 0.84		Last Calibration:	
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check	
				Vel. At 0 reference	Angle to get 0 Flow
9	.51				
10	.50				
11	.50				
12	.36				
13	.25				
14	.39				
15	.46				
16	.47				
1	.47	130	-.79		
2	.37				
3	.40				
4	.41				
5	.42				
6	.36				
7	.51				
8	.62				
9	.49				
10	.50				
11	.41				
12	.36				
13	.40				
14	.32				
15	.48				
16	.58				

RUN #2

RUN #3

## TRAVERSE POINT LOCATION WORKSHEET METHOD 1

**DATA**

**STACK CROSS SECTION DIAGRAM**

Plant:	GP-Toledo <small>#2 BSVV Combined Vent</small>	Location:	Toledo, OR	See Diagram	
Source:		Operator:	Homer		
Date		Port Depth(in.):	1.5		
Stack Dia. (in.)	16	Stack Area (ft2):	1.40		
Distance to disturbance:		Upstream(ft):	Downstream(ft):		
# of traverse points required:		16			
Traverse point #	% of Stack Dia.	Stack Dia.	% of Stack Dia. X Stack Dia.	Port Depth	Taverse Point Location
1	0.032	16	0.5	1.5	2.01
2	0.105	16	1.7	1.5	3.18
3	0.194	16	3.1	1.5	4.60
4	0.323	16	5.2	1.5	6.67
5	0.677	16	10.8	1.5	12.33
6	0.806	16	12.9	1.5	14.40
7	0.895	16	14.3	1.5	15.82
8	0.968	16	15.5	1.5	16.99

**NOTES:** \_\_\_\_\_

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EMISSION RATE

Georgia Pacific				
Karft BSW #3 Combined Vent				
Emissions Rates Calculations				
5-Nov-14				
	<b>Karft BSW #3 Combined Vent</b>			
	Run #1	Run #2	Run #3	Average
	09:55-10:55	11:00-12:00	12:05-13:05	
<b>MeOH (ppm)</b>	251.0819	298.5045	273.1132	274.2332
Stack Flow:				
acfm:	865	1226	1252	1114
dscfm:	627	888	884	799
Pulp Production:				
ODT/day:	399.00	399.00	399.00	399.00
<b>MeOH Emissions at Standard Conditions:</b>				
lb/hr:	0.78552	1.32261	1.20464	1.10426
lb/day:	18.85249	31.74256	28.91137	26.50214
lb/ODT:	0.04725	0.07956	0.07246	0.06642

MeOH concentration

Georgia Pacific				
Karft BSW #3 Combined Vent				
11/5/2014				
Total MeOH catch & DGM volume				
<b>Run 1</b>				
DGM Volume (l)	23.995			
Meter Y	1.01			
DGM Temp (C)	21.7			
Baro Pressure	29.76			
DGM Volume (dsc)	23.97			
		Total MeOH catch (mirco g)		8020
MW of MeOH	32.04	Correction Factor		1
MeOH (ppmvd)	251.08188			
<b>Run 2</b>				
DGM Volume (l)	24.036			
Meter Y	1.01			
DGM Temp (C)	25.8			
Baro Pressure	29.76			
DGM Volume (dsc)	23.68			
		Total MeOH catch (mirco g)		9420
MW of MeOH	32.04	Correction Factor		1
MeOH (ppmvd)	298.50453			
<b>Run 3</b>				
DGM Volume (l)	23.988			
Meter Y	1.01			
DGM Temp (C)	27.6			
Baro Pressure	29.76			
DGM Volume (dsc)	23.49			
		Total MeOH catch (mirco g)		8550
MW of MeOH	32.04	Correction Factor		1
MeOH (ppmvd)	273.11319			

Georgia Pacific  
 Karft BSW #3 Combined Vent  
 Stack Gas Flow Rate Data and Calculations  
 5-Nov-14

Run #1

Barometric Pressure: 29.76  
 Stack Diameter or Dimensions (in.): 16  
 Cross Sectional Area (sq ft): 1.3962622  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.06	141.6	601.6	-0.01	29.76	0.2449
2	0.06	141.6	601.6	-0.01	29.76	0.2449
3	0.04	141.6	601.6	-0.01	29.76	0.2
4	0.03	141.6	601.6	-0.01	29.76	0.1732
5	0.04	141.6	601.6	-0.01	29.76	0.2
6	0.02	141.6	601.6	-0.01	29.76	0.1414
7	0.02	141.6	601.6	-0.01	29.76	0.1414
8	0.01	141.6	601.6	-0.01	29.76	0.1
9	0.01	141.6	601.6	-0.01	29.76	0.1
10	0.01	141.6	601.6	-0.01	29.76	0.1
11	0.01	141.6	601.6	-0.01	29.76	0.1
12	0.02	141.6	601.6	-0.01	29.76	0.1414
13	0.03	141.6	601.6	-0.01	29.76	0.1732
14	0.03	141.6	601.6	-0.01	29.76	0.1732
15	0.03	141.6	601.6	-0.01	29.76	0.1732
16	0.06	141.6	601.6	-0.01	29.76	0.2449
AVG.		141.60	601.60		29.76	0.1657

wet bulb temp. (deg F): 134.60  
 stack vapor pressure: 5.1325697  
 %H2O: 17.026291  
 Molecular Density: 0.8297371  
 Molecular weight of dry gas: 28.6624 lb/lb mole dry  
 Molecular weight of wet stack gas: 26.846989 lb/lb mole wet  
 Stack gas velocity at stack conditions: 619.774873 afpm  
 Stack gas flow rate at std. conditions: 626.798805 dscfm  
 Stack gas flow rate at stack conditions: 865.368242 acfm

Georgia Pacific  
 Karft BSW #3 Combined Vent  
 Stack Gas Flow Rate Data and Calculations  
 5-Nov-14

Run #2

Barometric Pressure: 29.76  
 Stack Diameter or Dimensions (in.): 16  
 Cross Sectional Area (sq ft): 1.3962622  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.1	141.6	601.6	-0.01	29.76	0.3162
2	0.07	141.6	601.6	-0.01	29.76	0.2646
3	0.04	141.6	601.6	-0.01	29.76	0.2
4	0.05	141.6	601.6	-0.01	29.76	0.2236
5	0.06	141.6	601.6	-0.01	29.76	0.2449
6	0.08	141.6	601.6	-0.01	29.76	0.2828
7	0.01	141.6	601.6	-0.01	29.76	0.1
8	0.01	141.6	601.6	-0.01	29.76	0.1
9	0.06	141.6	601.6	-0.01	29.76	0.2449
10	0.07	141.6	601.6	-0.01	29.76	0.2646
11	0.08	141.6	601.6	-0.01	29.76	0.2828
12	0.05	141.6	601.6	-0.01	29.76	0.2236
13	0.06	141.6	601.6	-0.01	29.76	0.2449
14	0.07	141.6	601.6	-0.01	29.76	0.2646
15	0.04	141.6	601.6	-0.01	29.76	0.2
16	0.08	141.6	601.6	-0.01	29.76	0.2828
AVG.		141.6	601.6		29.76	0.2338

wet bulb temp. (deg F): 134.60  
 stack vapor pressure: 5.1325697  
 %H2O: 17.026291  
 Molecular Density: 0.8297371

Molecular weight of dry gas: 28.4004 lb/lb mole dry  
 Molecular weight of wet stack gas: 26.629598 lb/lb mole wet  
 Stack gas velocity at stack conditions: 877.751734 afpm  
 Stack gas flow rate at std. conditions: 887.699326 dscfm  
 Stack gas flow rate at stack conditions: 1225.57159 acfm

Georgia Pacific  
 Karft BSW #3 Combined Vent  
 Stack Gas Flow Rate Data and Calculations  
 5-Nov-14

Run #3

Barometric Pressure: 29.76  
 Stack Diameter or Dimensions (in.): 16  
 Cross Sectional Area (sq ft): 1.3962622  
 Pitot Tube Avg. Coeff.: 0.84

Traverse Point	Velocity Head ^P (in. H2O)	Stack Temperature (deg F)	Stack Temperature (deg R)	Stack Static Pressure (in. H2O)	Stack Static Pressure (in Hg.)	Sqrt ^P
1	0.08	140.6	600.6	-0.01	29.76	0.2828
2	0.06	140.6	600.6	-0.01	29.76	0.2449
3	0.05	140.6	600.6	-0.01	29.76	0.2236
4	0.06	140.6	600.6	-0.01	29.76	0.2449
5	0.05	140.6	600.6	-0.01	29.76	0.2236
6	0.04	140.6	600.6	-0.01	29.76	0.2
7	0.04	140.6	600.6	-0.01	29.76	0.2
8	0.04	140.6	600.6	-0.01	29.76	0.2
9	0.06	140.6	600.6	-0.01	29.76	0.2449
10	0.04	140.6	600.6	-0.01	29.76	0.2
11	0.05	140.6	600.6	-0.01	29.76	0.2236
12	0.08	140.6	600.6	-0.01	29.76	0.2828
13	0.08	140.6	600.6	-0.01	29.76	0.2828
14	0.06	140.6	600.6	-0.01	29.76	0.2449
15	0.07	140.6	600.6	-0.01	29.76	0.2646
16	0.06	140.6	600.6	-0.01	29.76	0.2449
AVG.		140.6	600.6		29.76	0.238

wet bulb temp. (deg F): 139.00  
 stack vapor pressure: 5.7601395  
 %H2O: 19.306524  
 Molecular Density: 0.8069348  
 Molecular weight of dry gas: 28.4012 lb/lb mole dry  
 Molecular weight of wet stack gas: 26.39309 lb/lb mole wet  
 Stack gas velocity at stack conditions: 896.987301 afpm  
 Stack gas flow rate at std. conditions: 883.691965 dscfm  
 Stack gas flow rate at stack conditions: 1252.42948 acfm

**Average stack gas flow rate at standard conditions: 799 dscfm**  
**Average stack gas flow rate at stack conditions: 1114 acfm**  
**Avg % Mois 17.79 Average Velocity 798.17**

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/5/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: BSW vent #3

Run Number: 1  
 Start Time: 0955 Stop Time: 1055  
 Ambient Temp at Start: 58 Ambient Temp at Stop: 58  
 Barometric Pressure: 29.70

Leak Test

Time: 945 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1055 Final Measurement (in Hga): 0 on DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample Flow Rate:  
 1. 65 2. 68 3. 71 4. 75 5. 76 Avg: 71 = 2176  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM Temp  
 DGM Pressure

Rotameter Readings

Time: 1005 Flow: 4.154  
 Time: 1015 Flow: 8.006  
 Time: 1025 Flow: 11.802  
 Time: 1035 Flow: 16.083  
 Time: 1045 Flow: 20.017  
 Time: 1055 Flow: 23.995

QA/QC Measures

Train Spike Conducted? Yes No  
 Duplicate Conducted? Yes No  
 Spiked Duplicate Made? Yes No  
 Field Blank Made? Yes No  
 Field Spike Made? Yes No

Sample Bottle Weight(s):

Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments

DGM used for sample volume collection

Bottle #1

Box #1 41.01

Figure 2. Field Sampling Data Sheet

	Dry Bulb	Wet bulb
1	141.8	131
2	141.4	138.2
Avg	141.6	134.6



NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/5/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: BSW Vent #3

Run Number: 2  
 Start Time: 1100 Stop Time: 1200  
 Ambient Temp at Start: 58 Ambient Temp at Stop: 60  
 Barometric Pressure: 29.76

Leak Test

Time: 1158 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1201 Final Measurement (in Hga): 0 on DGM, no bubbles

Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.

Meets Criteria? Yes No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample FlowRate:  
 1. 78 2. 78 3. 78 4. 78 5. 80 Avg: 75.8  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM  
Temp  
DGM  
Pressure

Rotameter Readings		QA/QC Measures	
Time: <u>1110</u>	Flow: <u>3.919</u>	Train Spike Conducted?	Yes No
Time: <u>1120</u>	Flow: <u>8.037</u>	Duplicate Conducted?	Yes No
Time: <u>1130</u>	Flow: <u>11.817</u>	Spiked Duplicate Made?	Yes No
Time: <u>1140</u>	Flow: <u>16.135</u>	Field Blank Made?	Yes No
Time: <u>1150</u>	Flow: <u>19.815</u>	Field Spike Made?	Yes No
Time: <u>1200</u>	Flow: <u>24.036</u>		

Sample Bottle Weight(s):  
 Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments  
DGM used for sample volume collection

Bottle # 2

Figure 2. Field Sampling Data Sheet

Dry Bulb	Wet bulb
<u>147.2</u>	<u>147.2</u>
<u>140</u>	<u>141.8</u>

Box #2

Aug Dry 147.2  
 140.9 wet

NCASI Chilled Impinger/Silica Gel Tube Test Method At Pulp Mill Sources For Methanol, Acetone, Acetaldehyde, Methyl Ethyl Ketone And Formaldehyde

Field Sampling Data Sheet

Mill Name: GP-Toledo Date: 11/5/14  
 City, State: Toledo, OR Sampler's Name: Homer  
 Source Name/Description: RSW vent #3

Run Number: 3  
 Start Time: 1205 Stop Time: 1305  
 Ambient Temp at Start: 60 Ambient Temp at Stop: 60  
 Barometric Pressure: 29.76

Leak Test

Time: 1203 Initial Measurement (in Hga): 0 on DGM, no bubbles  
 Time: 1307 Final Measurement (in Hga): 0 on DGM, no bubbles  
 Leak Check Criteria- Must not lose more than 1 inch of Hg (vacuum) in 2 minutes.  
 Meets Criteria? Yes No

System Flow Rate Measurement

Average of 5 flow measurements for Pre-Sample FlowRate:  
 1. 77 2. 81 3. 82 4. 83 5. 83 Avg: 27.60  
 Average of 5 flow measurements for Post-Sample Flow Rate:  
 1. 10 2. 10 3. 10 4. 10 5. 10 Avg: 10  
 Overall Average Sample Flow Rate: (indicate units!) Avg: \_\_\_\_\_

DGM  
Temp  
DGM  
Pressure

Rotameter Readings	QA/QC Measures
Time: <u>1215</u> Flow: <u>4.055</u>	Train Spike Conducted? Yes No
Time: <u>1225</u> Flow: <u>8.095</u>	Duplicate Conducted? Yes No
Time: <u>1235</u> Flow: <u>12.07</u>	Spiked Duplicate Made? Yes No
Time: <u>1245</u> Flow: <u>16.214</u>	Field Blank Made? Yes No
Time: <u>1255</u> Flow: <u>9.913</u>	Field Spike Made? Yes No
Time: <u>1305</u> Flow: <u>23.988</u>	

Sample Bottle Weight(s):  
 Bottle 1: Initial Weight: \_\_\_\_\_ Bottle 2: Initial Weight: \_\_\_\_\_  
 Final Weight: \_\_\_\_\_ Final Weight: \_\_\_\_\_

Notes/Comments  
DGM used for sample volume collection

Bottle #3

Box #2

Figure 2. Field Sampling Data Sheet

Dry Bulb	Wet bulb
<u>190.00</u>	<u>136.4</u>
<u>219.8</u>	<u>141.6</u>

August 1998  
 14016 139

# GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant GP-Toledo		Location: Toledo, OR		#3 BSW Combined Vent		
Date 11-5-14		Operator: Homer		Run No.: *		
Barometric Press. 29.76		Reading Location: Lab		Ambient Temp: 55°		
Elevation: 0		Elevation Corr.: 0		Corr. Bar. Press.: 0		
Avg. wet bulb temp (F) 13		% O2		% CO2:		
Pitot tube ID #: 4' Stype		Pitot Cp: .84		Last Calibration:		
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check		
				Vel. At 0 reference	Angle to get 0 Flow	
RUN #1	.06 <del>.05</del> <del>.05</del> BE	141.8	-.01	.02 <del>.02</del> <del>.05</del> BE	30 15	
	.06			0	0	
	.04			0	0	
	.03			0	0	
	.04			0	0	
	.02			0	0	
	.02			0	0	
	.01			0	0	
	.01			0	0	
	.01			0	0	
	.01			0	0	
	.02			0	0	
	.03			0	0	
	.03			0	0	
	.06		145.4		0	0
	RUN #2	.10	147.2	-.01		
.07						
.04						
.05						
.06						
.08						
.01						
.01						

**GAS VELOCITY AND VOLUMETRIC FLOW FORM  
METHOD 2**

Page 2

Plant GP-Toledo		Location: Toledo, OR		Source: #3 BSW Combined Vent	
Date 11-5-14 11/07/2000		Operator: Homer		Run No.: 2&3	
Barometric Press. 29.76		0 Reading Location: Lab		Ambient Temp: 55 0	
Elevation: 0		Elevation Corr.: 0		Corr. Bar. Press.: 0	
Avg. wet bulb temp (F) 0		% O2		% CO2:	
Pitot tube ID #: 4' Stype		Pitot Cp: 0		Last Calibration:	
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check	
				Vel. At 0 reference	Angle to get 0 Flow
9	.06		-.01		
10	.07				
11	.08				
12	.05				
13	.06				
14	.07				
15	.04				
16	.08	147.2			
1	.08	140	-.01		
2	.06				
3	.05				
4	.06				
5	.05				
6	.04				
7	.04				
8	.04				
9	.06	141.80	-.01		
10	.04				
11	.05				
12	.08				
13	.08				
14	.06				
15	.07				
16	.06				

RUN #2

RUN #3

## TRAVERSE POINT LOCATION WORKSHEET METHOD 1

### DATA

### STACK CROSS SECTION DIAGRAM

Plant: GP-Toledo <small>#3 BSW Combined Vent</small>		Location: Toledo, OR		See Diagram	
Source:		Operator: Homer			
Date		Port Depth(in.): 0.125			
Stack Dia. (in.) 16		Stack Area (ft2): 1.40			
Distance to disturbance: Upstream(ft):                      Downstream(ft):					
# of traverse points required: 16					
Traverse point #	% of Stack Dia.	Stack Dia.	% of Stack Dia. X Stack Dia.	Port Depth	Taverse Point Location
1	0.032	16	0.5	0.125	0.64
2	0.105	16	1.7	0.125	1.81
3	0.194	16	3.1	0.125	3.23
4	0.323	16	5.2	0.125	5.29
5	0.677	16	10.8	0.125	10.96
6	0.806	16	12.9	0.125	13.02
7	0.895	16	14.3	0.125	14.45
8	0.968	16	15.5	0.125	15.61

**NOTES:** \_\_\_\_\_

\_\_\_\_\_

# GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant: GP-Toledo		Location: Toledo, OR		Source: #1 BSW Combined Vent	
Date: 11/6/2014		Operator: Homer		Run No.: 1 & 2	
Barometric Press.		Reading Location: Lab		Ambient Temp:	
Elevation: 0		Elevation Corr.: 0		Corr. Bar. Press.: 0	
Avg. wet bulb temp (F)		% O2		% CO2:	
Pitot tube ID #: 4' Stype		Pitot Cp:		Last Calibration:	
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check	
				Vel. At 0 reference	Angle to get 0 Flow
1					
2					
3					
4					
5	Flow on #1 BSW is "backward" toward the #2				
6	Wester head. This was verified by inserting reaction tape and				
7	seeing it flutter toward the head. Therefore source was not				
8	tested and emissions assumed to be 0.				
9					
10					
11	The reverse flow was checked during each run				
12					
13					
14					
15					
16					
1					
2					
3	Reverse flow				
4					
5					
6					
7					
8					

RUN #1

RUN #2

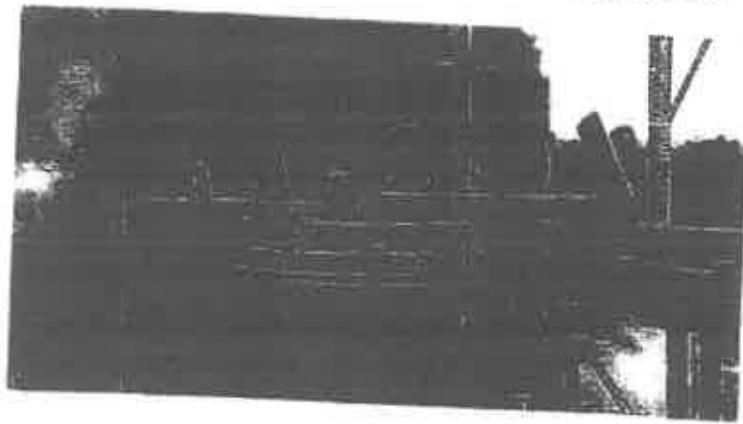
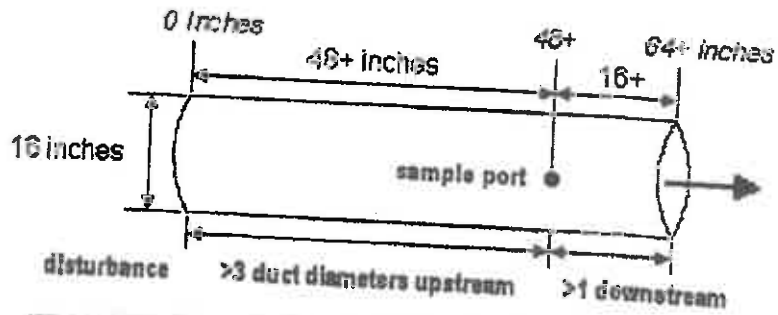
## GAS VELOCITY AND VOLUMETRIC FLOW FORM METHOD 2

Plant		GP-Toledo	Location: Toledo, OR		Source: #1 BSW Combined Vent	
Date		11/6/2014	Operator: Homer		Run No.: 2&3	
Barometric Press.		0	Reading Location: Lab		Ambient Temp: 0	
Elevation:		0	Elevation Corr.:		0	Corr. Bar. Press.: 0
Avg. wet bulb temp (F)		0	% O2		% CO2:	
Pitot tube ID #:		4' Stype	Pitot Cp:		0	Last Calibration: 1/0/1900
Traverse Point #	Velocity Head	Stack Temp (F)	Static Press.	Cyclonic Flow Check		
				Vel. At 0 reference	Angle to get 0 Flow	
9						
10						
11						
12						
13		↑ ↑				
14						
15						
16						
1						
2						
3						
4						
5						
6						
7	Reverse Flow					
8						
9						
10						
11						
12						
13						
14						
15						
16						

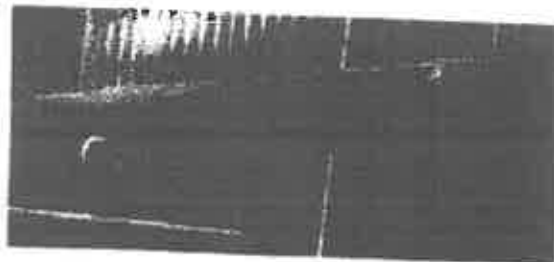
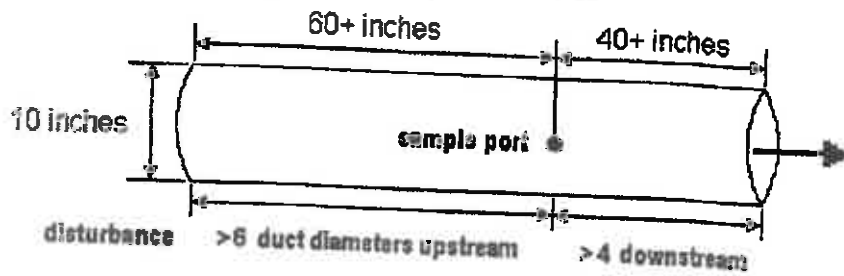
RUN #2

RUN #3

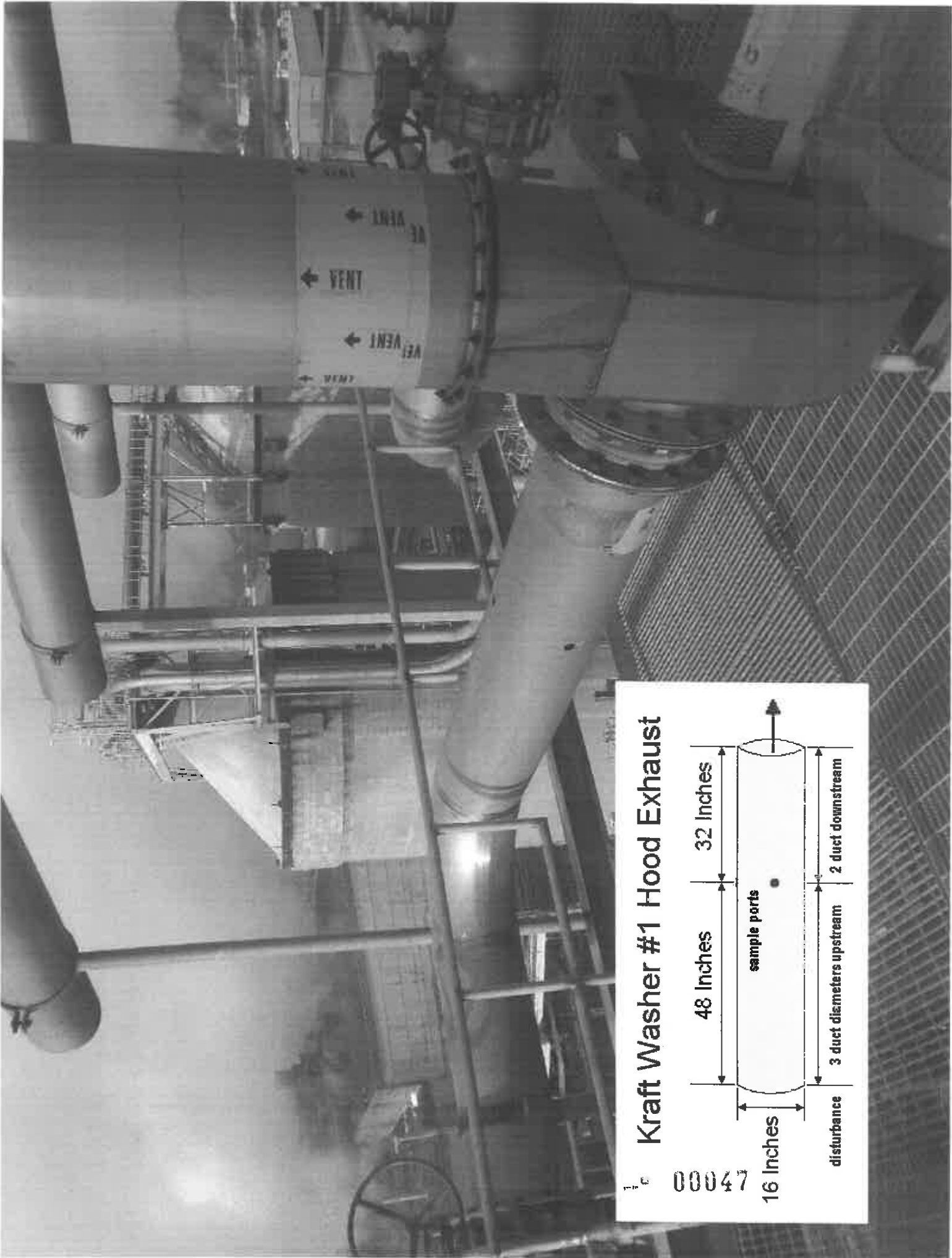
### Kraft Washer #1 – Foam Breaker Vent



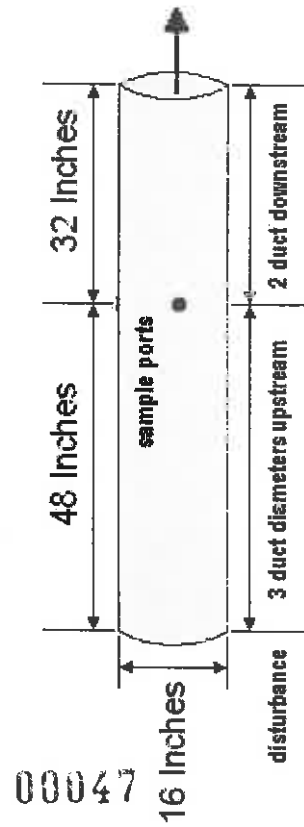
### Kraft Washer #1 – Vacuum Pump Exhaust



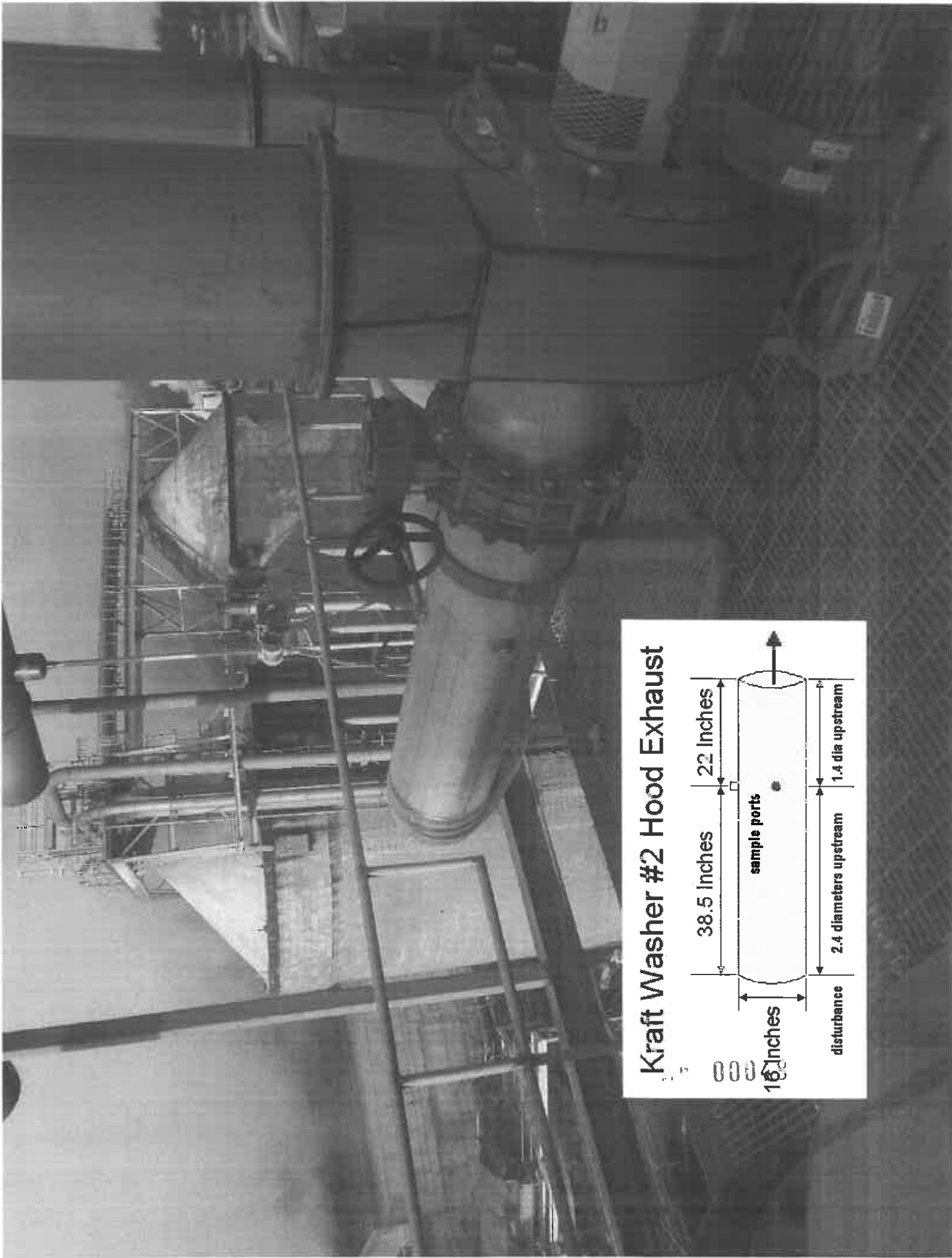




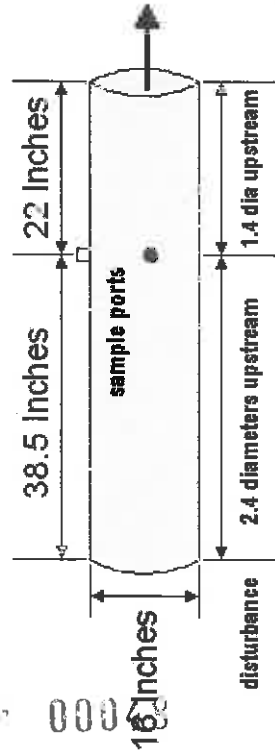
### Kraft Washer #1 Hood Exhaust

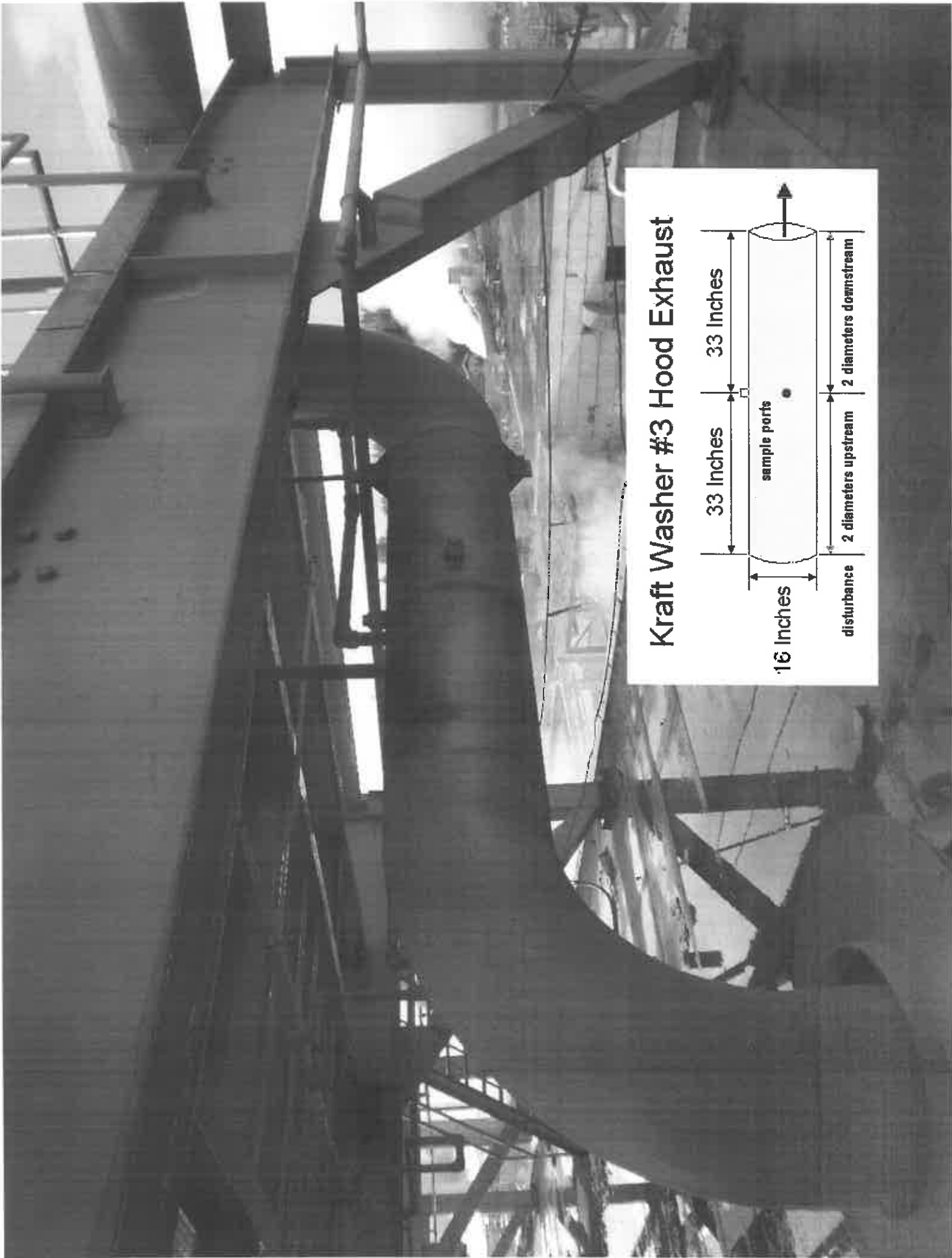


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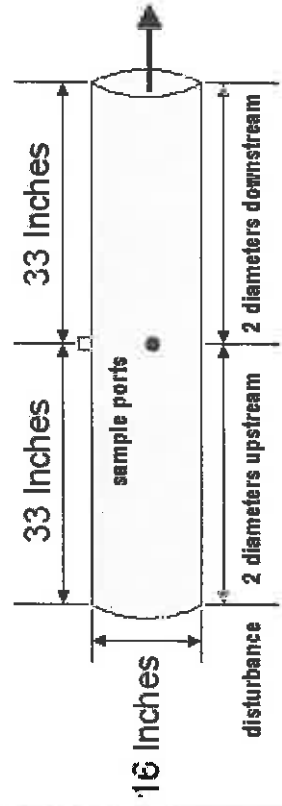


### Kraft Washer #2 Hood Exhaust





### Kraft Washer #3 Hood Exhaust



# BIGHORN ENVIRONMENTAL - FIELD DATA CALIBRATION SHEET

Plant Name	Date	QA Checks	
Source	Project #	Gas Divider	Leak Check
Stack Diameter	Probe Length	NO2 Conv	Response Time
		NA	2:00

Plant Name	Date	QA Checks	
Source	Project #	Gas Divider	Leak Check
Stack Diameter	Probe Length	NO2 Conv	Response Time
		NA	2:00

Cylinder ID	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	NO <sub>x</sub> (ppm)	CO (ppm)	SO <sub>2</sub> (ppm)	VOC (as Propane)	H <sub>2</sub> S (ppm)
	Mid						
	High	110%					

Analyzer Calibration	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	NO <sub>x</sub> (ppm)	CO (ppm)	SO <sub>2</sub> (ppm)	VOC (as Propane)	H <sub>2</sub> S (ppm)
	C <sub>v</sub>	C <sub>v</sub>	C <sub>dir</sub>	C <sub>dir</sub>	C <sub>v</sub>	C <sub>dir</sub>	C <sub>v</sub>
Zero (UPN)	0	0	0	0	0	0	0
Low							
Mid	9.09	9.76	2.22	2.75			
Span	20.93	21.01	4.23	4.23			

All zero values from Grade 5.0 UPN

Run Data	Run #1	Run #2	Run #3	Run #4	Run #5	Run #6	Run #7	Run #8	Run #9	Run #10	Run #11	Run #12	Run #13	Run #14	Run #15	Run #16	Run #17
Start Time	9:10	10:35	11:55														
End Time	10:10	11:35	12:55														
O <sub>2</sub> Run Average																	
CO <sub>2</sub> Run Average																	
NO <sub>x</sub> Run average																	
CO Run Average																	
SO <sub>2</sub> Run Average																	
TRS Run Average																	
VOC Run Average																	

Gas Checks	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	NO <sub>x</sub> (ppm)	CO (ppm)	SO <sub>2</sub> (ppm)	VOC (as Propane)	H <sub>2</sub> S (ppm)
	Zero	Zero	Zero	Zero	Zero	Zero	Zero
Pre Run #1	-1.10	-1.10	2.25				
Post #1/Pre #2	-1.12	-1.09	2.27				
Post #2/Pre #3							
Post #3/Pre #4							
Post #4/Pre #5							
Post #5/Pre #6							
Post #6/Pre #7							
Post #7/Pre #8							
Post #8/Pre #9							
Post #9/Pre #10							
Post #10/Pre #11							
Post #11/Pre #12							
Post #12/Pre #13							
Post #13/Pre #14							
Post #14/Pre #15							
Post #15/Pre #16							
Post #16							

All zero values from Grade 5.0 UPN

# BIGHORN ENVIRONMENTAL - FIELD DATA CALIBRATION SHEET

Plant Name <i>CP - Dakota</i>	Date <i>11/5/15</i>	QA Checks	
Source <i>usbs</i>	Project # <i>2014</i>	Gas Divider <input checked="" type="checkbox"/>	NO2 Conv <i>NA</i>
Stack Diameter <i>16</i>	Probe Length <i>8</i>	Leak Check <i>#2 BSU</i>	Response Time <i>2:00</i>

Cylinder ID	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	NO <sub>x</sub> (ppm)	CO (ppm)	SO <sub>2</sub> (ppm)	VOC (as Propane)	H <sub>2</sub> S (ppm)
Mid			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
High	<i>20.93</i>	<i>21.65</i>					

Analyzer Calibration	O <sub>2</sub> (%)		CO <sub>2</sub> (%)		NO <sub>x</sub> (ppm)		CO (ppm)		SO <sub>2</sub> (ppm)		VOC (as Propane)		H <sub>2</sub> S (ppm)	
	C <sub>v</sub>	C <sub>dir</sub>	C <sub>v</sub>	C <sub>dir</sub>	C <sub>v</sub>	C <sub>dir</sub>	C <sub>v</sub>	C <sub>dir</sub>	C <sub>v</sub>	C <sub>dir</sub>	C <sub>v</sub>	C <sub>dir</sub>	C <sub>v</sub>	C <sub>dir</sub>
Zero (UPN)	0	-11	0	-15										
Low														
Mid	<i>6.47</i>	<i>10.79</i>	<i>7.16</i>	<i>2.02</i>										
Span	<i>18.84</i>	<i>19.04</i>	<i>6.33</i>	<i>9.43</i>										

All zero values from Grade 5.0 UPN

Run Data	Run #1		Run #2		Run #3		Run #4		Run #5		Run #6		Run #7		Run #8		Run #9		Run #10		Run #11		Run #12		Run #13		Run #14		Run #15		Run #16		Run #17	
	Start Time	End Time	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	NO <sub>x</sub> (ppm)	CO (ppm)	SO <sub>2</sub> (ppm)	VOC (as Propane)	H <sub>2</sub> S (ppm)																									
	<i>09:52</i>	<i>11:51</i>	<i>1100</i>	<i>1705</i>	<i>1510</i>	<i>1619</i>																												
	<i>10:51</i>	<i>11:51</i>	<i>1304</i>	<i>1500</i>	<i>1609</i>	<i>1710</i>																												

Bags Checks	O <sub>2</sub> (%)		CO <sub>2</sub> (%)		NO <sub>x</sub> (ppm)		CO (ppm)		SO <sub>2</sub> (ppm)		VOC (as Propane)		H <sub>2</sub> S (ppm)	
	Zero	Upscale	Zero	Upscale	Zero	Upscale	Zero	Upscale	Zero	Upscale	Zero	Upscale	Zero	Upscale
Pre-Run #1	<i>-1.11</i>	<i>18.93</i>	<i>-1.13</i>	<i>2.07</i>										
Post #1/Pre #2	<i>-1.12</i>	<i>18.99</i>	<i>-1.09</i>	<i>2.06</i>										
Post #2/Pre #3														
Post #3/Pre #4	<i>-1.12</i>	<i>18.99</i>	<i>-1.09</i>	<i>2.06</i>										
Post #4/Pre #5	<i>-1.11</i>	<i>18.99</i>	<i>-1.12</i>	<i>2.06</i>										
Post #5/Pre #6														
Post #6/Pre #7														
Post #7/Pre #8														
Post #8/Pre #9														
Post #9/Pre #10														
Post #10/Pre #11														
Post #11/Pre #12														
Post #12/Pre #13														
Post #13/Pre #14														
Post #14/Pre #15														
Post #15/Pre #16														
Post #16														

All zero values from Grade 5.0 UPN

#2 BSU  
#2 BSN

#1, #2 and #3 BSW				Run Averages					
Run	Start	End	Minutes	O2	CO2				
1	11/5/2014 9:55	10:54	60	9.98	-0.11	#3 BSW, Run 1			
2	11/5/2014 11:00	11:59	60	10.01	-0.11	#3 BSW, Run 2			
3	11/5/2014 12:05	13:04	60	10.03	-0.11	#3 BSW, Run 3			
4	11/5/2014 14:00	14:59	60	19.49	-0.07	#2 BSW, Run1			
5	11/5/2014 15:10	16:09	60	19.22	-0.06	#2 BSW, Run2			
6	11/5/2014 16:19	17:18	60	19.26	-0.05	#2 BSW, Run3			
7	11/6/2014 9:10	10:09	60	17.70	-0.10	#1 BSW, Run 1			
8	11/6/2014 10:35	11:34	60	17.58	-0.09	#1 BSW, Run 2			
9	11/6/2014 11:55	12:54	60	17.70	-0.09	#1 BSW, Run 3			

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	6:30	20.9	-0.06
11/5/2014	6:31	20.9	-0.06
11/5/2014	6:32	20.9	-0.06
11/5/2014	6:33	20.91	-0.06
11/5/2014	6:34	20.9	-0.06
11/5/2014	6:35	20.9	-0.06
11/5/2014	6:36	20.9	-0.07
11/5/2014	6:37	20.9	-0.06
11/5/2014	6:38	20.9	-0.06
11/5/2014	6:39	16.17	-0.06
11/5/2014	6:40	0.05	-0.11
11/5/2014	6:41	-0.11	-0.13
11/5/2014	6:42	-0.12	-0.13
11/5/2014	6:43	0.75	-0.03
11/5/2014	6:44	1.84	1.57
11/5/2014	6:45	1.84	2.03
11/5/2014	6:46	1.84	2.03
11/5/2014	6:47	1.84	2.04
11/5/2014	6:48	16.92	14.42
11/5/2014	6:49	18.99	19.39
11/5/2014	6:50	18.98	19.38
11/5/2014	6:51	18.98	19.38
11/5/2014	6:52	18.98	19.39
11/5/2014	6:53	20.64	7.25
11/5/2014	6:54	20.98	0.39
11/5/2014	6:55	20.96	0.2
11/5/2014	6:56	20.94	0.12
11/5/2014	6:57	20.93	0.06
11/5/2014	6:58	20.93	0.01
11/5/2014	6:59	20.92	0
11/5/2014	7:00	20.92	-0.02
11/5/2014	7:01	20.91	-0.04
11/5/2014	7:02	20.9	-0.05
11/5/2014	7:03	20.9	-0.05
11/5/2014	7:04	20.9	-0.05
11/5/2014	7:05	20.89	-0.05
11/5/2014	7:06	20.89	-0.05
11/5/2014	7:07	20.89	-0.05
11/5/2014	7:08	20.89	-0.05
11/5/2014	7:09	20.9	0
11/5/2014	7:10	20.87	-0.02
11/5/2014	7:11	20.86	-0.05
11/5/2014	7:12	20.85	-0.06
11/5/2014	7:13	20.85	-0.06
11/5/2014	7:14	20.85	-0.06
11/5/2014	7:15	20.85	-0.06
11/5/2014	7:16	20.86	-0.06
11/5/2014	7:17	20.85	-0.06
11/5/2014	7:18	20.85	-0.06
11/5/2014	7:19	20.86	-0.06
11/5/2014	7:20	20.85	-0.05
11/5/2014	7:21	20.86	-0.05
11/5/2014	7:22	20.87	-0.06
11/5/2014	7:23	20.87	-0.06
11/5/2014	7:24	20.87	-0.06
11/5/2014	7:25	20.81	-0.03
11/5/2014	7:26	20.69	0.46
11/5/2014	7:27	20.85	0
11/5/2014	7:28	20.84	-0.06
11/5/2014	7:29	20.85	-0.06
11/5/2014	7:30	20.86	-0.07
11/5/2014	7:31	20.86	-0.06
11/5/2014	7:32	20.86	-0.06
11/5/2014	7:33	20.86	-0.06
11/5/2014	7:34	20.87	-0.06
11/5/2014	7:35	20.87	-0.06
11/5/2014	7:36	20.87	-0.06

00053

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	7:37	20.87	-0.07
11/5/2014	7:38	20.88	-0.07
11/5/2014	7:39	20.87	-0.06
11/5/2014	7:40	20.88	-0.07
11/5/2014	7:41	20.87	-0.07
11/5/2014	7:42	20.87	-0.07
11/5/2014	7:43	20.87	-0.06
11/5/2014	7:44	20.87	-0.07
11/5/2014	7:45	20.88	-0.07
11/5/2014	7:46	20.88	-0.07
11/5/2014	7:47	20.89	-0.07
11/5/2014	7:48	20.89	-0.07
11/5/2014	7:49	20.89	-0.07
11/5/2014	7:50	20.9	-0.07
11/5/2014	7:51	20.9	-0.07
11/5/2014	7:52	20.91	-0.07
11/5/2014	7:53	20.92	-0.07
11/5/2014	7:54	20.92	-0.06
11/5/2014	7:55	20.92	-0.07
11/5/2014	7:56	20.92	-0.06
11/5/2014	7:57	20.92	-0.06
11/5/2014	7:58	20.92	-0.06
11/5/2014	7:59	20.92	-0.06
11/5/2014	8:00	20.92	-0.06
11/5/2014	8:01	20.93	-0.06
11/5/2014	8:02	20.93	-0.06
11/5/2014	8:03	20.92	-0.07
11/5/2014	8:04	20.92	-0.06
11/5/2014	8:05	20.93	-0.06
11/5/2014	8:06	20.93	-0.07
11/5/2014	8:07	20.93	-0.06
11/5/2014	8:08	20.92	-0.06
11/5/2014	8:09	20.91	-0.05
11/5/2014	8:10	20.9	-0.06
11/5/2014	8:11	20.9	-0.06
11/5/2014	8:12	20.9	-0.06
11/5/2014	8:13	20.91	-0.06
11/5/2014	8:14	20.91	-0.06
11/5/2014	8:15	20.92	-0.07
11/5/2014	8:16	20.92	-0.06
11/5/2014	8:17	20.92	-0.07
11/5/2014	8:18	20.92	-0.05
11/5/2014	8:19	20.93	-0.06
11/5/2014	8:20	20.92	-0.06
11/5/2014	8:21	20.93	-0.07
11/5/2014	8:22	20.93	-0.06
11/5/2014	8:23	20.94	-0.06
11/5/2014	8:24	20.94	-0.07
11/5/2014	8:25	20.94	-0.06
11/5/2014	8:26	20.94	-0.07
11/5/2014	8:27	20.94	-0.07
11/5/2014	8:28	20.94	-0.07
11/5/2014	8:29	20.95	-0.07
11/5/2014	8:30	20.94	-0.07
11/5/2014	8:31	20.94	-0.07
11/5/2014	8:32	20.94	-0.07
11/5/2014	8:33	20.93	-0.07
11/5/2014	8:34	20.39	-0.03
11/5/2014	8:35	17.59	3.65
11/5/2014	8:36	20.74	0.27
11/5/2014	8:37	20.86	0.04
11/5/2014	8:38	20.89	-0.02
11/5/2014	8:39	20.91	-0.05
11/5/2014	8:40	20.91	-0.07
11/5/2014	8:41	20.9	-0.07
11/5/2014	8:42	20.91	-0.07
11/5/2014	8:43	20.9	-0.07

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#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	8:44	20.9	-0.06
11/5/2014	8:45	20.9	-0.07
11/5/2014	8:46	20.91	-0.06
11/5/2014	8:47	20.91	-0.07
11/5/2014	8:48	20.91	-0.06
11/5/2014	8:49	20.91	-0.07
11/5/2014	8:50	20.91	-0.07
11/5/2014	8:51	20.91	-0.07
11/5/2014	8:52	20.9	-0.07
11/5/2014	8:53	20.9	-0.06
11/5/2014	8:54	20.9	-0.07
11/5/2014	8:55	20.91	-0.06
11/5/2014	8:56	20.9	-0.06
11/5/2014	8:57	20.89	-0.06
11/5/2014	8:58	20.9	-0.06
11/5/2014	8:59	20.9	-0.06
11/5/2014	9:00	20.9	-0.06
11/5/2014	9:01	20.9	-0.06
11/5/2014	9:02	20.9	-0.06
11/5/2014	9:03	20.9	-0.06
11/5/2014	9:04	20.9	-0.06
11/5/2014	9:05	20.89	-0.07
11/5/2014	9:06	20.9	-0.06
11/5/2014	9:07	20.89	-0.06
11/5/2014	9:08	20.88	-0.06
11/5/2014	9:09	20.88	-0.06
11/5/2014	9:10	20.89	-0.06
11/5/2014	9:11	20.89	-0.06
11/5/2014	9:12	20.89	-0.06
11/5/2014	9:13	20.76	-0.06
11/5/2014	9:14	20.87	-0.06
11/5/2014	9:15	20.88	-0.06
11/5/2014	9:16	20.88	-0.06
11/5/2014	9:17	20.88	-0.07
11/5/2014	9:18	20.88	-0.06
11/5/2014	9:19	20.87	-0.06
11/5/2014	9:20	20.87	-0.06
11/5/2014	9:21	20.88	-0.06
11/5/2014	9:22	20.87	-0.06
11/5/2014	9:23	20.87	-0.06
11/5/2014	9:24	20.87	-0.06
11/5/2014	9:25	20.87	-0.07
11/5/2014	9:26	20.88	-0.06
11/5/2014	9:27	20.87	-0.06
11/5/2014	9:28	20.84	-0.06
11/5/2014	9:29	20.87	-0.06
11/5/2014	9:30	20.86	-0.06
11/5/2014	9:31	20.87	-0.06
11/5/2014	9:32	20.82	-0.06
11/5/2014	9:33	20.87	-0.06
11/5/2014	9:34	20.87	-0.06
11/5/2014	9:35	20.87	-0.06
11/5/2014	9:36	20.88	-0.06
11/5/2014	9:37	20.87	-0.06
11/5/2014	9:38	20.87	-0.06
11/5/2014	9:39	20.87	-0.06
11/5/2014	9:40	20.87	-0.06
11/5/2014	9:41	20.87	-0.06
11/5/2014	9:42	20.88	-0.06
11/5/2014	9:43	20.88	-0.06
11/5/2014	9:44	20.88	-0.06
11/5/2014	9:45	15.79	-0.07
11/5/2014	9:46	11.43	-0.1
11/5/2014	9:47	12.47	-0.1
11/5/2014	9:48	11.35	-0.11
11/5/2014	9:49	11.16	-0.1
11/5/2014	9:50	11.09	-0.11

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#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	9:51	11.03	-0.11
11/5/2014	9:52	10.96	-0.11
11/5/2014	9:53	10.93	-0.11
11/5/2014	9:54	10.99	-0.1
11/5/2014	9:55	11.05	-0.11
11/5/2014	9:56	10.89	-0.1
11/5/2014	9:57	10.79	-0.1
11/5/2014	9:58	10.76	-0.11
11/5/2014	9:59	10.86	-0.11
11/5/2014	10:00	10.51	-0.11
11/5/2014	10:01	10.35	-0.1
11/5/2014	10:02	10.28	-0.11
11/5/2014	10:03	10.26	-0.12
11/5/2014	10:04	10.27	-0.11
11/5/2014	10:05	10.22	-0.11
11/5/2014	10:06	10.17	-0.12
11/5/2014	10:07	10.16	-0.1
11/5/2014	10:08	10.16	-0.1
11/5/2014	10:09	10.16	-0.12
11/5/2014	10:10	10.14	-0.12
11/5/2014	10:11	10.12	-0.12
11/5/2014	10:12	10.07	-0.12
11/5/2014	10:13	10.02	-0.11
11/5/2014	10:14	9.97	-0.11
11/5/2014	10:15	9.98	-0.12
11/5/2014	10:16	9.94	-0.11
11/5/2014	10:17	9.9	-0.12
11/5/2014	10:18	9.9	-0.11
11/5/2014	10:19	9.88	-0.11
11/5/2014	10:20	9.84	-0.1
11/5/2014	10:21	9.77	-0.11
11/5/2014	10:22	9.76	-0.1
11/5/2014	10:23	9.77	-0.11
11/5/2014	10:24	9.74	-0.11
11/5/2014	10:25	9.67	-0.11
11/5/2014	10:26	9.66	-0.11
11/5/2014	10:27	9.68	-0.12
11/5/2014	10:28	9.68	-0.11
11/5/2014	10:29	9.74	-0.11
11/5/2014	10:30	9.79	-0.12
11/5/2014	10:31	9.86	-0.12
11/5/2014	10:32	9.95	-0.11
11/5/2014	10:33	10.04	-0.11
11/5/2014	10:34	10.1	-0.11
11/5/2014	10:35	10.1	-0.12
11/5/2014	10:36	10.02	-0.12
11/5/2014	10:37	9.91	-0.11
11/5/2014	10:38	9.75	-0.11
11/5/2014	10:39	9.67	-0.11
11/5/2014	10:40	9.67	-0.12
11/5/2014	10:41	9.68	-0.12
11/5/2014	10:42	9.65	-0.12
11/5/2014	10:43	9.66	-0.12
11/5/2014	10:44	9.67	-0.12
11/5/2014	10:45	9.69	-0.12
11/5/2014	10:46	9.73	-0.12
11/5/2014	10:47	9.77	-0.12
11/5/2014	10:48	9.78	-0.12
11/5/2014	10:49	9.79	-0.12
11/5/2014	10:50	9.78	-0.12
11/5/2014	10:51	9.74	-0.12
11/5/2014	10:52	9.66	-0.12
11/5/2014	10:53	9.62	-0.11
11/5/2014	10:54	9.61	-0.11
11/5/2014	10:55	9.61	-0.12
11/5/2014	10:56	9.56	-0.12
11/5/2014	10:57	9.53	-0.12

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	10:58	9.49	-0.12
11/5/2014	10:59	9.51	-0.11
11/5/2014	11:00	9.5	-0.11
11/5/2014	11:01	9.47	-0.12
11/5/2014	11:02	9.47	-0.12
11/5/2014	11:03	9.48	-0.12
11/5/2014	11:04	9.43	-0.12
11/5/2014	11:05	9.42	-0.12
11/5/2014	11:06	9.48	-0.11
11/5/2014	11:07	9.57	-0.12
11/5/2014	11:08	9.67	-0.12
11/5/2014	11:09	9.77	-0.11
11/5/2014	11:10	9.9	-0.11
11/5/2014	11:11	10.04	-0.11
11/5/2014	11:12	10.11	-0.11
11/5/2014	11:13	10.19	-0.11
11/5/2014	11:14	10.21	-0.11
11/5/2014	11:15	10.11	-0.11
11/5/2014	11:16	10.05	-0.1
11/5/2014	11:17	10.02	-0.11
11/5/2014	11:18	10	-0.11
11/5/2014	11:19	9.97	-0.11
11/5/2014	11:20	9.98	-0.11
11/5/2014	11:21	10.02	-0.11
11/5/2014	11:22	10.05	-0.12
11/5/2014	11:23	10.03	-0.1
11/5/2014	11:24	10.04	-0.1
11/5/2014	11:25	10.03	-0.1
11/5/2014	11:26	10.01	-0.1
11/5/2014	11:27	9.99	-0.1
11/5/2014	11:28	10.02	-0.1
11/5/2014	11:29	10.05	-0.1
11/5/2014	11:30	10.06	-0.1
11/5/2014	11:31	10.1	-0.1
11/5/2014	11:32	10.18	-0.1
11/5/2014	11:33	10.23	-0.1
11/5/2014	11:34	10.28	-0.1
11/5/2014	11:35	10.28	-0.1
11/5/2014	11:36	10.26	-0.1
11/5/2014	11:37	10.21	-0.1
11/5/2014	11:38	10.21	-0.1
11/5/2014	11:39	10.22	-0.1
11/5/2014	11:40	10.21	-0.1
11/5/2014	11:41	10.22	-0.1
11/5/2014	11:42	10.19	-0.1
11/5/2014	11:43	10.15	-0.1
11/5/2014	11:44	10.12	-0.1
11/5/2014	11:45	10.1	-0.1
11/5/2014	11:46	10.11	-0.1
11/5/2014	11:47	10.08	-0.1
11/5/2014	11:48	10.09	-0.1
11/5/2014	11:49	10.13	-0.1
11/5/2014	11:50	10.14	-0.1
11/5/2014	11:51	10.14	-0.11
11/5/2014	11:52	10.13	-0.1
11/5/2014	11:53	10.11	-0.11
11/5/2014	11:54	10.08	-0.1
11/5/2014	11:55	10.08	-0.1
11/5/2014	11:56	10.08	-0.1
11/5/2014	11:57	10.07	-0.11
11/5/2014	11:58	10.05	-0.11
11/5/2014	11:59	10.03	-0.1
11/5/2014	12:00	10.03	-0.1
11/5/2014	12:01	10.04	-0.11
11/5/2014	12:02	10.05	-0.1
11/5/2014	12:03	10.05	-0.11
11/5/2014	12:04	10.06	-0.11

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	12:05	10.08	-0.1
11/5/2014	12:06	10.06	-0.1
11/5/2014	12:07	10.04	-0.1
11/5/2014	12:08	10.02	-0.1
11/5/2014	12:09	10.04	-0.1
11/5/2014	12:10	10.03	-0.1
11/5/2014	12:11	10.02	-0.1
11/5/2014	12:12	10.04	-0.1
11/5/2014	12:13	10.05	-0.1
11/5/2014	12:14	10.05	-0.11
11/5/2014	12:15	10.06	-0.11
11/5/2014	12:16	10.09	-0.1
11/5/2014	12:17	10.13	-0.1
11/5/2014	12:18	10.16	-0.1
11/5/2014	12:19	10.2	-0.11
11/5/2014	12:20	10.23	-0.11
11/5/2014	12:21	10.24	-0.1
11/5/2014	12:22	10.25	-0.11
11/5/2014	12:23	10.24	-0.1
11/5/2014	12:24	10.22	-0.11
11/5/2014	12:25	10.22	-0.11
11/5/2014	12:26	10.23	-0.1
11/5/2014	12:27	10.26	-0.1
11/5/2014	12:28	10.27	-0.11
11/5/2014	12:29	10.22	-0.1
11/5/2014	12:30	10.19	-0.1
11/5/2014	12:31	10.2	-0.1
11/5/2014	12:32	10.2	-0.11
11/5/2014	12:33	10.19	-0.11
11/5/2014	12:34	10.16	-0.1
11/5/2014	12:35	10.1	-0.11
11/5/2014	12:36	10.08	-0.11
11/5/2014	12:37	10.06	-0.1
11/5/2014	12:38	10.04	-0.11
11/5/2014	12:39	10.03	-0.1
11/5/2014	12:40	10.03	-0.1
11/5/2014	12:41	10.05	-0.1
11/5/2014	12:42	10	-0.11
11/5/2014	12:43	9.95	-0.11
11/5/2014	12:44	9.94	-0.1
11/5/2014	12:45	9.93	-0.11
11/5/2014	12:46	9.9	-0.1
11/5/2014	12:47	9.85	-0.11
11/5/2014	12:48	9.84	-0.1
11/5/2014	12:49	9.81	-0.1
11/5/2014	12:50	9.78	-0.1
11/5/2014	12:51	9.8	-0.1
11/5/2014	12:52	9.82	-0.11
11/5/2014	12:53	9.85	-0.11
11/5/2014	12:54	9.85	-0.11
11/5/2014	12:55	9.82	-0.11
11/5/2014	12:56	9.81	-0.11
11/5/2014	12:57	9.83	-0.11
11/5/2014	12:58	10.05	-0.11
11/5/2014	12:59	10.02	-0.11
11/5/2014	13:00	9.94	-0.11
11/5/2014	13:01	9.85	-0.11
11/5/2014	13:02	9.82	-0.11
11/5/2014	13:03	9.82	-0.11
11/5/2014	13:04	9.81	-0.11
11/5/2014	13:05	9.76	-0.1
11/5/2014	13:06	9.67	-0.1
11/5/2014	13:07	9.58	-0.11
11/5/2014	13:08	9.56	-0.11
11/5/2014	13:09	9.56	-0.11
11/5/2014	13:10	9.57	-0.11
11/5/2014	13:11	9.59	-0.11

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	13:12	9.6	-0.11
11/5/2014	13:13	9.59	-0.11
11/5/2014	13:14	9.61	-0.11
11/5/2014	13:15	9.62	-0.1
11/5/2014	13:16	9.61	-0.1
11/5/2014	13:17	9.61	-0.1
11/5/2014	13:18	9.62	-0.1
11/5/2014	13:19	9.64	-0.1
11/5/2014	13:20	7.84	-0.09
11/5/2014	13:21	3.78	3.87
11/5/2014	13:22	3.9	4.46
11/5/2014	13:23	4.09	4.48
11/5/2014	13:24	3.11	2.42
11/5/2014	13:25	1.85	2.06
11/5/2014	13:26	1.84	2.06
11/5/2014	13:27	7.38	1.98
11/5/2014	13:28	15.18	4.5
11/5/2014	13:29	18.99	0.03
11/5/2014	13:30	18.98	-0.1
11/5/2014	13:31	9.73	-0.1
11/5/2014	13:32	0.03	-0.1
11/5/2014	13:33	-0.12	-0.09
11/5/2014	13:34	-0.13	-0.1
11/5/2014	13:35	11.02	0.03
11/5/2014	13:36	4.44	2.51
11/5/2014	13:37	9.03	0.17
11/5/2014	13:38	9.24	-0.05
11/5/2014	13:39	9.22	-0.09
11/5/2014	13:40	9.21	-0.09
11/5/2014	13:41	9.23	-0.09
11/5/2014	13:42	9.25	-0.1
11/5/2014	13:43	9.26	-0.1
11/5/2014	13:44	9.31	-0.1
11/5/2014	13:45	9.38	-0.1
11/5/2014	13:46	9.46	-0.1
11/5/2014	13:47	9.51	-0.1
11/5/2014	13:48	9.58	-0.1
11/5/2014	13:49	9.57	-0.1
11/5/2014	13:50	9.56	-0.1
11/5/2014	13:51	9.53	-0.1
11/5/2014	13:52	10.1	-0.1
11/5/2014	13:53	19.44	-0.08
11/5/2014	13:54	19.98	-0.06
11/5/2014	13:55	19.51	-0.07
11/5/2014	13:56	19.53	-0.08
11/5/2014	13:57	19.54	-0.08
11/5/2014	13:58	19.59	-0.08
11/5/2014	13:59	19.63	-0.08
11/5/2014	14:00	19.64	-0.07
11/5/2014	14:01	19.63	-0.07
11/5/2014	14:02	19.61	-0.08
11/5/2014	14:03	19.62	-0.07
11/5/2014	14:04	19.6	-0.08
11/5/2014	14:05	19.6	-0.07
11/5/2014	14:06	19.6	-0.08
11/5/2014	14:07	19.6	-0.08
11/5/2014	14:08	19.6	-0.08
11/5/2014	14:09	19.6	-0.08
11/5/2014	14:10	19.6	-0.07
11/5/2014	14:11	19.61	-0.08
11/5/2014	14:12	19.6	-0.08
11/5/2014	14:13	19.6	-0.07
11/5/2014	14:14	19.59	-0.08
11/5/2014	14:15	19.6	-0.07
11/5/2014	14:16	19.6	-0.08
11/5/2014	14:17	19.58	-0.08
11/5/2014	14:18	19.57	-0.07

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#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	14:19	19.57	-0.07
11/5/2014	14:20	19.56	-0.08
11/5/2014	14:21	19.56	-0.08
11/5/2014	14:22	19.53	-0.07
11/5/2014	14:23	19.51	-0.07
11/5/2014	14:24	19.5	-0.07
11/5/2014	14:25	19.48	-0.07
11/5/2014	14:26	19.47	-0.07
11/5/2014	14:27	19.47	-0.07
11/5/2014	14:28	19.46	-0.07
11/5/2014	14:29	19.44	-0.07
11/5/2014	14:30	19.42	-0.07
11/5/2014	14:31	19.4	-0.07
11/5/2014	14:32	19.41	-0.07
11/5/2014	14:33	19.41	-0.08
11/5/2014	14:34	19.42	-0.07
11/5/2014	14:35	19.4	-0.07
11/5/2014	14:36	19.46	-0.08
11/5/2014	14:37	19.46	-0.08
11/5/2014	14:38	19.47	-0.08
11/5/2014	14:39	19.47	-0.08
11/5/2014	14:40	19.48	-0.07
11/5/2014	14:41	19.47	-0.07
11/5/2014	14:42	19.48	-0.08
11/5/2014	14:43	19.49	-0.07
11/5/2014	14:44	19.5	-0.07
11/5/2014	14:45	19.49	-0.08
11/5/2014	14:46	19.47	-0.07
11/5/2014	14:47	19.45	-0.07
11/5/2014	14:48	19.43	-0.07
11/5/2014	14:49	19.41	-0.08
11/5/2014	14:50	19.39	-0.07
11/5/2014	14:51	19.41	-0.07
11/5/2014	14:52	19.39	-0.07
11/5/2014	14:53	19.37	-0.07
11/5/2014	14:54	19.33	-0.07
11/5/2014	14:55	19.32	-0.07
11/5/2014	14:56	19.33	-0.07
11/5/2014	14:57	19.34	-0.07
11/5/2014	14:58	19.33	-0.08
11/5/2014	14:59	19.31	-0.07
11/5/2014	15:00	19.29	-0.07
11/5/2014	15:01	19.27	-0.07
11/5/2014	15:02	19.25	-0.07
11/5/2014	15:03	19.24	-0.07
11/5/2014	15:04	19.22	-0.07
11/5/2014	15:05	19.19	-0.07
11/5/2014	15:06	19.16	-0.07
11/5/2014	15:07	19.14	-0.07
11/5/2014	15:08	19.12	-0.07
11/5/2014	15:09	19.11	-0.07
11/5/2014	15:10	19.11	-0.07
11/5/2014	15:11	19.13	-0.07
11/5/2014	15:12	19.41	-0.06
11/5/2014	15:13	19.39	-0.05
11/5/2014	15:14	19.35	-0.05
11/5/2014	15:15	19.34	-0.06
11/5/2014	15:16	19.35	-0.06
11/5/2014	15:17	19.36	-0.06
11/5/2014	15:18	19.35	-0.06
11/5/2014	15:19	19.33	-0.06
11/5/2014	15:20	19.31	-0.06
11/5/2014	15:21	19.29	-0.06
11/5/2014	15:22	19.27	-0.06
11/5/2014	15:23	19.26	-0.06
11/5/2014	15:24	19.24	-0.06
11/5/2014	15:25	19.21	-0.06

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	15:26	19.19	-0.07
11/5/2014	15:27	19.14	-0.07
11/5/2014	15:28	19.11	-0.06
11/5/2014	15:29	19.01	-0.07
11/5/2014	15:30	18.97	-0.07
11/5/2014	15:31	19.01	-0.07
11/5/2014	15:32	19.13	-0.07
11/5/2014	15:33	19.17	-0.07
11/5/2014	15:34	19.11	-0.06
11/5/2014	15:35	19.09	-0.07
11/5/2014	15:36	19.12	-0.07
11/5/2014	15:37	19.2	-0.06
11/5/2014	15:38	19.63	-0.06
11/5/2014	15:39	19.41	-0.06
11/5/2014	15:40	19.32	-0.06
11/5/2014	15:41	19.63	-0.06
11/5/2014	15:42	19.26	-0.05
11/5/2014	15:43	19.24	-0.04
11/5/2014	15:44	19.23	-0.05
11/5/2014	15:45	19.21	-0.04
11/5/2014	15:46	19.18	-0.05
11/5/2014	15:47	19.16	-0.05
11/5/2014	15:48	19.11	-0.05
11/5/2014	15:49	19.08	-0.05
11/5/2014	15:50	18.98	-0.04
11/5/2014	15:51	18.94	-0.05
11/5/2014	15:52	18.98	-0.05
11/5/2014	15:53	19.1	-0.05
11/5/2014	15:54	19.14	-0.05
11/5/2014	15:55	19.08	-0.05
11/5/2014	15:56	19.06	-0.06
11/5/2014	15:57	19.09	-0.06
11/5/2014	15:58	19.17	-0.05
11/5/2014	15:59	19.6	-0.05
11/5/2014	16:00	19.38	-0.05
11/5/2014	16:01	19.18	-0.05
11/5/2014	16:02	19.16	-0.04
11/5/2014	16:03	19.14	-0.04
11/5/2014	16:04	19.13	-0.05
11/5/2014	16:05	19.13	-0.05
11/5/2014	16:06	19.15	-0.04
11/5/2014	16:07	19.43	-0.04
11/5/2014	16:08	19.41	-0.04
11/5/2014	16:09	19.37	-0.04
11/5/2014	16:10	19.36	-0.04
11/5/2014	16:11	19.37	-0.04
11/5/2014	16:12	19.38	-0.05
11/5/2014	16:13	19.37	-0.05
11/5/2014	16:14	19.35	-0.04
11/5/2014	16:15	19.33	-0.05
11/5/2014	16:16	19.31	-0.05
11/5/2014	16:17	19.29	-0.05
11/5/2014	16:18	19.28	-0.05
11/5/2014	16:19	19.26	-0.05
11/5/2014	16:20	19.23	-0.05
11/5/2014	16:21	19.21	-0.05
11/5/2014	16:22	19.16	-0.05
11/5/2014	16:23	19.18	-0.05
11/5/2014	16:24	19.12	-0.05
11/5/2014	16:25	19.1	-0.05
11/5/2014	16:26	19.13	-0.05
11/5/2014	16:27	19.21	-0.05
11/5/2014	16:28	19.64	-0.05
11/5/2014	16:29	19.42	-0.05
11/5/2014	16:30	19.22	-0.05
11/5/2014	16:31	19.2	-0.05
11/5/2014	16:32	19.18	-0.04

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#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	16:33	19.17	-0.05
11/5/2014	16:34	19.17	-0.05
11/5/2014	16:35	19.19	-0.05
11/5/2014	16:36	19.47	-0.05
11/5/2014	16:37	19.45	-0.05
11/5/2014	16:38	19.41	-0.05
11/5/2014	16:39	19.4	-0.05
11/5/2014	16:40	19.11	-0.05
11/5/2014	16:41	19.05	-0.05
11/5/2014	16:42	19.03	-0.05
11/5/2014	16:43	19.06	-0.05
11/5/2014	16:44	19.14	-0.05
11/5/2014	16:45	19.57	-0.05
11/5/2014	16:46	19.35	-0.05
11/5/2014	16:47	19.15	-0.05
11/5/2014	16:48	19.13	-0.05
11/5/2014	16:49	19.11	-0.05
11/5/2014	16:50	19.1	-0.04
11/5/2014	16:51	19.1	-0.05
11/5/2014	16:52	19.12	-0.05
11/5/2014	16:53	19.4	-0.05
11/5/2014	16:54	19.38	-0.05
11/5/2014	16:55	19.34	-0.05
11/5/2014	16:56	19.33	-0.05
11/5/2014	16:57	19.34	-0.04
11/5/2014	16:58	19.23	-0.03
11/5/2014	16:59	19.51	-0.04
11/5/2014	17:00	19.49	-0.04
11/5/2014	17:01	19.45	-0.03
11/5/2014	17:02	19.44	-0.03
11/5/2014	17:03	19.15	-0.05
11/5/2014	17:04	19.09	-0.04
11/5/2014	17:05	19.07	-0.03
11/5/2014	17:06	19.1	-0.05
11/5/2014	17:07	19.18	-0.05
11/5/2014	17:08	19.61	-0.05
11/5/2014	17:09	19.39	-0.05
11/5/2014	17:10	19.19	-0.05
11/5/2014	17:11	19.17	-0.05
11/5/2014	17:12	19.15	-0.05
11/5/2014	17:13	19.14	-0.05
11/5/2014	17:14	19.14	-0.05
11/5/2014	17:15	19.16	-0.04
11/5/2014	17:16	19.44	-0.04
11/5/2014	17:17	19.51	-0.05
11/5/2014	17:18	19.49	-0.05
11/5/2014	17:19	19.45	-0.05
11/5/2014	17:20	20.79	-0.05
11/5/2014	17:21	20.81	-0.05
11/5/2014	17:22	20.83	-0.05
11/5/2014	17:23	20.83	-0.05
11/5/2014	17:24	5.87	-0.06
11/5/2014	17:25	-0.09	-0.1
11/5/2014	17:26	-0.11	-0.1
11/5/2014	17:27	-0.12	-0.1
11/5/2014	17:28	2.5	0.22
11/5/2014	17:29	1.85	1.89
11/5/2014	17:30	1.85	2.06
11/5/2014	17:31	1.85	2.06
11/5/2014	17:32	10.64	7.01
11/5/2014	17:33	18.89	19.04
11/5/2014	17:34	20.9	1.72
11/5/2014	17:35	20.87	0.07
11/5/2014	17:36	20.48	0.39
11/5/2014	17:37	7.98	8.12
11/5/2014	17:38	20.07	0.42
11/5/2014	17:39	21.19	-0.06

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#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/5/2014	17:40	20.59	-0.06
11/5/2014	17:41	20.58	-0.09
11/5/2014	17:42	20.58	-0.09
11/5/2014	17:43	20.58	-0.09
11/5/2014	17:44	20.58	-0.1
11/5/2014	17:45	20.58	-0.1
11/5/2014	17:46	20.91	-0.1
11/5/2014	17:47	21.02	-0.1
11/5/2014	17:48	21.02	-0.1
11/5/2014	17:49	21.01	-0.1
11/5/2014	17:50	16	0.13
11/5/2014	17:51	18.49	0.35
11/5/2014	17:52	20.79	-0.02
11/5/2014	17:53	20.83	-0.04
11/5/2014	17:54	20.83	-0.04
11/5/2014	17:55	20.82	-0.04
11/5/2014	17:56	20.83	-0.04
11/5/2014	17:57	20.82	-0.04
11/5/2014	17:58	20.83	-0.04
11/5/2014	17:59	20.83	-0.04
11/5/2014	18:00	20.83	-0.04
11/6/2014	6:00	20.93	-0.06
11/6/2014	6:01	20.93	-0.05
11/6/2014	6:02	20.93	-0.05
11/6/2014	6:03	20.93	-0.05
11/6/2014	6:04	20.93	-0.05
11/6/2014	6:05	20.92	-0.04
11/6/2014	6:06	20.92	-0.05
11/6/2014	6:07	20.92	-0.05
11/6/2014	6:08	20.92	-0.05
11/6/2014	6:09	20.92	-0.06
11/6/2014	6:10	20.92	-0.05
11/6/2014	6:11	20.93	-0.05
11/6/2014	6:12	20.92	-0.05
11/6/2014	6:13	20.93	-0.05
11/6/2014	6:14	20.93	-0.05
11/6/2014	6:15	20.93	-0.06
11/6/2014	6:16	20.93	-0.05
11/6/2014	6:17	20.93	-0.05
11/6/2014	6:18	20.93	-0.06
11/6/2014	6:19	20.93	-0.06
11/6/2014	6:20	20.93	-0.04
11/6/2014	6:21	20.93	-0.05
11/6/2014	6:22	20.93	-0.05
11/6/2014	6:23	20.93	-0.05
11/6/2014	6:24	20.93	-0.05
11/6/2014	6:25	20.93	-0.05
11/6/2014	6:26	20.93	-0.06
11/6/2014	6:27	20.93	-0.06
11/6/2014	6:28	20.93	-0.06
11/6/2014	6:29	20.93	-0.05
11/6/2014	6:30	20.93	-0.04
11/6/2014	6:31	20.93	-0.05
11/6/2014	6:32	20.93	-0.06
11/6/2014	6:33	20.93	-0.05
11/6/2014	6:34	20.93	-0.05
11/6/2014	6:35	20.93	-0.05
11/6/2014	6:36	20.92	-0.05
11/6/2014	6:37	20.92	-0.05
11/6/2014	6:38	20.92	-0.05
11/6/2014	6:39	20.92	-0.05
11/6/2014	6:40	20.92	-0.05
11/6/2014	6:41	20.92	-0.05
11/6/2014	6:42	20.92	-0.05
11/6/2014	6:43	20.92	-0.06
11/6/2014	6:44	20.92	-0.06
11/6/2014	6:45	20.92	-0.06

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/6/2014	6:46	20.92	-0.05
11/6/2014	6:47	20.92	-0.05
11/6/2014	6:48	20.92	-0.05
11/6/2014	6:49	20.91	-0.05
11/6/2014	6:50	20.91	-0.05
11/6/2014	6:51	20.91	-0.05
11/6/2014	6:52	20.91	-0.05
11/6/2014	6:53	20.91	-0.05
11/6/2014	6:54	20.91	-0.05
11/6/2014	6:55	10.23	-0.06
11/6/2014	6:56	-0.06	-0.1
11/6/2014	6:57	-0.1	-0.1
11/6/2014	6:58	0.73	-0.1
11/6/2014	6:59	9.09	0.07
11/6/2014	7:00	1.69	1.82
11/6/2014	7:01	1.68	2.23
11/6/2014	7:02	1.69	2.25
11/6/2014	7:03	5.68	2.21
11/6/2014	7:04	14.33	5.13
11/6/2014	7:05	9.22	11.13
11/6/2014	7:06	9.26	11.16
11/6/2014	7:07	9.28	11.16
11/6/2014	7:08	12.99	9.21
11/6/2014	7:09	21	0.2
11/6/2014	7:10	20.9	0.03
11/6/2014	7:11	20.84	0.02
11/6/2014	7:12	20.82	0.02
11/6/2014	7:13	20.82	0.01
11/6/2014	7:14	20.82	0
11/6/2014	7:15	20.82	0
11/6/2014	7:16	20.83	-0.01
11/6/2014	7:17	20.83	-0.01
11/6/2014	7:18	20.84	-0.01
11/6/2014	7:19	20.84	-0.02
11/6/2014	7:20	20.85	-0.02
11/6/2014	7:21	20.85	-0.02
11/6/2014	7:22	20.85	-0.02
11/6/2014	7:23	20.85	-0.04
11/6/2014	7:24	20.86	-0.04
11/6/2014	7:25	20.86	-0.04
11/6/2014	7:26	20.86	-0.04
11/6/2014	7:27	20.86	-0.04
11/6/2014	7:28	20.86	-0.04
11/6/2014	7:29	20.86	-0.04
11/6/2014	7:30	20.86	-0.04
11/6/2014	7:31	20.86	-0.04
11/6/2014	7:32	20.87	-0.04
11/6/2014	7:33	20.87	-0.04
11/6/2014	7:34	20.87	-0.04
11/6/2014	7:35	20.87	-0.05
11/6/2014	7:36	20.87	-0.04
11/6/2014	7:37	20.87	-0.04
11/6/2014	7:38	20.88	-0.04
11/6/2014	7:39	20.88	-0.04
11/6/2014	7:40	20.83	-0.02
11/6/2014	7:41	20.8	0.03
11/6/2014	7:42	20.81	0.01
11/6/2014	7:43	20.8	-0.01
11/6/2014	7:44	20.77	-0.02
11/6/2014	7:45	20.75	-0.03
11/6/2014	7:46	20.74	-0.02
11/6/2014	7:47	20.73	-0.02
11/6/2014	7:48	20.75	-0.02
11/6/2014	7:49	20.78	-0.02
11/6/2014	7:50	20.79	-0.02
11/6/2014	7:51	20.8	-0.02
11/6/2014	7:52	20.8	-0.02

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#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/6/2014	7:53	20.81	-0.02
11/6/2014	7:54	20.81	-0.02
11/6/2014	7:55	20.81	-0.02
11/6/2014	7:56	20.81	-0.02
11/6/2014	7:57	20.81	-0.02
11/6/2014	7:58	20.81	-0.02
11/6/2014	7:59	20.81	-0.02
11/6/2014	8:00	20.81	-0.02
11/6/2014	8:01	20.81	-0.02
11/6/2014	8:02	20.81	-0.02
11/6/2014	8:03	20.81	-0.01
11/6/2014	8:04	20.81	-0.01
11/6/2014	8:05	20.81	-0.01
11/6/2014	8:06	20.81	-0.01
11/6/2014	8:07	20.83	-0.04
11/6/2014	8:08	20.19	-0.06
11/6/2014	8:09	20.81	-0.05
11/6/2014	8:10	20.84	-0.05
11/6/2014	8:11	20.84	-0.04
11/6/2014	8:12	20.83	-0.05
11/6/2014	8:13	20.82	-0.06
11/6/2014	8:14	20.8	-0.06
11/6/2014	8:15	20.8	-0.06
11/6/2014	8:16	20.82	-0.06
11/6/2014	8:17	20.84	-0.06
11/6/2014	8:18	20.84	-0.05
11/6/2014	8:19	20.85	-0.05
11/6/2014	8:20	20.85	-0.06
11/6/2014	8:21	20.83	-0.05
11/6/2014	8:22	20.75	-0.01
11/6/2014	8:23	20.68	0.02
11/6/2014	8:24	20.71	0.09
11/6/2014	8:25	20.77	-0.04
11/6/2014	8:26	20.77	-0.05
11/6/2014	8:27	20.78	-0.05
11/6/2014	8:28	20.78	-0.05
11/6/2014	8:29	20.78	-0.05
11/6/2014	8:30	20.77	-0.05
11/6/2014	8:31	20.77	-0.05
11/6/2014	8:32	20.78	-0.05
11/6/2014	8:33	20.77	-0.05
11/6/2014	8:34	20.78	-0.05
11/6/2014	8:35	20.78	-0.06
11/6/2014	8:36	20.78	-0.06
11/6/2014	8:37	20.77	-0.05
11/6/2014	8:38	20.78	-0.05
11/6/2014	8:39	20.77	-0.05
11/6/2014	8:40	20.77	-0.05
11/6/2014	8:41	20.77	-0.05
11/6/2014	8:42	20.77	-0.05
11/6/2014	8:43	20.77	-0.05
11/6/2014	8:44	20.77	-0.05
11/6/2014	8:45	20.77	-0.05
11/6/2014	8:46	20.77	-0.05
11/6/2014	8:47	20.78	-0.05
11/6/2014	8:48	20.77	-0.05
11/6/2014	8:49	20.77	-0.05
11/6/2014	8:50	20.77	-0.05
11/6/2014	8:51	20.78	-0.05
11/6/2014	8:52	20.77	-0.05
11/6/2014	8:53	18.53	-0.07
11/6/2014	8:54	17.62	-0.09
11/6/2014	8:55	17.58	-0.1
11/6/2014	8:56	17.51	-0.1
11/6/2014	8:57	17.51	-0.1
11/6/2014	8:58	17.52	-0.1
11/6/2014	8:59	17.49	-0.1

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#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/6/2014	9:00	17.48	-0.1
11/6/2014	9:01	17.48	-0.1
11/6/2014	9:02	17.5	-0.1
11/6/2014	9:03	17.49	-0.1
11/6/2014	9:04	17.59	-0.1
11/6/2014	9:05	17.62	-0.1
11/6/2014	9:06	17.59	-0.1
11/6/2014	9:07	17.57	-0.1
11/6/2014	9:08	17.49	-0.1
11/6/2014	9:09	17.49	-0.1
11/6/2014	9:10	17.5	-0.1
11/6/2014	9:11	17.5	-0.1
11/6/2014	9:12	17.43	-0.1
11/6/2014	9:13	17.42	-0.1
11/6/2014	9:14	17.39	-0.1
11/6/2014	9:15	17.36	-0.1
11/6/2014	9:16	17.38	-0.1
11/6/2014	9:17	17.54	-0.1
11/6/2014	9:18	17.7	-0.1
11/6/2014	9:19	17.6	-0.1
11/6/2014	9:20	17.67	-0.1
11/6/2014	9:21	17.72	-0.1
11/6/2014	9:22	17.74	-0.1
11/6/2014	9:23	17.63	-0.1
11/6/2014	9:24	17.47	-0.1
11/6/2014	9:25	17.4	-0.1
11/6/2014	9:26	17.37	-0.1
11/6/2014	9:27	17.47	-0.1
11/6/2014	9:28	17.56	-0.1
11/6/2014	9:29	17.73	-0.1
11/6/2014	9:30	17.85	-0.1
11/6/2014	9:31	17.87	-0.1
11/6/2014	9:32	17.91	-0.1
11/6/2014	9:33	17.86	-0.1
11/6/2014	9:34	17.82	-0.1
11/6/2014	9:35	17.79	-0.1
11/6/2014	9:36	17.76	-0.1
11/6/2014	9:37	17.76	-0.1
11/6/2014	9:38	17.71	-0.1
11/6/2014	9:39	17.69	-0.1
11/6/2014	9:40	17.73	-0.1
11/6/2014	9:41	17.76	-0.1
11/6/2014	9:42	17.71	-0.1
11/6/2014	9:43	17.81	-0.1
11/6/2014	9:44	17.85	-0.1
11/6/2014	9:45	17.78	-0.1
11/6/2014	9:46	17.66	-0.1
11/6/2014	9:47	17.62	-0.1
11/6/2014	9:48	17.55	-0.1
11/6/2014	9:49	17.54	-0.1
11/6/2014	9:50	17.51	-0.1
11/6/2014	9:51	17.54	-0.1
11/6/2014	9:52	17.67	-0.1
11/6/2014	9:53	17.68	-0.1
11/6/2014	9:54	17.78	-0.1
11/6/2014	9:55	17.91	-0.1
11/6/2014	9:56	17.93	-0.1
11/6/2014	9:57	18.02	-0.1
11/6/2014	9:58	17.96	-0.1
11/6/2014	9:59	18	-0.1
11/6/2014	10:00	17.94	-0.1
11/6/2014	10:01	17.94	-0.1
11/6/2014	10:02	17.84	-0.1
11/6/2014	10:03	17.89	-0.1
11/6/2014	10:04	17.82	-0.1
11/6/2014	10:05	17.81	-0.1
11/6/2014	10:06	17.73	-0.1

00066

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/6/2014	10:07	17.75	-0.1
11/6/2014	10:08	17.73	-0.1
11/6/2014	10:09	17.72	-0.1
11/6/2014	10:10	17.68	-0.1
11/6/2014	10:11	17.75	-0.1
11/6/2014	10:12	17.7	-0.1
11/6/2014	10:13	17.67	-0.1
11/6/2014	10:14	17.63	-0.1
11/6/2014	10:15	17.54	-0.1
11/6/2014	10:16	17.52	-0.09
11/6/2014	10:17	17.5	-0.1
11/6/2014	10:18	17.59	-0.09
11/6/2014	10:19	17.52	-0.09
11/6/2014	10:20	17.54	-0.09
11/6/2014	10:21	17.51	-0.09
11/6/2014	10:22	17.45	-0.09
11/6/2014	10:23	17.51	-0.09
11/6/2014	10:24	17.45	-0.09
11/6/2014	10:25	17.48	-0.1
11/6/2014	10:26	17.54	-0.09
11/6/2014	10:27	17.55	-0.09
11/6/2014	10:28	17.59	-0.1
11/6/2014	10:29	17.49	-0.09
11/6/2014	10:30	17.43	-0.09
11/6/2014	10:31	17.5	-0.09
11/6/2014	10:32	17.49	-0.09
11/6/2014	10:33	17.57	-0.09
11/6/2014	10:34	17.55	-0.09
11/6/2014	10:35	17.56	-0.09
11/6/2014	10:36	17.56	-0.1
11/6/2014	10:37	17.4	-0.09
11/6/2014	10:38	17.49	-0.1
11/6/2014	10:39	17.66	-0.09
11/6/2014	10:40	17.59	-0.09
11/6/2014	10:41	17.63	-0.1
11/6/2014	10:42	17.6	-0.09
11/6/2014	10:43	17.66	-0.09
11/6/2014	10:44	17.56	-0.09
11/6/2014	10:45	17.61	-0.1
11/6/2014	10:46	17.49	-0.1
11/6/2014	10:47	17.51	-0.1
11/6/2014	10:48	17.58	-0.1
11/6/2014	10:49	17.68	-0.09
11/6/2014	10:50	17.64	-0.1
11/6/2014	10:51	17.66	-0.1
11/6/2014	10:52	17.69	-0.1
11/6/2014	10:53	17.6	-0.1
11/6/2014	10:54	17.61	-0.1
11/6/2014	10:55	17.55	-0.1
11/6/2014	10:56	17.5	-0.1
11/6/2014	10:57	17.57	-0.1
11/6/2014	10:58	17.61	-0.09
11/6/2014	10:59	17.62	-0.09
11/6/2014	11:00	17.7	-0.1
11/6/2014	11:01	17.65	-0.1
11/6/2014	11:02	17.67	-0.09
11/6/2014	11:03	17.65	-0.1
11/6/2014	11:04	17.61	-0.1
11/6/2014	11:05	17.61	-0.09
11/6/2014	11:06	17.52	-0.1
11/6/2014	11:07	17.54	-0.09
11/6/2014	11:08	17.5	-0.09
11/6/2014	11:09	17.54	-0.09
11/6/2014	11:10	17.5	-0.09
11/6/2014	11:11	17.61	-0.1
11/6/2014	11:12	17.59	-0.09
11/6/2014	11:13	17.59	-0.1

00067

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/6/2014	11:14	17.53	-0.1
11/6/2014	11:15	17.55	-0.09
11/6/2014	11:16	17.53	-0.09
11/6/2014	11:17	17.62	-0.09
11/6/2014	11:18	17.6	-0.1
11/6/2014	11:19	17.58	-0.09
11/6/2014	11:20	17.56	-0.09
11/6/2014	11:21	17.6	-0.09
11/6/2014	11:22	17.51	-0.09
11/6/2014	11:23	17.52	-0.09
11/6/2014	11:24	17.52	-0.1
11/6/2014	11:25	17.48	-0.1
11/6/2014	11:26	17.47	-0.09
11/6/2014	11:27	17.49	-0.09
11/6/2014	11:28	17.53	-0.09
11/6/2014	11:29	17.63	-0.1
11/6/2014	11:30	17.64	-0.09
11/6/2014	11:31	17.67	-0.09
11/6/2014	11:32	17.63	-0.09
11/6/2014	11:33	17.68	-0.1
11/6/2014	11:34	17.63	-0.09
11/6/2014	11:35	17.5	-0.09
11/6/2014	11:36	17.38	-0.1
11/6/2014	11:37	17.39	-0.09
11/6/2014	11:38	17.47	-0.09
11/6/2014	11:39	17.35	-0.09
11/6/2014	11:40	17.77	-0.09
11/6/2014	11:41	17.77	-0.09
11/6/2014	11:42	17.86	-0.09
11/6/2014	11:43	17.42	-0.09
11/6/2014	11:44	17.45	-0.09
11/6/2014	11:45	17.8	-0.09
11/6/2014	11:46	17.75	-0.08
11/6/2014	11:47	17.59	-0.09
11/6/2014	11:48	17.52	-0.09
11/6/2014	11:49	17.51	-0.09
11/6/2014	11:50	17.59	-0.09
11/6/2014	11:51	17.64	-0.09
11/6/2014	11:52	17.74	-0.1
11/6/2014	11:53	17.77	-0.09
11/6/2014	11:54	17.72	-0.09
11/6/2014	11:55	17.81	-0.09
11/6/2014	11:56	18.06	-0.09
11/6/2014	11:57	17.62	-0.09
11/6/2014	11:58	17.59	-0.09
11/6/2014	11:59	17.75	-0.09
11/6/2014	12:00	17.58	-0.09
11/6/2014	12:01	17.45	-0.09
11/6/2014	12:02	17.61	-0.09
11/6/2014	12:03	17.6	-0.09
11/6/2014	12:04	17.5	-0.09
11/6/2014	12:05	17.43	-0.09
11/6/2014	12:06	17.51	-0.09
11/6/2014	12:07	17.42	-0.09
11/6/2014	12:08	17.41	-0.09
11/6/2014	12:09	17.45	-0.09
11/6/2014	12:10	17.59	-0.09
11/6/2014	12:11	17.93	-0.09
11/6/2014	12:12	17.91	-0.09
11/6/2014	12:13	18.01	-0.09
11/6/2014	12:14	17.74	-0.09
11/6/2014	12:15	17.9	-0.09
11/6/2014	12:16	17.83	-0.09
11/6/2014	12:17	17.75	-0.09
11/6/2014	12:18	17.84	-0.09
11/6/2014	12:19	17.68	-0.09
11/6/2014	12:20	17.72	-0.09

#1 #2 and #3 BSW 1 min avgs.xls

Date	Time	O2	CO2
11/6/2014	12:21	17.75	-0.09
11/6/2014	12:22	17.71	-0.09
11/6/2014	12:23	17.51	-0.09
11/6/2014	12:24	17.61	-0.09
11/6/2014	12:25	17.59	-0.09
11/6/2014	12:26	17.5	-0.09
11/6/2014	12:27	17.51	-0.1
11/6/2014	12:28	17.57	-0.09
11/6/2014	12:29	17.5	-0.09
11/6/2014	12:30	17.58	-0.09
11/6/2014	12:31	17.61	-0.09
11/6/2014	12:32	17.65	-0.09
11/6/2014	12:33	17.75	-0.09
11/6/2014	12:34	17.64	-0.1
11/6/2014	12:35	17.59	-0.1
11/6/2014	12:36	17.56	-0.1
11/6/2014	12:37	17.96	-0.1
11/6/2014	12:38	17.72	-0.1
11/6/2014	12:39	17.66	-0.1
11/6/2014	12:40	17.69	-0.1
11/6/2014	12:41	17.76	-0.1
11/6/2014	12:42	17.98	-0.09
11/6/2014	12:43	17.74	-0.09
11/6/2014	12:44	17.82	-0.09
11/6/2014	12:45	17.78	-0.09
11/6/2014	12:46	17.98	-0.1
11/6/2014	12:47	17.8	-0.1
11/6/2014	12:48	17.69	-0.09
11/6/2014	12:49	17.83	-0.1
11/6/2014	12:50	17.74	-0.09
11/6/2014	12:51	17.77	-0.09
11/6/2014	12:52	17.83	-0.1
11/6/2014	12:53	18.14	-0.08
11/6/2014	12:54	17.67	-0.09
11/6/2014	12:55	17.54	-0.1
11/6/2014	12:56	17.88	-0.09
11/6/2014	12:57	1.38	-0.06
11/6/2014	12:58	-0.1	-0.09
11/6/2014	12:59	-0.12	-0.09
11/6/2014	13:00	-0.12	-0.09
11/6/2014	13:01	1.95	-0.04
11/6/2014	13:02	1.67	1.61
11/6/2014	13:03	6.35	2.26
11/6/2014	13:04	21.02	2.27
11/6/2014	13:05	20.96	2.22
11/6/2014	13:06	20.92	0.68
11/6/2014	13:07	20.91	-0.01

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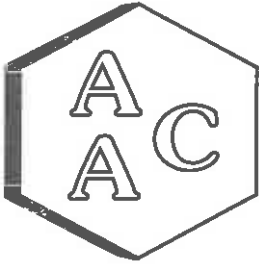
GP BSW #1, #2 and #3 meOH Testing  
QA/QC Spikes

→ Bottle 20 - Blank  
Lab result: < SRL

→ Bottle 21 - ~~Low~~ Low Spike  
 $50 \mu\text{L} \times 15,000 \mu\text{g}/\text{mL} = 750 \mu\text{g}$   
Lab result = 835  $\mu\text{g}$

→ Bottle 22 - High Spike  
 $300 \mu\text{L} \times 15,000 \mu\text{g}/\text{mL} = 4500 \mu\text{g}$   
Lab result = 4940  $\mu\text{g}$





# Atmospheric Analysis & Consulting, Inc.

Client : Bighorn Environmental  
Client Project Name : GP-Toledo 2014 BSW testing  
Client Project Number : NA  
AAC Project Number : 141814  
Reporting Date : 11/21/2014


On November 19, 2014, Atmospheric Analysis & Consulting, Inc. received fifteen (15) liquid samples for Methanol Analysis by NCASI Method 94.02. Upon receipt the samples were assigned unique Laboratory ID numbers as follows:

Client Sample ID	AAC Sample ID	Client Sample ID	AAC Sample ID
BSW #2 Combined Vent Run 1	141814-75802	#1 Vacuum Pump Run 3	141814-75810
BSW #2 Combined Vent Run 2	141814-75803	#1 Foam Breaker Run 1	141814-75811
BSW #2 Combined Vent Run 3	141814-75804	#1 Foam Breaker Run 2	141814-75812
BSW #3 Combined Vent Run 1	141814-75805	#1 Foam Breaker Run 3	141814-75813
BSW #3 Combined Vent Run 2	141814-75806	Blank	141814-75814
BSW #3 Combined Vent Run 3	141814-75807	High Spike	141814-75815
#1 Vacuum Pump Run 1	141814-75808	Low Spike	141814-75816
#1 Vacuum Pump Run 2	141814-75809		

NCASI Method 94.02 – A portion of each of the liquid samples was transferred to a GC vial and spiked with internal standard, and was then analyzed on a GC/FID. Holding times for preparation and analysis were complied with.

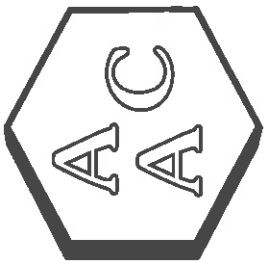
No problems were encountered during receiving, preparation, and/ or analysis of these samples. The test results included in this report meet all requirements of the NELAC Standards and/or AAC SOP# N.94.02.02.

I certify that this data is technically accurate, complete, and in compliance with the terms and conditions of the contract. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Director or his designee, as verified by the following signature. If you have any questions or require further explanation of data results, please contact the undersigned.

  
Marcus Hueppe  
Laboratory Director

This report consists of 7 pages.





# Atmospheric Analysis & Consulting, Inc.

## Laboratory Analysis Report

Client : Bighorn Environmental  
 Client Project Name : GP-Toledo 2014 BSW testing  
 AAC Project No. : 141814  
 Analyst : EG

Sampling Date : 11/05-06/2014  
 Receiving Date : 11/19/2014  
 Analysis Date : 11/20/2014  
 Reporting Date : 11/21/2014

### Methanol Analysis by NCASI Method 94.02

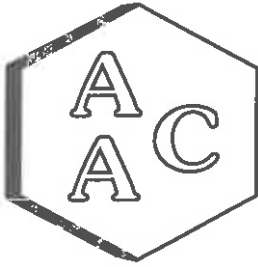
Client Sample ID	AAC Sample ID	Sample Volume (mL)	Methanol (ug/mL)	Methanol (ug/sample)	SRL (ug/sample)	Internal Standard (Cyclohexanol) % Recovery
BSW #2 Combined Vent Run 1	141814-75802	26.0	144	3740	13.0	97.9
BSW #2 Combined Vent Run 2	141814-75803	30.2	97.3	2940	15.1	101
BSW #2 Combined Vent Run 3	141814-75804	19.0	90.4	1720	9.50	99.6
BSW #3 Combined Vent Run 1	141814-75805	20.2	397	8020	10.1	98.7
BSW #3 Combined Vent Run 2	141814-75806	29.8	316	9420	14.9	100
BSW #3 Combined Vent Run 3	141814-75807	31.0	276	8550	15.5	100
#1 Vacuum Pump Run 1	141814-75808	23.3	40.8	950	11.7	101
#1 Vacuum Pump Run 2	141814-75809	22.7	40.8	925	11.4	101
#1 Vacuum Pump Run 3	141814-75810	25.0	40.9	1020	12.5	98.6
#1 Foam Breaker Run 1	141814-75811	23.5	386	9070	11.8	106
#1 Foam Breaker Run 2	141814-75812	41.2	372	15300	20.6	104
#1 Foam Breaker Run 3	141814-75813	29.2	271	7910	14.6	105
Blank	141814-75814	40.5	<SRL	<SRL	20.3	108
High Spike	141814-75815	41.0	121	4940	20.5	98.9
Low Spike	141814-75816	40.5	20.6	835	20.3	99.4

MRL - Method Reporting Limit = 0.500 ug/mL

SRL - Sampling Reporting Limit (ug/sample) = MRL (0.500 ug/mL) x Sample Volume (mL) x Analysis Dilution Factor

<SRL - Analyte was analyzed for but not detected at or above the SRL

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# Atmospheric Analysis & Consulting, Inc.

## Laboratory Analysis Report

Methanol Analysis by NCASI Method Q4 07

Client : Bighorn Environmental  
 Client Project Name : GP-Toledo 2014 BSW testing  
 AAC Project No. : 141814  
 Analyst : EG

Sampling Date : 11/05-06/2014  
 Receiving Date : 11/19/2014  
 Analysis Date : 11/20/2014  
 Reporting Date : 11/21/2014

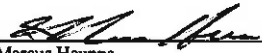
### Spiking Solution Evaluation

Client Sample ID	Sample Volume (mL)	Analyte	Measured Concentration (ug/sample)	Target Concentration (ug/sample)	Internal Standard % Recovery	% Recovery
High Spike	41.0	Methanol	4940	4740	108	104
Low Spike	40.5	Methanol	835	790	98.9	106
Client Sample ID	Sample Volume (mL)	Analyte	Measured Concentration (ug/ml)	Target Concentration (ug/ml)	Internal Standard % Recovery	% Recovery
Lab Spiking Solution (retained at Lab and analyzed with samples)	23.0	Methanol	15700	NA	10413	NA
Field Spiking Solution (went to field and back with samples)	23.0	Methanol	15800	15700	10739	101

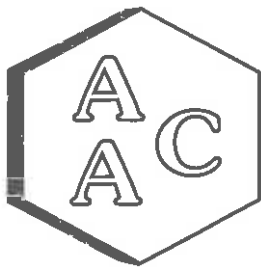
<SRL - Analyte was analyzed for but not detected at or above the SRL

Internal Standard recovery should be between 80-120%

The target concentration for the Spikes is based on the measured Field Spiking Solution concentration x the spiked amount

  
 Marcus Heuppe  
 Laboratory Director





# Atmospheric Analysis & Consulting, Inc.

## Quality Control/Quality Assurance Report

NCASI Method 94.02

FID Calibration Verification of the 9/18/2014 Calibration


Analysis Date : 11/20/2014  
Analyst : EG

Instrument ID : GC 6890 #1

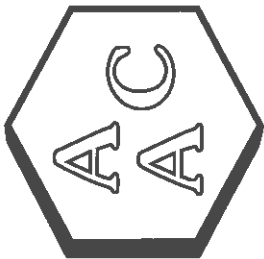
Sample ID	Analyte	Target Concentration (ug/mL)	Measured Concentration (ug/mL)	Percent Recovery (%)*
Opening CV	Methanol	500	475	95.0
	Cyclohexanol (IS)	20.0	19.4	96.9
Continuing CV	Methanol	500	502	100
	Cyclohexanol (IS)	20.0	19.9	99.4
Continuing CV	Methanol	500	527	105
	Cyclohexanol (IS)	20.0	20.2	101
Closing CV	Methanol	500	504	101
	Cyclohexanol (IS)	20.0	20.7	104
Second Source	Methanol	500	503	101
	Cyclohexanol (IS)	20.0	20.7	103

\* Must be 85 - 115 %

IS - Internal Standard

  
Marcus Hueppe  
Laboratory Director





# Atmospheric Analysis & Consulting, Inc.

## Quality Control/Quality Assurance Report NCASI Method 94.02

Analysis Date : 11/20/2014      Analyst : EG      Instrument ID : GC 6890 #1

### Laboratory Control Spike Analysis

Analyte	Sample Concentration (ug/mL)	Spike Concentration (ug/mL)	Measured Spike Concentration (ug/mL)	Measured Spike Dup Concentration (ug/mL)	Spike Recovery (%)*	Spike Dup Recovery (%)*	%RPD**
Methanol	0.000	250	254	256	102	102	0.7
Cyclohexanol (IS)	0.000	20.0	19.5	19.8	97.3	99	1.9

\* Must be 85-115%

\*\* Must be ≤ 25%

### Matrix Spike Analysis (141802-75804)

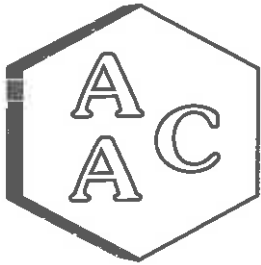
Analyte	Sample Concentration (ug/mL)	Spike Concentration (ug/mL)	Measured Spike Concentration (ug/mL)	Measured Spike Dup Concentration (ug/mL)	Spike Recovery (%)*	Spike Dup Recovery (%)*	%RPD**
Methanol	44.9	250	304	301	104	102	1.0
Cyclohexanol (IS)	0.000	20.0	19.9	19.3	99.4	96.3	3.2

\* Must be 75-125%

\*\* Must be ≤ 25%

Marcus Hueppe  
Laboratory Director

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# Atmospheric Analysis & Consulting, Inc.

## Quality Control/Quality Assurance Report NCASI Method 94.02

Analysis Date : 11/20/2014  
Analyst : EG

Instrument ID : GC 6890 #1

### Duplicate Analysis

Sample ID	Analyte	Sample Concentration (ug/mL)	Duplicate Concentration (ug/mL)	%RPD*
141802-75804	Methanol	90.4	89.3	1.2
	Cyclohexanol (IS)	19.9	20.6	3.4
141802-75803	Methanol	97.3	98.3	1.0
	Cyclohexanol (IS)	20.1	19.4	3.6
141802-75812	Methanol	372	374	0.5
	Cyclohexanol (IS)	20.7	20.4	1.9

\* Must be ≤15%

### Method Blank Analysis

Sample ID	Analyte	Concentration (ug/mL)	RL / SRL (ug/mL)
Method Blank	Methanol	<RL	0.500
Internal Standard (IS)	Target Concentration (ug/mL)	Measured Conc. (ug/mL)	% Recovery
Cyclohexanol (IS)	20.0	19.9	99.5

RL - Reporting Limit

SRL - Sample Reporting Limit

  
 \_\_\_\_\_  
 Marcus Hueppe  
 Laboratory Director





ATMOSPHERIC ANALYSIS & CONSULTING, INC.  
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AAC Project No. 141814

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**CHAIN OF CUSTODY/ ANALYSIS REQUEST FORM**

Client Name GP-Toledo		Project Name 2014 BSW Testing		Analysis Requested		Send report:	
Project Mgr (Print Name) Tim Homer		Project Number				Tim Homer	
Sampler's Name (Print Name) Tim Homer		Sampler's Signature				Attr: _____	
AAC Sample No.	Date Sampled	Time Sampled	Sample Type	Client Sample ID/Description	Type/No. of Containers		Phone#: _____ Fax#: _____
BSW #2 Combined Vent	Run 1	Run 1	Liq	75802	/	X	Send invoice to: _____
BSW #2 Combined Vent	Run 2	Run 2	"	75803	/	X	Attr: _____
BSW #2 Combined Vent	Run 3	Run 3	"	75804	/	X	P.O. # _____
BSW #3 Combined Vent	Run 1	Run 1	"	75805	/	X	Turnaround Time 24-Hr _____ 48-Hr _____
BSW #3 Combined Vent	Run 2	Run 2	"	75806	/	X	5 Day _____ Normal _____ X
BSW #3 Combined Vent	Run 3	Run 3	"	75807	/	X	Other (Specify) Special Instructions/remarks: 75814, 75815, 75816 Blank, High and Low Spikes also included
#1 Vacuum Pump	Run 1	Run 1	"	75808	/	X	
#1 Vacuum Pump	Run 2	Run 2	"	75809	/	X	
#1 Vacuum Pump	Run 3	Run 3	"	75810	/	X	
#1 Foam Breaker	Run 1	Run 1	"	75811	/	X	
#1 Foam Breaker	Run 2	Run 2	"	75812	/	X	
#1 Foam Breaker	Run 3	Run 3	"	75813	/	X	
Relinquished by (Signature): _____		Print Name: Tim Homer		Date/Time 11/15 13:00		Received by (signature): _____ Print Name	
Relinquished by (Signature): _____		Print Name: _____		Date/Time 11/19/14 1420		Received by (signature): _____ Print Name Tony DiCeglio	

FedEx 7.6°C

**APPENDIX B  
CALCULATIONS**



## CALCULATIONS

### FLOW RATES:

$$A = \text{Vent pipe cross-sectional area (ft}^2\text{)} = \pi r^2$$

$$P_{\text{bar}} = \text{Barometric pressure at measurement site (in Hg)}$$

$$P_g = \text{Stack static pressure (in Hg)} = \text{in. H}_2\text{O} \div 13.6 \text{ in H}_2\text{O/in. Hg}$$

$$P_s = \text{Absolute stack gas pressure (in. Hg)} = P_{\text{bar}} + P_g$$

$$t_d = \text{Temperature dry bulb (}^\circ\text{F)}$$

$$t_w = \text{Temperature wet bulb (}^\circ\text{F)}$$

$$e'' = \text{Stack vapor pressure (in. Hg)} \\ = (0.00000608746 \times t_w^3) - (0.00100431 \times t_w^2) + (0.0756026 \times t_w) - 1.69343$$

$$\% \text{H}_2\text{O} = [e'' - (P_s - e'')(t_d - t_w)] \div (2800 - (1.3 \times t_w)) \div P_s \times 100$$

$$\text{MD} = \text{Molecular Density} = (100 - \% \text{H}_2\text{O}) \div 100$$

$$M_d = \text{Molecular weight of dry stack gas (lb/lb-mole)} \\ = (\% \text{CO}_2 \times 0.44) + (\% \text{O}_2 \times 0.32) + [(\% \text{CO} + \% \text{N}_2) \times 0.28]$$

$$M_s = \text{Molecular weight of wet stack gas (lb/lb-mole)} \\ = M_d \times (\text{MD}) + 18 \text{ lb/lb-mole} \times (1 - \text{MD})$$

$$C_p = \text{Pitot tube coefficient}$$

$$(\sqrt{\square p})_{\text{avg}} = \text{Average square root velocity head of stack gas (in. H}_2\text{O)}$$

$$T_s = \text{Absolute stack temperature (}^\circ\text{R)} = 460 + t_d$$

$$V_s = \text{Average stack gas velocity (ft}^3\text{/min.)} \\ = 85.49 \text{ ft/sec} \times 60 \text{ sec/min} \times C_p \times (\sqrt{\square p})_{\text{avg}} \times \text{sqrt}(T_s \sqrt{(P_s \times M_s)})$$

$$Q_{\text{sd}} = \text{Stack gas dry molecular flow rate corrected to standard conditions}$$

$$(\text{dscfm}) = \text{MD} \times V_s \times A \times (528^\circ\text{R} \div T_s) \times (P_s \div 29.92'' \text{ Hg})$$

$$Q_{\text{ac}} = \text{Stack gas flow rate at actual conditions (acfm)} = V_s \times A$$

### **EMISSION RATES:**

ODT = Oven Dry Tons of pulp production

$$\frac{\text{lb MeOH}}{\text{hour}} = (C_{\text{gas}} \div 1,000,000) \times (1 \text{ lb-mole} \div 385 \text{ ft}^3) \times 32.04 \text{ lb MeOH/lb-mole} \times Q_{\text{sd}} \times 60 \text{ min/hr}$$

$$\frac{\text{lb MeOH}}{\text{ODT}} = \frac{\text{lb MeOH}}{\text{hour}} \div \frac{\text{ODT}}{\text{hour}}$$

# COMPLIANCE TEST - MANUAL CALCULATIONS SHEET

CLIENT: GP-Toledo  
 PROJECT: #1 BSW Foam Breaker  
 RUN TIME CHECKED: 9:10-10:10  
 DATE: 11/6/14  
 CHECKED BY: YH

## FLOW RATES: 40CFR 60 APP. A, Method 2

$$r = \text{Stack radius (ft)} = (\text{diameter (in.)} \div 12) \div 2 = \underline{15.75} - .6563$$

$$A = \text{Stack cross-sectional area (ft}^2\text{)} = \pi r^2 = 3.14159 \times (.6563)^2 = \underline{1.353}$$

$$P_{\text{bar}} = \text{Barometric pressure at measurement site (in Hg)} = \underline{29.81}$$

$$P_g = \text{Stack static pressure (in Hg)} = \text{in. H}_2\text{O} \div 13.6 \text{ in H}_2\text{O/in. Hg} = \left( \frac{-0.6}{13.6} \right) = \underline{\hspace{2cm}}$$

$$P_s = \text{Absolute stack gas pressure (in. Hg)} = P_{\text{bar}} + P_g = \underline{29.81} + \underline{-0.0044} = \underline{29.806}$$

$$t_d = \text{Temperature dry bulb (}^\circ\text{F)} = \underline{115}$$

$$t_w = \text{Temperature wet bulb (}^\circ\text{F)} = \underline{115}$$

$$e'' = \text{Stack vapor pressure (in. Hg)}$$

$$= (0.00000608746 \times t_w^3) - (0.00100431 \times t_w^2) + (0.0756026 \times t_w) - 1.69343$$

$$= (0.00000608746 \times \underline{115}^3) - (0.00100431 \times \underline{115}^2) + (0.0756026 \times \underline{115}) - 1.69343 = \underline{2.977}$$

9.258

13.222

8.694

$$\% \text{H}_2\text{O} = e'' - [(P_s - e'')(t_d - t_w)] \div (2800 - (1.3 \times t_w)) \div P_s \times 100$$

$$= \frac{2.977 - [((29.806 - 2.977) \times (115 - 115))]}{(2800 - (1.3 \times 115))} \div (29.806) \times 100 = \underline{9.99}$$

$$\text{MD} = \text{Molecular Density} = (100 - \% \text{H}_2\text{O}) \div 100 = \frac{(100 - 9.99)}{100} = \underline{.9001}$$

$$(\% \text{CO} + \% \text{N}_2) = 100 - \% \text{CO}_2 - \% \text{O}_2 = 100 - (17.7) - (0) = \underline{82.3}$$

$$M_d = \text{Molecular weight of dry stack gas (lb/lb-mole)} = (\% \text{CO}_2 \times 0.44) + (\% \text{O}_2 \times 0.32) + [(\% \text{CO} + \% \text{N}_2) \times 0.28]$$

$$= (0 \times 0.44) + (17.7 \times 0.32) + ((82.3) \times 0.28) = \underline{28.706}$$

$$M_s = \text{Molecular weight of wet stack gas (lb/lb-mole)} = M_d \times (\text{MD}) + (18 \text{ lb/lb-mole} \times (1 - \text{MD}))$$

$$= \underline{28.708} \times (\underline{.9001}) + (18 \text{ lb/lb-mole} \times (1 - \underline{.9001})) = \underline{27.638}$$

$$C_p = \text{Pitot tube coefficient} = \underline{.84}$$

$$(\sqrt{\Delta p})_{\text{avg}} = \text{Average square root velocity head of stack gas (in. H}_2\text{O)} = \underline{.4462}$$

$$T_s = \text{Absolute stack temperature (}^\circ\text{R)} = 460 + t_d = 460 + \underline{115} = \underline{575}$$

$$V_s = \text{Average stack gas velocity (ft}^2\text{/min.)}$$

$$= 85.49 \text{ ft/sec} \times 60 \text{ sec/min} \times C_p \times (\sqrt{\Delta p})_{\text{avg}} \times \text{sqrt}(T_s \div (P_s \times M_s))$$

$$= (85.49) \times (60) \times (\underline{.84}) \times (\underline{.4462}) \times \text{sqrt}(\underline{575}) = \underline{1606.2}$$

(27.638 x 29.806)

$$Q_{\text{sd}} = \text{Dry stack gas flow rate at standard conditions} = MD \times V_s \times A \times (528^\circ\text{R} \div T_s) \times (P_s \div 29.92 \text{ Hg})$$

$$= \underline{.9001} \times \underline{1606.2} \times \underline{1.353} \times (528^\circ\text{R}) \times (\underline{29.806}) = \underline{1789.4}$$

(575) x (29.92)      ,028

$$Q = \text{Stack gas flow rate at actual conditions (acfm)} = V_s \times A = (\underline{1606.2}) \times (\underline{1.353}) = \underline{2173.2}$$

$$\text{Combined Stack Flow} = \underline{\hspace{2cm}} + \underline{\hspace{2cm}} + \underline{\hspace{2cm}} = \underline{\hspace{2cm}}$$

### EMISSIONS:

$$\text{Molecular Weight (MW)} = \frac{\text{lb}}{\text{lb mole}}$$

$$\text{MeOH} = 32.04$$

$$\frac{\text{lb Pollutant}}{\text{hour}} = (C_{\text{gas}} \div 1,000,000) \times (11 \text{ lb-mole} \div 385 \text{ ft}^3) \times \text{MW} \times Q_{\text{sd}} \times 60 \text{ min/hr}$$

$$= \frac{(\underline{278.36}) \times (\underline{32.04}) \times (\underline{\hspace{1cm}}) \times (\underline{1789.4}) \times (60)}{1,000,000 \times 385} = \underline{2.486}$$

$$\frac{\text{lb Pollutant}}{\text{ODTP}} = \frac{\text{lb Pollutant}}{\text{hour}} \div \frac{\text{ODTP}}{\text{hour}}$$

$$= \frac{(\underline{2.486})}{(\underline{16.08})} = \underline{.1546}$$

$$\text{Meter Vol (dscl)} = \text{Meter vol} * ((273+20)/(273+\text{Meter temp})) * \text{Meter Y} * (\text{Meter Pressure}/29.92) = \underline{\hspace{2cm}}$$

$23.992 \times 1.006 \times \frac{293}{288.2} \cdot \frac{29.81}{29.92} \approx 24.448$

$$\text{MeOH ppm} = \frac{\text{mg/sample}}{\text{MeOH MW}} \cdot \frac{24.04}{\text{Meter Vol (dscl)}} = \frac{9070}{37104} \cdot \frac{24.04}{24.448} \approx 278.36$$

# COMPLIANCE TEST - MANUAL CALCULATIONS SHEET

CLIENT: GP-Triado  
 PROJECT: #1 BSW Vacuum Pump  
 RUN TIME CHECKED: 910-1010  
 DATE: 11/6/14  
 CHECKED BY: TP

**FLOW RATES: 40CFR 60 APP. A, Method 2**

$r = \text{Stack radius (ft)} = (\text{diameter (in.)} \div 12) \div 2 = \underline{10} = \underline{.4167}$

$A = \text{Stack cross-sectional area (ft}^2\text{)} = \pi r^2 = 3.14159 \times (\underline{.4167})^2 = \underline{.5454}$

$P_{\text{bar}} = \text{Barometric pressure at measurement site (in Hg)} = \underline{29.81}$

$P_g = \text{Stack static pressure (in Hg)} = \text{in. H}_2\text{O} \div 13.6 \text{ in H}_2\text{O/in. Hg} = (\underline{0}) \div 13.6 = \underline{0}$

$P_s = \text{Absolute stack gas pressure (in. Hg)} = P_{\text{bar}} + P_g = \underline{29.81} + \underline{0} = \underline{29.81}$

$t_d = \text{Temperature dry bulb (}^\circ\text{F)} = \underline{101.3}$

$t_w = \text{Temperature wet bulb (}^\circ\text{F)} = \underline{97.7}$

$e'' = \text{Stack vapor pressure (in. Hg)}$

$= (0.00000608746 \times t_w^3) - (0.00100431 \times t_w^2) + (0.0756026 \times t_w) - 1.69343$

$= (0.00000608746 \times \underline{97.7}^3) - (0.00100431 \times \underline{97.7}^2) + (0.0756026 \times \underline{97.7}) - 1.69343 = \underline{1.784}$   
 $\frac{5.677}{9.586} \quad \frac{7.386}{7.386}$

$\%H_2O = e'' - [(P_s - e'') \times (t_d - t_w)] \div (2800 - (1.3 \times t_w)) \div P_s \times 100$   
 $= \frac{1.784 - [(29.81 - 1.784) \times (101.3 - 97.7)]}{(2800 - (1.3 \times 97.7))} \div (29.81) \times 100 = \underline{5.861}$

$MD = \text{Molecular Density} = (100 - \%H_2O) \div 100 = (100 - \underline{5.861}) \div 100 = \underline{.94139}$

$(\%CO + \%N_2) = 100 - \%CO_2 - \%O_2 = 100 - (\underline{17.8}) - (\underline{0}) = \underline{82.3}$

$M_d = \text{Molecular weight of dry stack gas (lb/lb-mole)} = (\%CO_2 \times 0.44) + (\%O_2 \times 0.32) + [(\%CO + \%N_2) \times 0.28]$   
 $= (\underline{0} \times 0.44) + (\underline{17.7} \times 0.32) + ((\underline{82.3}) \times 0.28) = \underline{28.704}$

$M_s = \text{Molecular weight of wet stack gas (lb/lb-mole)} = M_d \times (MD) + (18 \text{ lb/lb-mole} \times (1 - MD))$

$$= \underline{.94139} \times (\underline{28.102}) + (18 \text{ lb/lb-mole} \times (1 - \underline{.94139})) = \underline{28.082}$$

$$C_p = \text{Pitot tube coefficient} = \underline{.84}$$

$$(\sqrt{\Delta p})_{\text{avg}} = \text{Average square root velocity head of stack gas (in. H}_2\text{O)} = \underline{.8833}$$

$$T_s = \text{Absolute stack temperature (}^\circ\text{R)} = 460 + t_d = 460 + \underline{101.3} = \underline{561.3}$$

$$V_s = \text{Average stack gas velocity (ft}^2\text{/min.)}$$

$$= 85.49 \text{ ft/sec} \times 60 \text{ sec/min} \times C_p \times (\sqrt{\Delta p})_{\text{avg}} \times \text{sqrt}(T_s \div (P_s \times M_s))$$

$$= (85.49) \times (60) \times (\underline{.84}) \times (\underline{.8833}) \times \text{sqrt}(\underline{561.3} \div (\underline{28.082} \times \underline{29.81})) = \underline{3116.4}$$

$$Q_{sd} = \text{Dry stack gas flow rate at standard conditions} = MD \times V_s \times A \times (528^\circ\text{R} \div T_s) \times (P_s \div 29.92 \text{ Hg})$$

$$= \underline{.94139} \times \underline{.5454} \times \underline{3116.4} \times (528^\circ\text{R}) \times (\underline{29.81}) \div (\underline{561.3}) \times (29.92) = \underline{1499.6}$$

$$Q = \text{Stack gas flow rate at actual conditions (acfm)} = V_s \times A = (\underline{3116.4}) \times (\underline{.5454}) = \underline{1699.7}$$

$$\text{Combined Stack Flow} = \underline{\hspace{2cm}} + \underline{\hspace{2cm}} + \underline{\hspace{2cm}} + \underline{\hspace{2cm}} = \underline{\hspace{2cm}}$$

**EMISSIONS:**

$$\text{Molecular Weight (MW)} = \frac{\text{lb}}{\text{lb mole}}$$

$$\text{MeOH} = 32.04$$

$$\frac{\text{lb Pollutant}}{\text{hour}} = (C_{\text{gas}} \div 1,000,000) \times (1 \text{ lb-mole} \div 385 \text{ ft}^3) \times \text{MW} \times Q_{sd} \times 60 \text{ min/hr}$$

$$= \frac{(\underline{28.01}) \times (\underline{32.04}) \times (\underline{\hspace{1cm}}) \times (\underline{1499.6}) \times (60)}{1,000,000 \times 385} = \underline{1.2164}$$

$$\frac{\text{lb Pollutant}}{\text{ODTP}} = \frac{\text{lb Pollutant}}{\text{hour}} \div \frac{\text{ODTP}}{\text{hour}}$$

$$= \frac{(\underline{1.2164})}{(\underline{1608})} = \underline{.000757}$$

$$\text{Meter Vol (dscl)} = \text{Meter vol} \times ((273+20)/(273+\text{Meter temp})) \times \text{Meter Y} \times (\text{Meter Pressure}/29.92) = \underline{\hspace{2cm}}$$

$$24.029 \times 1.006 \times \frac{293}{2862} \times \frac{29.81}{29.92} = 24.657$$

$$\frac{950}{32.04} \times \frac{24.04}{24.657} = 28.91$$

# COMPLIANCE TEST - MANUAL CALCULATIONS SHEET

CLIENT: GP-Tulelec  
 PROJECT: #2 BSW  
 RUN TIME CHECKED: 1400-1500  
 DATE: 11/5/14  
 CHECKED BY: YR

## FLOW RATES: 40CFR 60 APP. A, Method 2

$r = \text{Stack radius (ft)} = (\text{diameter (in.)} \div 12) \div 2 = \underline{1.6}$

$A = \text{Stack cross-sectional area (ft}^2) = \pi r^2 = 3.14159 \times (\underline{1.67})^2 = \underline{1.396}$

$P_{\text{bar}} = \text{Barometric pressure at measurement site (in Hg)} = \underline{29.76}$

$P_g = \text{Stack static pressure (in Hg)} = \text{in. H}_2\text{O} \div 13.6 \text{ in H}_2\text{O/in. Hg} = (\underline{-1.74}) \div \underline{13.6} = \underline{.05414}$

$P_s = \text{Absolute stack gas pressure (in. Hg)} = P_{\text{bar}} + P_g = \underline{29.76} + \underline{.0544} = \underline{29.7056}$

$t_d = \text{Temperature dry bulb (}^\circ\text{F)} = \underline{130.1}$

$t_w = \text{Temperature wet bulb (}^\circ\text{F)} = \underline{125.6}$

$e'' = \text{Stack vapor pressure (in. Hg)}$

$= (0.00000608746 \times t_w^3) - (0.00100431 \times t_w^2) + (0.0756026 \times t_w) - 1.69343$

$= (0.00000608746 \times \underline{125.6}^3) - (0.00100431 \times \underline{125.6}^2) + (0.0756026 \times \underline{125.6}) - 1.69343 = \underline{4.022}$

$\frac{12.062}{12.062}$ 
 $\frac{15.843}{15.843}$ 
 $\frac{9.496}{9.496}$

$\%H_2O = e'' - [(P_s - e'') \times (t_d - t_w)] \div (2800 - (1.3 \times t_w)) \div P_s \times 100$

$= \frac{\underline{4.022} - [(\underline{29.7056} - \underline{4.022}) \times (\underline{130.1} - \underline{125.6})]}{(2800 - (1.3 \times \underline{125.6}))} \div (\underline{29.7056}) \times 100 = \underline{13.389}$

$MD = \text{Molecular Density} = (100 - \%H_2O) \div 100 = \frac{(100 - \underline{13.389})}{100} = \underline{.86611}$

$(\%CO + \%N_2) = 100 - \%CO_2 - \%O_2 = 100 - (\underline{14.49}) - (\underline{2}) = \underline{80.51}$

$M_d = \text{Molecular weight of dry stack gas (lb/lb-mole)} = (\%CO_2 \times 0.44) + (\%O_2 \times 0.32) + [(\%CO + \%N_2) \times 0.28]$

$= (\underline{2} \times 0.44) + (\underline{14.49} \times 0.32) + ((\underline{80.51}) \times 0.28) = \underline{24.777}$

$M_s = \text{Molecular weight of wet stack gas (lb/lb-mole)} = M_d \times (MD) + (18 \text{ lb/lb-mole} \times (1 - MD))$

$$= 28,777 \times (.8661) + (18 \text{ lb/lb-mole} \times (1 - .8661)) = 27,336$$

$$C_p = \text{Pitot tube coefficient} = .84$$

$$(\sqrt{\Delta p})_{\text{avg}} = \text{Average square root velocity head of stack gas (in. H}_2\text{O)} = .6437$$

$$T_s = \text{Absolute stack temperature (}^\circ\text{R)} = 460 + t_d = 460 + 130.1 = 590.1$$

$$V_s = \text{Average stack gas velocity (ft}^2\text{/min.)}$$

$$= 85.49 \text{ ft/sec} \times 60 \text{ sec/min} \times C_p \times (\sqrt{\Delta p})_{\text{avg}} \times \text{sqrt}(T_s \div (P_s \times M_s))$$

$$= (85.49) \times (60) \times (.84) \times (.6437) \times \text{sqrt}(590.1) = 2364.3$$

(27.336 x 29.7056)

$$Q_{sd} = \text{Dry stack gas flow rate at standard conditions} = MD \times V_s \times A \times (528^\circ\text{R} \div T_s) \times (P_s \div 29.92 \text{ Hg})$$

$$= .8661 \times 1.396 \times 2364.3 \times (528^\circ\text{R}) \times (29.7056) = 2539.5$$

(590.1) x (29.92)

$$Q = \text{Stack gas flow rate at actual conditions (acfm)} = V_s \times A = (2364.3) \times (1.396) = 3300.6$$

$$\text{Combined Stack Flow} = \underline{\hspace{2cm}} + \underline{\hspace{2cm}} + \underline{\hspace{2cm}} = \underline{\hspace{2cm}}$$

**EMISSIONS:**

$$\text{Molecular Weight (MW)} = \frac{\text{lb}}{\text{lb mole}}$$

$$\text{MeOH} = 32.04$$

$$\frac{\text{lb Pollutant}}{\text{hour}} = (C_{\text{gas}} \div 1,000,000) \times (1 \text{ lb-mole} \div 385 \text{ ft}^3) \times \text{MW} \times Q_{sd} \times 60 \text{ min/hr}$$

$$= \frac{(118.50)}{1,000,000} \times \frac{(32.04)}{385} \times (1) \times (2539.5) \times (60) = 1.502$$

$$\frac{\text{lb Pollutant}}{\text{ODTP}} = \frac{\text{lb Pollutant}}{\text{hour}} \div \frac{\text{ODTP}}{\text{hour}}$$

$$= \frac{(1.502)}{(14.67)} = .0924$$

$$\text{Meter Vol (dscl)} = \text{Meter vol} \times ((273+20)/(273+\text{Meter temp})) \times \text{Meter Y} \times (\text{Meter Pressure}/29.92) =$$

$$= 24.007 \times 1.01 \times \frac{293}{298.4} \times \frac{29.76}{29.92} = 23.68$$

$$\text{MeOH ppm} = \frac{3740}{32.04} \times \frac{24.04}{23.68} = 118.50$$



# COMPLIANCE TEST - MANUAL CALCULATIONS SHEET

CLIENT: GP-Tulco  
 PROJECT: #2 BSW MUD  
 RUN TIME CHECKED: 955-1055  
 DATE: 11/5/14  
 CHECKED BY: YD

## FLOW RATES: 40CFR 60 APP. A, Method 2

$r = \text{Stack radius (ft)} = (\text{diameter (in.)} \div 12) \div 2 = \underline{16} \text{ . } \underline{67}$

$A = \text{Stack cross-sectional area (ft}^2) = \pi r^2 = 3.14159 \times (\underline{16.67})^2 = \underline{1,396}$

$P_{\text{bar}} = \text{Barometric pressure at measurement site (in Hg)} = \underline{29.76}$

$P_g = \text{Stack static pressure (in Hg)} = \text{in. H}_2\text{O} \div 13.6 \text{ in H}_2\text{O/in. Hg} = (\underline{-1.01}) \div \underline{13.6} = \underline{-0.0735}$

$P_s = \text{Absolute stack gas pressure (in. Hg)} = P_{\text{bar}} + P_g = \underline{29.76} + \underline{-0.0735} = \underline{29.759}$

$t_d = \text{Temperature dry bulb (}^\circ\text{F)} = \underline{141.6}$

$t_w = \text{Temperature wet bulb (}^\circ\text{F)} = \underline{134.6}$

$e'' = \text{Stack vapor pressure (in. Hg)}$

$= (0.00000608746 \times t_w^3) - (0.00100431 \times t_w^2) + (0.0756026 \times t_w) - 1.69343$

$= (0.00000608746 \times \underline{134.6}^3) - (0.00100431 \times \underline{134.6}^2) + (0.0756026 \times \underline{134.6}) - 1.69343 = \underline{5.133}$

$\%H_2O = e'' - [(P_s - e'') \times (t_d - t_w)] \div (2800 - (1.3 \times t_w)) \div P_s \times 100$

$= \underline{5.133} - [((\underline{29.759} - \underline{5.133}) \times (\underline{141.6} - \underline{134.6}))] \div (\underline{2800} - (1.3 \times \underline{134.6})) \div \underline{29.759} \times 100 = \underline{17.028}$

$MD = \text{Molecular Density} = (100 - \%H_2O) \div 100 = (\underline{100 - 17.028}) \div \underline{100} = \underline{0.82972}$

$(\%CO + \%N_2) = 100 - \%CO_2 - \%O_2 = 100 - (\underline{9.98}) - (\underline{0}) = \underline{90.02}$

$M_d = \text{Molecular weight of dry stack gas (lb/lb-mole)} = (\%CO_2 \times 0.44) + (\%O_2 \times 0.32) + [(\%CO + \%N_2) \times 0.28]$

$= (\underline{0}) \times 0.44 + (\underline{9.98} \times 0.32) + (\underline{90.02} \times 0.28) = \underline{28.663}$

$M_s = \text{Molecular weight of wet stack gas (lb/lb-mole)} = M_d \times (MD) + (18 \text{ lb/lb-mole} \times (1 - MD))$

$$= \underline{28.663} \times (\underline{.82972}) + (18 \text{ lb/lb-mole} \times (1 - \underline{.82972})) = \underline{26.244}$$

$$C_p = \text{Pitot tube coefficient} = \underline{.84}$$

$$(\sqrt{\square p})_{\text{avg}} = \text{Average square root velocity head of stack gas (in. H}_2\text{O)} = \underline{.1657}$$

$$T_s = \text{Absolute stack temperature (}^\circ\text{R)} = 460 + t_d = 460 + \underline{141.6} = \underline{601.6}$$

$$V_s = \text{Average stack gas velocity (ft}^2\text{/min.)}$$

$$= 85.49 \text{ ft/sec} \times 60 \text{ sec/min} \times C_p \times (\sqrt{\square p})_{\text{avg}} \times \text{sqrt}(T_s \div (P_s \times M_s))$$

$$= (85.49) \times (60) \times (\underline{.84}) \times (\underline{.1657}) \times \text{sqrt}(\underline{601.6} \div (\underline{26.244} \times \underline{29.759})) = \underline{619.57}$$

$$Q_{\text{sd}} = \text{Dry stack gas flow rate at standard conditions} = MD \times V_s \times A \times (528^\circ\text{R} \div T_s) \times (P_s \div 29.92 \text{ Hg})$$

$$= \underline{.82972} \times \underline{1.396} \times \underline{619.57} \times (528^\circ\text{R}) \times (\underline{29.759} \div (\underline{601.6} \times (29.92))) = \underline{626.5}$$

$$Q = \text{Stack gas flow rate at actual conditions (acfm)} = V_s \times A = (\underline{619.57}) \times (\underline{1.396}) = \underline{864.9}$$

$$\text{Combined Stack Flow} = \underline{\hspace{2cm}} + \underline{\hspace{2cm}} + \underline{\hspace{2cm}} + \underline{\hspace{2cm}} = \underline{\hspace{2cm}}$$

### EMISSIONS:

$$\text{Molecular Weight (MW)} = \frac{\text{lb}}{\text{lb mole}}$$

$$\text{MeOH} = 32.04$$

$$\frac{\text{lb Pollutant}}{\text{hour}} = (C_{\text{gas}} \div 1,000,000) \times (1 \text{ lb-mole} \div 385 \text{ ft}^3) \times \text{MW} \times Q_{\text{sd}} \times 60 \text{ min/hr}$$

$$= \frac{(\underline{251.085})}{1,000,000} \times \frac{(\underline{32.04})}{385} \times (1) \times (\underline{626.5}) \times (60) = \underline{.785}$$

$$\frac{\text{lb Pollutant}}{\text{ODTP}} = \frac{\text{lb Pollutant}}{\text{hour}} \div \frac{\text{ODTP}}{\text{hour}}$$

$$= \frac{(\underline{.785})}{(\underline{16163})} = \underline{.047}$$

$$\text{Meter Vol (dscl)} = \text{Meter vol} * ((273+20)/(273+\text{Meter temp})) * \text{Meter Y} * (\text{Meter Pressure}/29.92) = \underline{\hspace{2cm}}$$

$$23,995 \times 1.01 \times \frac{292}{294.7} \times \frac{29.16}{29.92} = 23,966$$

$$\text{MeOH ppm} = \frac{352.2}{32104} \times \frac{24.04}{23.966} = 251.085$$

**APPENDIX C  
QUALITY RECORDS**



## Thermo cal 10-14-07

8/18/2014									
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 3' #1 Probe</b>	32	0		208	-2		448	-2	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 3' #2 Probe</b>	34	2		208	-2		449	-1	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 4' Hi-Temp Probe</b>	34	2		208	-2		452	2	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 4' #1</b>	34	2		206	-4		446	-4	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 5' Probe</b>	34	2		208	-2		448	-2	
NIST Thermometer I.D.:		E93-486							
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 6' #1 Probe</b>	36	4		206	-4		446	-4	
NIST Thermometer I.D.:		E93-486							
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 6' #2 Probe</b>	34	2		206	-4		447	-3	
NIST Thermometer I.D.:		E93-486							
Calibration date:		2/26/2013							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST		N/A	6.9		N/A	6.9		N/A	6.9
		0			0			0	
NIST Thermometer I.D.:		E93-486							
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 6' #4 Probe</b>	33	1		206	-4		453	3	
NIST Thermometer I.D.:		E93-486							

Thermo cal 10-14-07

Calibration date:		2/19/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST		N/A	6.9		N/A	6.9		N/A	6.9
		0			0			0	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>MFB 7' #1 Probe</b>	31	-1		207	-3		453	3	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 7' #2 Probe</b>	31	-1		207	-3		450	0	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 8' #1</b>	32	0		207	-3		451	1	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 9' #1 Probe</b>	33	1		208	-2		447	-3	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 10' #1 Probe</b>	31	-1		207	-3		448	-2	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05	450	N/A	13.65
<b>BH 10' #2 Probe</b>	34	2		207	-3		445	-5	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	212	N/A	10.08	450	N/A	13.65
<b>BH 16' #1 Probe</b>	30	-2		209	-3		449	-1	
Calibration date:		8/18/2014							
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	212	N/A	10.08	450	N/A	13.65
<b>BH 16' #2 Probe</b>	29	-3		210	-2		453	3	



<b>BH Filter Oven #4</b>	31	-1		205	-5	
<b>Calibration date:</b>						
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05
	32	0		207	-3	
<b>Meter Box #906017</b>						
<b>Calibration date:</b>						
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05
	32	0		207	-3	
<b>Meter Box #0610022</b>						
<b>Calibration date:</b>						
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05
	34	2		206	-4	
<b>Meter Box #0307031</b>						
<b>Calibration date:</b>						
Temp.	Test	Difference	Acceptance	Test	Difference	Acceptance
Device	Value	(°K)	Criteria (+/-)	Value	(°K)	Criteria (+/-)
NIST	32	N/A	7.38	210	N/A	10.05
	30			208		
<b>Meter Box #1208030</b>						
		-2			-2	



PRE

19-Sep-14

**DRY GAS METER**

Model:	<b>623</b>			
Serial #:	<b>805005 Box 2</b>		<b>High Flow</b>	
Location:	<b>GEG</b>			
Date	9/19/2014	9/19/2014	9/19/2014	9/19/2014
Console leak check (cfm)	0	0	0	0
Orifice setting (^h)	1.575	2.362	3.15	3.937
Barometric pressure (in. Hg)	27.77	27.77	27.77	27.77
<b>Volume</b>				
beginning reading	0	0	0	0
ending reading	0.3474257	0.4048121	0.48314	0.5309914
Total Volume (Vd) ft3	0.3474257	0.4048121	0.48314	0.5309914
<b>Temperature (deg F)</b>				
beginning inlet	66.2	75.2	77	78.8
ending inlet	75.2	77	78.8	80.6
beginning outlet	66.2	80.6	77	78.8
ending outlet	75.2	77	78.8	80.6
average outlet temp (Tmo)	70.7	78.8	77.9	79.7
average temp (Tm)	70.7	77.45	77.9	79.7

**CALIBRATION METER**

	<b>Yc</b>	<b>1.006</b>	<b>1.006</b>	<b>1.006</b>	<b>1.006</b>
<b>Volume</b>					
beginning reading		467.160	467.510	467.920	468.4
ending reading		467.510	467.920	468.400	468.92
Total Volume (Vc) ft3		0.35	0.41	0.48	0.52
<b>Temperature</b>					
beginning		69.8	71.6	71.6	71.6
ending		71.6	71.6	71.6	71.6
average temp (Tc)		70.7	71.6	71.6	71.6
<b>Time (min)</b>		11	11	11	10
	<b>Y:</b>	1.009	1.023	1.002	0.989
<b>Difference from Average:</b>		0.003	0.017	-0.003	-0.017

**AVERAGE  
1.006**

**Y Acceptance criteria: +/- 0.02 From Average**

00006

PRIZ

0.0353147

19-Aug-14

**DRY GAS METER**

Model: **623**  
 Serial #: **805005 BOX 1** High Flow  
 Location: **GEG**  
 Date: **8/19/2014 8/19/2014 8/19/2014 8/19/2014**  
 Console leak check (cfm) **0 0 0 0**  
 Orifice setting (^h) **1.575 2.362 3.15 3.937**  
 Barometric pressure (in. Hg) **27.77 27.77 27.77 27.77**  
**Volume**  
 beginning reading **0 0 0 0**  
 ending reading **1.1689509 1.5748224 2.1676498 2.3550647**  
 Total Volume (Vd) ft3 **1.1689509 1.5748224 2.1676498 2.3550647**  
**Temperature (deg F)**  
 beginning inlet **66 69 73 76**  
 ending inlet **69 73 76 77**  
 beginning outlet **66 69 73 76**  
 ending outlet **69 73 76 77**  
 average outlet temp (Tmo) **67.5 71 74.5 76.5**  
 average temp (Tm) **67.5 71 74.5 76.5**

**CALIBRATION METER**

**Yc 1.006 1.006 1.006 1.006**  
**Volume**  
 beginning reading **459.560 460.730 462.310 464.48**  
 ending reading **460.730 462.310 464.480 466.84**  
 Total Volume (Vc) ft3 **1.17 1.58 2.17 2.36**  
**Temperature**  
 beginning **66 67 67 67**  
 ending **67 67 67 67**  
 average temp (Tc) **66.5 67 67 67**

**Time (min)**  
**10 10 12 12**  
**AVERAGE**  
**1.010**

**Y: 1.004 1.010 1.012 1.015**  
**Difference from Average: -0.006 0.000 0.002 0.005**

Y Acceptance criteria: +/- 0.02 From Average

00007

POST

20-Nov-14

**DRY GAS METER**

Model: **623**      **805005 BOX 1**      **High Flow**      **0.0353147**  
Serial #:      **805005 BOX 1**

Location: **GEG**  
Date: **11/20/2014**      **11/20/2014**      **11/20/2014**      **11/20/2014**  
Console leak check (cfm): **0**      **0**      **0**      **0**  
Orifice setting (^h): **1.575**      **2.362**      **3.15**      **3.937**  
Barometric pressure (in. Hg): **27.75**      **27.75**      **27.75**      **27.75**

**Volume**  
beginning reading: **0**      **0**      **0**      **0**  
ending reading: **1.1969907**      **1.5976004**      **1.8181758**      **1.9046967**  
Total Volume (Vd) ft3: **1.1969907**      **1.5976004**      **1.8181758**      **1.9046967**

**Temperature (deg F)**  
beginning inlet: **63**      **58**      **61**      **63**  
ending inlet: **58**      **61**      **63**      **64**  
beginning outlet: **63**      **58**      **61**      **63**  
ending outlet: **58**      **61**      **63**      **64**  
average outlet temp (Tmo): **60.5**      **59.5**      **62**      **63.5**  
average temp (Tm): **60.5**      **59.5**      **62**      **63.5**

**3003 CALIBRATION METER**

**Volume**      **Yc**      **1.006**      **1.006**      **1.006**      **1.006**  
beginning reading: **76.525**      **77.730**      **79.345**      **81.17**  
ending reading: **77.730**      **79.345**      **81.170**      **83.085**  
Total Volume (Vc) ft3: **1.205**      **1.615**      **1.825**      **1.915**  
**Temperature**  
beginning: **51**      **56**      **55**      **55**  
ending: **56**      **55**      **55**      **56**  
average temp (Tc): **53.5**      **55.5**      **55**      **55.5**

**Time (min)**      **10**      **10**      **10**      **10**  
**AVERAGE**  
**1.018**

**Y Acceptance criteria: +/- 0.02 From Average**

Post

20-Nov-14

**DRY GAS METER**

Model: **623**      **805005 Box 2**      **High Flow**      **0.0353147**  
Serial #:      **805005 Box 2**

Location: **GEG**

Date: **11/20/2014**      **11/20/2014**      **11/20/2014**      **11/20/2014**

Console leak check (cfm)      **0**      **0**      **0**      **0**  
Orifice setting (^h)      **1.575**      **2.362**      **3.15**      **3.937**  
Barometric pressure (in. Hg)      **27.75**      **27.75**      **27.75**      **27.75**

**Volume**  
beginning reading      **0**      **0**      **0**      **0**  
ending reading      **0.6269413**      **0.7423497**      **0.9241849**      **0.9597115**  
Total Volume (Vd) ft3      **0.6269413**      **0.7423497**      **0.9241849**      **0.9597115**

**Temperature (deg F)**  
beginning inlet      **50**      **62.6**      **64.4**      **68**  
ending inlet      **62.6**      **64.4**      **66.2**      **71.6**  
beginning outlet      **50**      **62.6**      **64.4**      **68**  
ending outlet      **62.6**      **64.4**      **66.2**      **71.6**  
average outlet temp (Tmo)      **56.3**      **63.5**      **65.3**      **69.8**  
average temp (Tm)      **56.3**      **63.5**      **65.3**      **69.8**

**CALIBRATION METER**

**Volume**      **Yc**      **1.006**      **1.006**      **1.006**      **1.006**  
beginning reading      **83.435**      **84.060**      **85.620**      **86.54**  
ending reading      **84.060**      **84.790**      **86.540**      **87.48**  
Total Volume (Vc) ft3      **0.625**      **0.73**      **0.92**      **0.94**

**Temperature**  
beginning      **57.2**      **57.2**      **59**      **59**  
ending      **57.2**      **59**      **59**      **59**  
average temp (Tc)      **57.2**      **58.1**      **59**      **59**

**Time (min)**      **10**      **10**      **11**      **10**      **AVERAGE**  
**Y:**      **0.996**      **0.993**      **1.005**      **0.995**      **0.997**  
**Difference from Average:**      **-0.001**      **-0.004**      **0.007**      **-0.002**

Y Acceptance criteria: +/- 0.02 From Average

GAS DILUTION SYSTEM VERIFICATION METHOD									
Project: GP-Toledo		Date: 11/3/2014							
Dilution Gas	20.93 % O2	1ST DILUTION= 90 %							
Undiluted Gas	18.01 % O2	2ND DILUTION= 50 %							
		Run 1		Run 2		Run 3		Average	
Actual Concn. (ppm)	Instrument Response (ppm)	% Diff. from Average (ppm)	Instrument Response (ppm)	% Diff. from Average (ppm)	Instrument Response (ppm)	% Diff. from Average (ppm)	Instrument Response (ppm)	% Diff. from Average (ppm)	Instrument Response (ppm)
1ST DILUTION	18.837	19.1	0.1%	19.12	0.2%	19.03	0.3%	19.08	1.3%
2ND DILUTION	10.465	10.31	-0.1%	10.35	0.3%	10.3	0.2%	10.32	-1.4%
Mid-Level Gas	18.01	18.41	0.3%	18.32	-0.1%	18.31	0.2%	18.35	1.9%

Note: All percent differences must be within +/- 2.0%.

00010



Praxair  
 5700 South Alameda Street  
 Los Angeles, CA 90058  
 Tel: (323) 585-2154 Fax: (714) 542-6689  
 PGVPID: F22013

DocNumber: 000052499

**Customer & Order Information:**

PRAXAIR WHSE VANCOUVER W  
 603 SE VICTORY AVE  
 VANCOUVER WA 986810

Praxair Order Number: 23050520  
 Customer P. O. Number: 04307063  
 Customer Reference Number:

Fill Date: 3/9/2013  
 Part Number: NI CD2205E-AS  
 Lot Number: 108306801  
 Cylinder Style & Outlet: AS CGA 590  
 Cylinder Pressure & Volume: 2000 psig 140 cu. ft.

**Certified Concentration:**

Expiration Date:	4/13/2021	NIST Traceable
Cylinder Number:	CC49794	Analytical Uncertainty:
21.85 %	CARBON DIOXIDE	± 2 %
20.93 %	OXYGEN	± 1 %
Balance	NITROGEN	

**Certification Information:** Certification Date: 4/13/2013 Term: 96 Months Expiration Date: 4/13/2021

This cylinder was certified according to the 1997 EPA Traceability Protocol, Document #EPA-800/R-97/121, using Procedure G2. The certification expiration date was assigned using the May 2012 revision of the EPA Traceability Protocol document. Do Not Use this Standard if Pressure is less than 150 PSIG.

**G2 ANALYSIS FOR CO2 WAS DONE USING STEC INC SGD-710C @ 70% (C.F.=0.6943)**

**Analytical Data:** (R=Reference Standard, Z=Zero Gas, C=Gas Candidate)

**1. Component: CARBON DIOXIDE**

Requested Concentration: 22 %  
 Certified Concentration: 21.85 %  
 Instrument Used: Horiba VIA-S10 S/N 2907014  
 Analytical Method: NDIR  
 Last Multipoint Calibration: 3/20/2013

Reference Standard Type: GMIS  
 Ref. Std. Cylinder #: CC265304  
 Ref. Std. Conc: 17.97%  
 Ref. Std. Traceable to SRM #: 2745  
 SRM Sample #: 9-B-09  
 SRM Cylinder #: CAL-010765

First Analysis Data:		Date:	4/10/2013
Z: 0	R: 17.97	C: 15.02	Conc: 15.02
R: 17.87	Z: 0	C: 15.04	Conc: 15.04
Z: 0	C: 15.04	R: 17.97	Conc: 15.04
UOM: %	Mean Test Assay:		15.03 %

Second Analysis Data:		Date:	
Z: 0	R: 0	C: 0	Conc: 0
R: 0	Z: 0	C: 0	Conc: 0
Z: 0	C: 0	R: 0	Conc: 0
UOM: %	Mean Test Assay:		0 %

**2. Component: OXYGEN**

Requested Concentration: 21 %  
 Certified Concentration: 20.93 %  
 Instrument Used: OXYMAT 5E  
 Analytical Method: PARAMAGNETIC  
 Last Multipoint Calibration: 3/20/2013

Reference Standard Type: GMIS  
 Ref. Std. Cylinder #: CC92589  
 Ref. Std. Conc: 19.99%  
 Ref. Std. Traceable to SRM #: 2659a  
 SRM Sample #: 71-37-B  
 SRM Cylinder #: CLM-006734

First Analysis Data:		Date:	4/10/2013
Z: 0	R: 20	C: 20.94	Conc: 20.93
R: 20	Z: 0	C: 20.94	Conc: 20.93
Z: 0	C: 20.94	R: 20	Conc: 20.93
UOM: %	Mean Test Assay:		20.93 %

Second Analysis Data:		Date:	
Z: 0	R: 0	C: 0	Conc: 0
R: 0	Z: 0	C: 0	Conc: 0
Z: 0	C: 0	R: 0	Conc: 0
UOM: %	Mean Test Assay:		0 %

Analyzed by:   
 Shameela Jiffrey

Certified by:

Information contained herein has been prepared at your request by qualified experts within Praxair Distribution, Inc. While we believe that the information is accurate within the limits of the analytical methods employed and is complete to the extent of the specific analyses performed, we make no warranty or representation as to the suitability of the use of the information for any purpose. The information is offered with the understanding that any use of the information is at the sole discretion and risk of the user. In no event shall the liability of Praxair Distribution, Inc., arising out of the use of the information contained herein exceed the fee established for providing such information.

DocNumber: 000051337

**CERTIFICATE OF ANALYSIS / EPA PROTOCOL GAS**

**Customer & Order Information:**

PRAXAIR WHSE VANCOUVER W  
603 SE VICTORY AVE  
VANCOUVER WA 986610

Praxair Order Number: 23050701  
Customer P. O. Number: 04307067  
Customer Reference Number:

Fill Date: 3/9/2013  
Part Number: NI CD1105E-AS  
Lot Number: 109306804  
Cylinder Style & Outlet: AS CGA 590  
Cylinder Pressure & Volume: 2000 psig 140 cu. ft.

**Certified Concentration:**

Expiration Date:	3/27/2021	NIST Traceable
Cylinder Number:	CC120997	Analytical Uncertainty:
11.02 %	CARBON DIOXIDE	± 1 %
10.49 %	OXYGEN	± 1 %
Balance	NITROGEN	

**Certification Information:** Certification Date: 3/27/2013 Term: 96 Months Expiration Date: 3/27/2021

This cylinder was certified according to the 1997 EPA Traceability Protocol, Document #EPA-600/R-97/121, using Procedure G1. The certification expiration date was assigned using the May 2012 revision of the EPA Traceability Protocol document. Do Not Use this Standard if Pressure is less than 150 PSIG.

**Analytical Data:** (R=Reference Standard, Z=Zero Gas, C=Gas Candidate)

**1. Component: CARBON DIOXIDE**

Requested Concentration: 11 %  
Certified Concentration: 11.02 %  
Instrument Used: Horiba VIA-510 S/N 2807014  
Analytical Method: NDIR  
Last Multipoint Calibration: 3/4/2013

Reference Standard Type: GMIS  
Ref. Std. Cylinder #: CC7663  
Ref. Std. Conc: 10.07%  
Ref. Std. Traceable to SRM #: 1875b  
SRM Sample #: 6-F-51  
SRM Cylinder #: CAL014588

<b>First Analysis Data:</b>		<b>Date:</b> 3/15/2013	
Z: 0	R: 10.07	C: 11.01	Conc: 11.01
R: 10.07	Z: 0	C: 11.02	Conc: 11.02
Z: 0	C: 11.03	R: 10.07	Conc: 11.03
UOM: %	Mean Test Assay:		11.02 %

<b>Second Analysis Data:</b>		<b>Date:</b>	
Z: 0	R: 0	C: 0	Conc: 0
R: 0	Z: 0	C: 0	Conc: 0
Z: 0	C: 0	R: 0	Conc: 0
UOM: %	Mean Test Assay:		0 %

**2. Component: OXYGEN**

Requested Concentration: 10.5 %  
Certified Concentration: 10.49 %  
Instrument Used: OXYMAT 5E  
Analytical Method: PARAMAGNETIC  
Last Multipoint Calibration: 3/4/2013

Reference Standard Type: GMIS  
Ref. Std. Cylinder #: SA15925  
Ref. Std. Conc: 10.01%  
Ref. Std. Traceable to SRM #: 2658a  
SRM Sample #: 72-28-B  
SRM Cylinder #: CLM-006896

<b>First Analysis Data:</b>		<b>Date:</b> 3/15/2013	
Z: 0	R: 10	C: 10.48	Conc: 10.49
R: 10	Z: 0	C: 10.48	Conc: 10.49
Z: 0	C: 10.48	R: 10	Conc: 10.49
UOM: %	Mean Test Assay:		10.49 %

<b>Second Analysis Data:</b>		<b>Date:</b>	
Z: 0	R: 0	C: 0	Conc: 0
R: 0	Z: 0	C: 0	Conc: 0
Z: 0	C: 0	R: 0	Conc: 0
UOM: %	Mean Test Assay:		0 %

Analyzed by:

Certified by:

  
Shameela Jiffrey

# AIRDATA MULTIMETER CERTIFICATE OF CALIBRATION

Customer ID: 020243 S/N: M1217  
 Customer: Bighorn Environmental City: Liberty Lake State: WA  
 Model #: 860c PO #: \_\_\_\_\_ Calibration Due Date: \_\_\_\_\_ Order #: 120531  
 Test By: [Signature] Date 03-19-12 Rh 25 % Ambient Temperature 72 °F Barometric Pressure 28.36

### ABSOLUTE PRESSURE TEST (in Hg) TEST METER TOLERANCE = ± 2.0 % ± .1 in Hg

Pressure Standard: Heise #02-R S/N: 41741/42451 <input checked="" type="checkbox"/>	Pressure Standard: Heise #12-R S/N: 43168/44731 _____
Pressure Standard: Heise #04-R S/N: 41743/42453 _____	Pressure Standard: Heise #14-R S/N: 43412/45043 _____
Pressure Standard: Heise #06-R S/N: 41742/42452 _____	Pressure Standard: Heise #18-R S/N: 44581/46845 _____
Pressure Standard: Heise #08-R S/N: 42186/43328 _____	Pressure Standard: Heise #20-R S/N: 44582/46847 _____
Pressure Standard: Heise #10-R S/N: 42203/43352 _____	

Approx Set Point	Standard	Test Meter	% Diff
14.0	13.84	13.8	-29
28.4	28.36	28.3	-21
40.0	40.39	40.3	-22

### DIFFERENTIAL PRESSURE TEST (in wc) TEST METER TOLERANCE = ± 2.0 % ± 0.001 in wc

Pressure Standard: Heise #01-L S/N: 41739/42449 <input checked="" type="checkbox"/>	Pressure Standard: Heise #11-L S/N: 43165/44551 _____
Pressure Standard: Heise #01-R S/N: 41739/42448 <input checked="" type="checkbox"/>	Pressure Standard: Heise #11-R S/N: 43185/44730 _____
Pressure Standard: Heise #02-L S/N: 41741/42454 <input checked="" type="checkbox"/>	Pressure Standard: Heise #12-L S/N: 43168/44732 _____
Pressure Standard: Heise #03-L S/N: 41738/42448 _____	Pressure Standard: Heise #13-L S/N: 43415/45041 _____
Pressure Standard: Heise #03-R S/N: 41738/42445 _____	Pressure Standard: Heise #13-R S/N: 43415/45039 _____
Pressure Standard: Heise #04-L S/N: 41743/42456 _____	Pressure Standard: Heise #14-L S/N: 43412/45045 _____
Pressure Standard: Heise #05-L S/N: 41740/42450 _____	Pressure Standard: Heise #17-L S/N: 44579/46842 _____
Pressure Standard: Heise #05-R S/N: 41740/42447 _____	Pressure Standard: Heise #17-R S/N: 44579/46841 _____
Pressure Standard: Heise #06-L S/N: 41742/42455 _____	Pressure Standard: Heise #18-L S/N: 44581/46846 _____
Pressure Standard: Heise #07-L S/N: 42185/42186 _____	Pressure Standard: Heise #19-L S/N: 44580/46844 _____
Pressure Standard: Heise #07-R S/N: 42185/43326 _____	Pressure Standard: Heise #19-R S/N: 44580/46843 _____
Pressure Standard: Heise #08-L S/N: 42186/43329 _____	Pressure Standard: Heise #20-L S/N: 44582/46848 _____
Pressure Standard: Heise #08-R S/N: 42202/43351 _____	
Pressure Standard: Heise #09-R S/N: 42202/43350 _____	
Pressure Standard: Heise #10-L S/N: 42203/43353 _____	

Approx Set Point	Standard	Test Meter	% Diff
.0500	.0515	.0513	-.39
.1250	.1277	.1274	-.23
.2250	.2254	.2250	-.18
.2700	.2705	.2701	-.15
2.000	2.059	2.053	-.29
3.600	3.661	3.648	-.36
4.400	4.415	4.414	-.02
27.00	27.31	27.37	.22
50.00	50.56	50.58	.04
Over Pressure	NA	✓	NA

**Shortridge Instruments, Inc.**  
 7855 East Redfield Road Scottsdale, Arizona 85260  
 (480) 991-6744 • Fax (480) 443-1267 • www.shortridge.com



# Shorridge Instruments, Inc. AirData Multimeter Calibration Equipment

Order Number: 120539 Serial Number: M12172 Test Type: Initial As-Received Final

Model	S/N	Heise Model	Mfgd & Calibrated by	Calibration Date	Due Date
ADM #02-R	41741/42451	PPM-2	Dresser Industries (Ashcroft)	04/08/11	04/2012
ADM #04-R	41743/42453	PPM-2	Dresser Industries (Ashcroft)	10/10/11	10/2012
ADM #06-R	41742/42452	PPM-2	Dresser Industries (Ashcroft)	09/19/11	09/2012
ADM #08-R	42189/43328	PPM-2	Dresser Industries (Ashcroft)	03/16/11	03/2012
ADM #10-R	42209/43322	PPM-2	Dresser Industries (Ashcroft)	01/16/12	01/2013
ADM #12-R	43186/44731	PPM-2	Dresser Industries (Ashcroft)	12/19/11	12/2012
ADM #14-R	43412/46045	PPM-2	Dresser Industries (Ashcroft)	07/21/11	07/2012
ADM #18-R	44581/48845	PPM-2	Dresser Industries (Ashcroft)	04/29/11	04/2012
ADM #20-R	44582/48847	PPM-2	Ashcroft, Inc.	05/28/11	05/2012
602-R, 04-R, 06-R, 08-R, 10-R, 12-R, 14-R, 18-R, 20-R		Rated Accuracy: 0.05% fs (0.0305 in Hg)	Range: 0-80 in Hg	Resolution: 0.01	Uncertainty: < 0.0358
		Rated Accuracy: 0.05% fs (0.0305 in Hg)	Range: 0-80 in Hg	Resolution: 0.001	Uncertainty: < 0.0358

Model	S/N	Heise Model	Mfgd & Calibrated by	Calibration Date	Due Date
ADM #01-L	41738/42448	PPM-1	Dresser Industries (Ashcroft)	04/28/11	04/2012
ADM #01-R	41739/42446	PPM-1	Dresser Industries (Ashcroft)	05/04/11	04/2012
ADM #02-L	41741/42454	PPM-1	Dresser Industries (Ashcroft)	04/08/11	04/2012
ADM #03-L	41738/42448	PPM-1	Dresser Industries (Ashcroft)	11/08/11	10/2012
ADM #03-R	41739/42445	PPM-1	Dresser Industries (Ashcroft)	10/19/11	10/2012
ADM #04-L	41743/42455	PPM-1	Dresser Industries (Ashcroft)	10/19/11	10/2012
ADM #05-L	41740/42450	PPM-1	Dresser Industries (Ashcroft)	10/18/11	10/2012
ADM #05-R	41740/42447	PPM-1	Dresser Industries (Ashcroft)	10/14/11	09/2012
ADM #06-L	41742/42455	PPM-1	Dresser Industries (Ashcroft)	09/30/11	09/2012
ADM #07-L	42186/42138	PPM-1	Dresser Industries (Ashcroft)	08/27/11	08/2012
ADM #07-R	42185/43328	PPM-1	Dresser Industries (Ashcroft)	03/18/11	03/2012
ADM #08-L	42186/43329	PPM-1	Dresser Industries (Ashcroft)	03/10/11	03/2012
ADM #08-R	42202/43351	PPM-1	Dresser Industries (Ashcroft)	03/10/11	03/2012
ADM #09-R	42202/43350	PPM-1	Dresser Industries (Ashcroft)	01/25/12	01/2013
ADM #10-L	42203/43353	PPM-1	Dresser Industries (Ashcroft)	01/23/12	01/2013
ADM #11-L	43185/44551	PPM-1	Dresser Industries (Ashcroft)	01/23/12	01/2013
ADM #11-R	43185/44730	PPM-1	Dresser Industries (Ashcroft)	01/23/12	01/2013
ADM #12-L	43186/44732	PPM-1	Dresser Industries (Ashcroft)	12/22/11	12/2012
ADM #13-L	43415/46041	PPM-1	Dresser Industries (Ashcroft)	12/02/11	12/2012
ADM #13-R	43415/46039	PPM-1	Dresser Industries (Ashcroft)	12/14/11	12/2012
ADM #14-L	43412/46045	PPM-1	Dresser Industries (Ashcroft)	07/21/11	07/2012
ADM #17-L	44578/48842	PPM-1	Dresser Industries (Ashcroft)	07/14/11	07/2012
ADM #17-R	44579/48841	PPM-1	Ashcroft, Inc.	07/14/11	07/2012
ADM #18-L	44581/48846	PPM-1	Ashcroft, Inc.	04/08/11	04/2012
ADM #18-R	44580/48844	PPM-1	Ashcroft, Inc.	04/29/11	04/2012
ADM #19-R	44580/48844	PPM-1	Ashcroft, Inc.	08/27/11	08/2012
ADM #20-L	44582/48848	PPM-1	Ashcroft, Inc.	08/14/11	08/2012
#01-L, 03-L, 05-L, 07-L, 09-L, 11-L, 13-L, 17-L, 18-L, 201-R, 03-R, 05-R, 07-R, 09-R, 11-R, 13-R, 17-R, 19-R, #02-L, 04-L, 06-L, 08-L, 10-L, 12-L, 14-L, 16-L, 20-L		Rated Accuracy: > 0.07% fs (0.000175 in wc)	Range: 0.0-0.25 in wc	Res.: 0.00001	Uncertainty: < 0.00035
		Rated Accuracy: > 0.06% fs ( 0.003 in wc)	Range: 0.0-5.0 in wc	Res.: 0.0001	Uncertainty: < 0.00348
		Rated Accuracy: > 0.08% fs (0.03 in wc)	Range: 0.0-50.0 in wc	Res.: 0.001	Uncertainty: < 0.0348

Model	S/N	Model	Mfgd & Calibrated by	Calibration Date	Due Date
Vel Eqv Transfer Standard	S/N: M02009	Model ADM-870C	Shorridge Instruments, Inc.	12/19/11	12/2012
Vel Eqv Transfer Standard	S/N: M02803	Model ADM-870C	Shorridge Instruments, Inc.	01/24/12	01/2013
Vel Eqv Transfer Standard	S/N: M02903	Model ADM-870C	Shorridge Instruments, Inc.	12/19/11	12/2012
Vel Eqv Transfer Standard	S/N: M10639	Model ADM-870C	Shorridge Instruments, Inc.	12/19/11	12/2012
Vel Eqv Transfer Standard	S/N: M10840	Model ADM-870C	Shorridge Instruments, Inc.	12/19/11	12/2012
Vel Eqv Transfer Standard	S/N: M10867	Model ADM-870C	Shorridge Instruments, Inc.	01/24/12	01/2013
Vel Eqv Transfer Standard	S/N: M10901	Model ADM-870C	Shorridge Instruments, Inc.	12/19/11	12/2012
Rated Accuracy: Velocity ± 1.5% ± 3.5 fpm			Range: 100-6000 fpm Resolution: 0.1	Uncertainty: < 5.00 fpm at 100 fpm; < 7.50 fpm at 500 fpm	

Model	S/N	Model	Mfgd & Calibrated by	Calibration Date	Due Date
RTD Simulator	S/N: 249	Model RTD-1000/500	General Resistance	01/24/08	01/2012
RTD Simulator	S/N: 250	Model RTD-1000/500	General Resistance	01/24/08	01/2012
RTD Simulator	S/N: 253	Model RTD-1000/500	General Resistance	01/24/08	01/2012
RTD Simulator	S/N: 254	Model RTD-1000/500	General Resistance	03/07/08	03/2012
RTD Simulator	S/N: 256	Model RTD-1000/500	General Resistance	03/07/08	03/2012
RTD Simulator	S/N: 257	Model RTD-1000/500	General Resistance	03/07/08	03/2012
RTD Simulator	S/N: 282	Model RTD-1000/500	General Resistance	12/19/11	12/2012
RTD Simulator	S/N: 283	Model RTD-1000/500	General Resistance	12/18/11	12/2012
RTD Simulator	S/N: 284	Model RTD-1000/500	General Resistance	12/19/11	12/2012
Rated Accuracy: 0.025% of setting			Range: 100 Ω to 11111.10 Ω Resolution: 0.01 Ω	Uncertainty: ± 0.00032° F	

Model	S/N	Model	Mfgd & Calibrated by	Calibration Date	Due Date
Thermometer #1	S/N: 8A089/Thermistor	S/N A410880	Hart Scientific (Fluke)	01/14/11	01/2013
Thermometer #2	S/N: 8B104/Thermistor	S/N 871507	Hart Scientific (Fluke)	11/09/10	11/2012
Thermometer #5	S/N: B11780/Thermistor	S/N B10505	Hart Scientific (Fluke)	01/24/11	01/2013
Thermometer #6	S/N: B11782/Thermistor	S/N B10509	Hart Scientific (Fluke)	01/24/11	01/2013
Rated Accuracy(Combined): 0.028° F @ 0.018° F			Range: 32° F-178° F Resolution: 0.001° F	Combined Uncertainty with Baths: ± 0.040° F	

Model	S/N	Model	Mfgd & Calibrated by	Calibration Date	Due Date
Temp Transfer Standard	S/N M00136	Model ADM-870	Shorridge Instruments, Inc.	10/25/11	10/2012
Temp Transfer Standard	S/N M96100	Model ADM-870	Shorridge Instruments, Inc.	03/08/11	03/2012
Rated Accuracy: 0.03° F			Range: 33° F-158° F Resolution: 0.01° F	Uncertainty: < 0.023° F	
Total combined Uncertainty for MultiTemp and TempProbe testing: ± 0.046° F					

This form must remain with the Certificate of Calibration corresponding to the Order Number listed above.

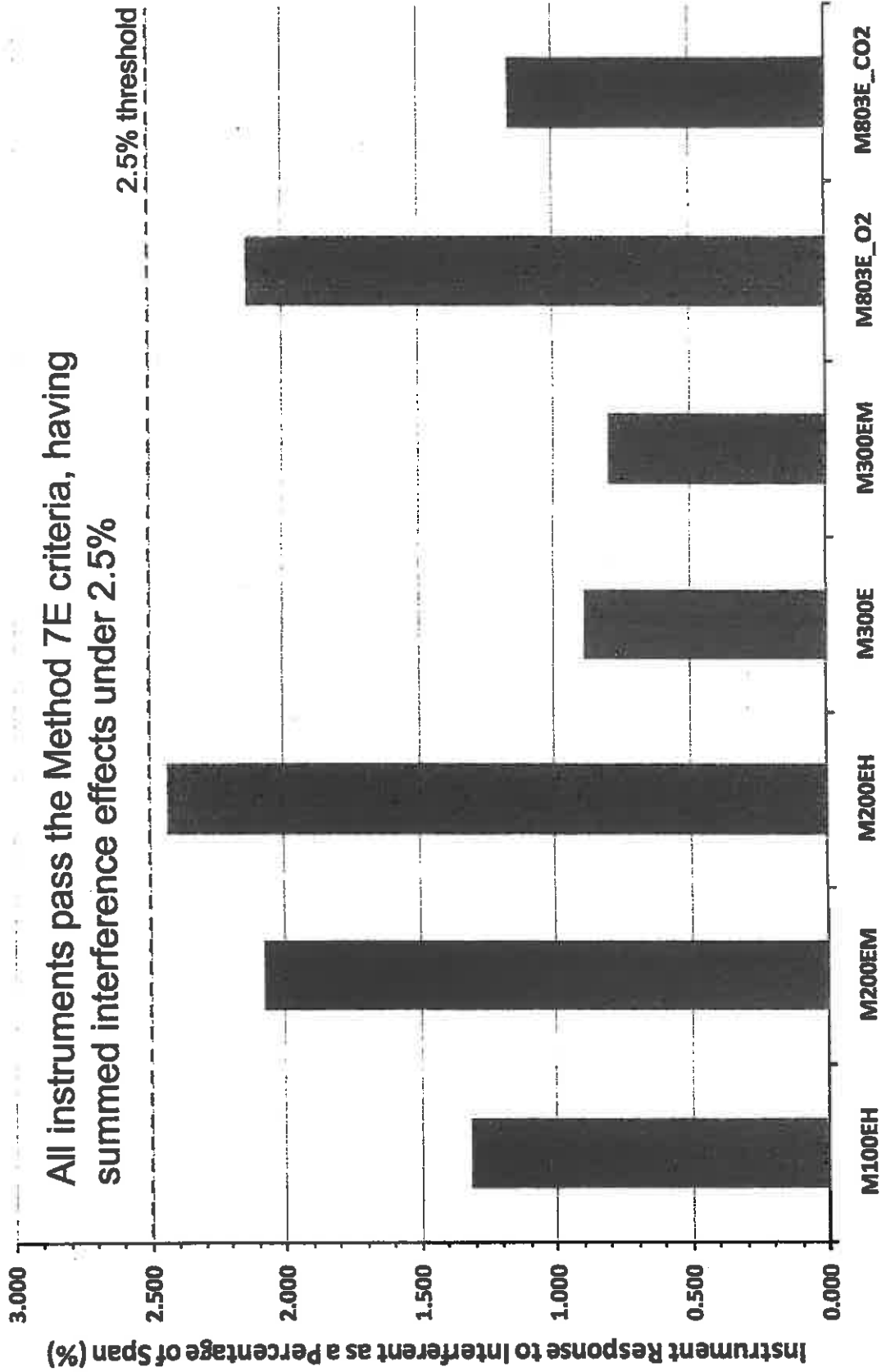
**Shorridge Instruments, Inc.**  
7855 East Redfield Road Scottsdale, Arizona 85260 • (480) 991-5744 • Fax (480) 443-1267 • www.shorridge.com

00014

# Span + Interferent: 40CFR60 App. 4-A Method 7E

## 40CFR60 App. A-4 Method 7E - Zero + Interferent Effect as a Percentage of Span

All instruments pass the Method 7E criteria, having summed interference effects under 2.5%



APIEX INSTRUMENTS REFERENCE METER VERIFICATION  
USING WET-TEST METER #11A88

2-POINT ENGLISH UNITS

Parameter	Conversion	Units
Old Meter	528	"R
Old Probe	29.92	in Hg
K <sub>1</sub>	17.847	in Air Hg

Calibration Conditions	
Date	16-Jan-14
Time	8:00
Barometric Pressure	29.60 in Hg
Calibration Tech	EW
DCM Serial Number	S-110-367185

Calibration Meter Information	
Volume Model #	AL20
WTM Model #	11A88
WTM Number	0.8999
Original Sign Certificate	0.8999

Run Time	Metering Conditions				Calibration Meter				Reference Meter						
	Volume Initial (cc)	Volume Final (cc)	Volume (cc)	Volume (cc)	Volume Initial (cc)	Volume Final (cc)	Volume (cc)	Volume (cc)	Outlet Temp (°C)	Outlet Temp (°F)	Outlet Temp (°C)	Outlet Temp (°F)	Correction Factor	Final (cc)	Final (cc)
6.00	983.870	983.870	0.000	983.870	977.780	977.780	0.000	977.780	67	67	67	67	0.8915	0.8883	0.975
10.00	989.284	989.284	5.414	989.284	977.780	977.780	0.000	977.780	67	67	67	67	0.8915	1.0055	0.557

I certify that the above dry Gas Meter was calibrated in accordance with 16CFR 101.11(a), CFR 40 Part 60, App A, Method 4, Paragraph 7.1.2.2, using the Precision Wet Test Meter # 11A88, which in turn was calibrated using the American Test Power # 3786, certificate # P107, which is traceable to the National Bureau of Standards (NBS-1).

Signature: *[Handwritten Signature]*

Date: 1/16/14

**APPENDIX D  
GP PRODUCTION DATA**



Source Tested	Date	Date	Date	time (days)	BSW#2 cooks/day	BSW#2 ADT/day	BSW#2 ODT/day	stock flow GPM
BSW#2	11/5/2014 14:00:00	11/5/2014 15:00:00		0.042	22	391	352	1824
								31FIC365
								stock flow GPM
								1861
								Target Range
								1783-2179
								Average Stock Flow GPM During Tests
								1539.9
								Average Stock Flow Day
								33FIC004A
								stock flow GPM
								1748
								33FIC004A
								stock flow GPM
								2011
								October Average
								Washer Flow GPM
								1649.53972 from PI
								Tons Production
								1175 From plb2014



**APPENDIX E  
EPA/ODEQ CORRESPONDENCE**



September 25, 2014

Mr. Mike Eisele  
Oregon Department of Environmental Quality  
750 Front Street, Suite 120  
Salem, OR 97301

**RE: Georgia-Pacific West Toledo, Oregon Mill's Brown Stock Washer Methanol Testing**

Dear Mr. Eisele:

Please allow this letter to serve as notification that Bighorn Environmental is scheduled to perform methanol testing on Georgia Pacific's Brown Stock Washer Lines to comply with the CCA rules at their Toledo, Oregon Pulp and Paper Mill.

**Purpose of Tests:** To determine compliance with the CCA rules as outlined in GP's permit.

**Sources, Parameters, and Test Dates:** The following table outlines sources, parameters, and proposed test dates.

SOURCES	PARAMETERS	TEST DATES
#1 Wash Row Combined Vent	Methanol, Velocity & Moisture	November 3-7
#1 Wash Row Foam Breaker	Methanol, Velocity & Moisture	
#1 Wash Row Vacuum Pump	Methanol, Velocity & Moisture	
#2 Wash Row Combined Vent	Methanol, Velocity & Moisture	
#3 Wash Row Combined Vent	Methanol, Velocity & Moisture	

If testing dates change, Bighorn or Georgia Pacific personnel will call you soon after scheduling the new dates so you can make preparations to observe.

**Test Methods:** Testing will be conducted in accordance with EPA Methods in *Title 40 CFR 60, Appendix A, July 2013*, and ODEQ methods in its *Source Sampling Manual, Volume 1, January 1992*.

Flow Rates: EPA Methods 1 & 2 (Shortridge digital manometer for low velocity sources, expected to be used on #1 WR combined vent)  
O<sub>2</sub> & CO<sub>2</sub>: EPA Method 3A  
Moisture: Oregon DEQ Method 4  
Methanol: NCASI CI/SG/PULP 94.03

**Discussion of Methods:** EPA Methods 1 & 2 will be used to determine flow rates. O<sub>2</sub> and CO<sub>2</sub> will be measured at each stack either directly or with a bag sample. The absence of cyclonic flow will be verified for each source. Georgia Pacific's Sam Adams received approval to use NCASI Method 94.03 (see attached letter). This method includes a spike solution and method blank as part of its QA/QC.

**Data Collection:** Bighorn uses standard forms, which contain all required regulatory data and any additional information necessary for flow rate determinations.

**Process data:** GP personnel will record the pulp production from each wash row during each test period.

**Sampling Replicates and Duration:** Bighorn will conduct tests consisting of a minimum of three-one hour runs for methanol including a pitot traverse and moisture determination during each run to determine flow rates. These

will be conducted concurrently with each test run. Testing on the three #1 Wash Row Vents will be conducted simultaneously.

**QC/QA:** Cross checks such as manual calculations of Bighorn's computer generated spreadsheet summaries allow test results verification. Bighorn files manufacturers' accuracy certificates and interference tables for CEMS, flow controllers, gases, etc. Additionally dry gas meters, pitot tubes, thermocouples, gas dividers, etc. are certified as per ODEQ and EPA requirements and frequencies. Where EPA or ODEQ frequencies are not specified, Bighorn has established those based on neighboring state's regulatory criteria.

Thorough sample methodology adherence, chain-of-custody procedures, and documentation provide proof of our QA/QC efforts. Relevant QA/QC documentation is included in the final report's Appendices for results support and regulatory review.

**ODEQ Source Sampling Manual Volume One Language**

- a. It is assumed today, but will be confirmed on or before the test day, that the duct air flow measuring meets criteria in EPA Methods 1 and 2.
- b. In no case, will sampling replicates be accepted if separated by a time duration of 24 or more hours, unless prior authorization is granted by ODEQ.
- c. The source to be tested must operate at a normal production rate during testing. Rates not in agreement with those stipulated in the Title V Operating Permit can result in test rejection for application to determine compliance. Imposed process limitations could also result from atypical rates.
- d. The department must be notified of any changes in source test plans prior to testing. Significant changes not acknowledged by ODEQ which could affect the accuracy and reliability of results could result in test report rejection.
- e. Method specific quality assurance/quality control procedures must be performed to ensure the data is valid for determining source compliance. Documentation of the procedures and results shall be presented in the source test report for review. Omission of this critical information may result in rejection of the data, requiring a re-test.
- f. Source test reports must be submitted to the department within 60 days of the test dates, unless another deadline has been stipulated, either by permit condition, or by ODEQ letter approval.
- g. Two copies of the completed source test report must be sent to the ODEQ Regional Operations staff person responsible for the source and the second copy to the Source Testing Coordinator, ODEQ headquarters in Portland, Oregon.

Please call me if you have any questions.

Sincerely,

Tim Homer  
Air Emissions Lab Manager

cc: Dan Kunde - Georgia Pacific



# Oregon

John A. Kitzhaber, MD, Governor

Department of Environmental Quality

Western Region - Salem Office

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Salem, OR 97301-1011

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[www.oregon.gov/DEQ](http://www.oregon.gov/DEQ)

September 29, 2014

Mr. Daniel Kunde  
Georgia Pacific Corporation  
1400 SE Butler Bridge Rd.  
Toledo, OR 97391

Mr. Tim Homer  
Bighorn Environmental Air Quality  
1324 N Liberty Lake Rd.  
Liberty Lake, WA 99019

Re: Georgia Pacific Corporation  
Title V Permit 21-0005-TV-01  
Brown Stock Washer Methanol Source Test Plan

Dear Mr. Kunde and Mr. Homer:

The source test plan received on September 26, 2014 for testing at the Georgia Pacific facility located in Toledo, OR has been review. The plan proposes to check the methanol emission rates from the brown stock washers. The methanol testing is approved with the following conditions:

#### GENERAL PROCESS CONDITIONS

- 1.) Only regular operating staff may adjust the production process and emission control parameters during the source performance tests and within two (2) hours prior to the tests. Any operating adjustments made during the source performance tests, which are a result of consultation during the tests with source testing personnel, equipment vendors or consultants, may render the source performance test invalid
- 2.) Unless otherwise specified in the Permit, source testing shall be performed as follows:
  - At least 90% of the design capacity for new or modified equipment.
  - At least 90% of the maximum operating rate for existing equipment; or
  - At 90 to 110% of the normal maximum operating rate for existing equipment. The normal maximum operating rate is defined as the 90<sup>th</sup> percentile of the average hourly operating rates during a 12 month period.

Documentation supporting the design capacity or operating rate determinations used must be included within the source test report.

- 3.) During compliance source testing, the following process parameters shall be determined, recorded and documented in the source test report. The process parameters below are to be reported for each individual test run and averaged for all test runs if appropriate.
  - Washer production rate (oven dried ton/hr)

#### EPA/ODEQ METHODS 1-4 CONDITIONS

- 4.) The flow rate for the exhaust stacks must meet the EPA Methods 1 & 2 criteria. For ducts with diameters less than 12" use EPA Method 1A instead of EPA Method 1. Clear diagrams and documentation of this must be included in the source test report.
- 5.) The exhaust ducts must be checked for cyclonic flow. Documentation of this must be provided in the test report.



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY  
RESEARCH TRIANGLE PARK, NC 27711

AUG 23 2006

OFFICE OF  
AIR QUALITY PLANNING  
AND STANDARDS

Mr. W. Samuel Adams, Jr.  
Environmental Superintendent  
Georgia-Pacific West, Inc.  
Toledo Pulp and Paper Operations  
1400 SE Butler Bridge Road  
Toledo, Oregon 97391

Dear Mr. Adams:

This is in response to your letter dated August 3, 2006, which requests the approval of an alternative test method for measuring the methanol concentration of gas emission streams from your Kraft pulp mill in Toledo, Oregon. The method that you are proposing would be an alternative to Method 308 required by 40 CFR Part 63, Subpart S, National Emission Standards for Hazardous Air Pollutants from the Pulp and Paper Industry, Section 63.457. You are proposing to use NCASI Method C/SG/PULP-94.03, entitled, "Chilled Impinger Test Method for Use on Pulp Mill Sources to Quantify Methanol Emissions," developed by the National Council for Air and Stream Improvement (NCASI) to measure methanol emissions. I notified the NCASI by letter dated October 6, 2004, that this test method met Method 301 criteria for measuring methanol from pulp and paper mill sources provided that the tester uses the appropriate correction factor. A copy of this letter is enclosed. Based on the data submitted by the NCASI and the similarity of the gas streams for which you propose to use the method to the gas streams from which the NCASI collected their supporting data, we are approving your request for use of this alternative test method at your facility in Toledo, Oregon.

Because we are currently able to approve alternative methods only on a site-specific basis, this approval to use NCASI Method C/SG/PULP-94.03 is limited to its use at your facility in Toledo, Oregon. If you need further assistance, please contact Gary McAlester at (919) 541-1062.

Sincerely,

Constance E. Oldham, Ph.D., Group Leader  
Measurement Technology Group

Enclosure

cc: Mr. Gary Andes, DEQ Western Regional Office  
Mr. Doug Hardesty, Region 10  
Mr. Rai Peterson, DEQ Western Regional Office  
Mr. Stephen Shedd, EPA/OAQPS/SPPD



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY  
RESEARCH TRIANGLE PARK, NC 27711

OCT 6 2004

OFFICE OF  
AIR QUALITY PLANNING  
AND STANDARDS

Dr. Vipin Varma  
NCASI  
Southern Regional Center  
P.O. Box 141020  
Gainesville, Florida 32614-1020


Dear Dr. Varma:

I am writing in response to your request dated June 5, 2003, asking that we review the data that you submitted supporting your request to modify NCASI Method C/SG/PULP-94.02 by eliminating the backup silica gel tubes from the sampling train when it is used to measure only methanol. The modified method would be renamed as NCASI Method C/SG/PULP-94.03. We agree with your conclusion that the modified method met Method 301 criteria for measuring methanol in air emissions samples from various sources at pulp and paper mills regulated under 40 CFR Part 63, Subpart S, Paragraph 446. I have summarized in the enclosed Table the correction factors for the different sources. During any future testing, the tester must document and use the appropriate correction factor to correct the data from the test method.

As we discussed, each specific source must make its own alternative test method request. However, we can and will consider the validation data that you submitted in evaluating an alternative method request from any source similar to the ones at which you collected your validation data.

If you have any questions about our comments or you would like to meet to discuss them, please contact Gary McAllister of my staff at (919) 541-1062.

Sincerely,

  
Connesus B. Oldham, Ph.D., Group Leader  
Source Measurement Technology Group

Enclosure

cc: K. C. Husted (C439-03)  
Stephen A. Shedd (C439-03)  
Jeffrey A. Telander (C504-05)

Internet Address (URL) = <http://www.epa.gov>

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